Rheological Studies on Pretreated Feed and Melter Feed from C-104 and AZ-102

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January 2001

Prepared for CH2M Hill Hanford Group under Project Number 41503

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Summary

Rheological and physical properties testing was conducted on actual AZ-102 and C-104 melter feed samples prior to the addition of glass formers and secondary waste products. Analyses were repeated on the C-104 samples following the addition of simulated Sr/TRU secondary waste. Analyses were repeated again following addition of glass formers to both AZ-102 and C-104 samples. Samples from both feeds were tested at the target solids concentrations of 5, 15, and 25 wt%¹. This data on actual waste is required to validate and qualify results obtained with simulants.

The AZ-102 feed was received for this task after washing and leaching. The AZ-102 feed contained 9.54 wt% solids. At this solids concentration, no standing liquid was observed in the AZ-102 feed. The C-104 feed was also received following washing and leaching. The AZ-102 feed contained 20 wt% solids and contained roughly 15 vol% standing liquid.

The initial AZ-102 and C-104 feeds displayed very different rheological properties. The initial 5 and 15 wt% C-104 feeds displayed near Newtonian behavior, and the 25 feed has a small yield stress of ~5 Pa giving it a slight Bingham Plastic component. The viscosity of the feeds at 33 s⁻¹ were 9.8, 15, and 160 cP for the 5, 15, and 25 wt% feeds respectively with very little if any thixotropic behavior. By comparison, the AZ-102 feed showed much higher initial viscosities of 12, 530, 900, and 4600 cP for the 5, 15, 20, and 25 wt% feeds. In addition, the AZ-102 feeds displayed significant irreversible shear thinning. Surprisingly, no significant temperature effects were seen for the C-104 or AZ-102 samples measured at 25 and 50°C.

Very little change in rheological properties was observed following secondary waste product and glass former addition to the C-104 feed while the yield and viscosity the AZ-102 feed dropped following glass former and secondary waste addition. Since the addition of dry glass formers to the AZ-102 feed should have increased the total solids load, it would have been expected to see an increase the rheological properties. The observed decrease is most likely the result of the irreversible shear thinning of the AZ-102 samples as the testing progressed.

A mixing and aging study was conducted on the 15 wt% AZ-102 and 25 wt% C-104 feeds following glass former and secondary waste product additions. The additions were made and the slurries were stirred at a rate that delivered the same energy per volume as expected in the River Protection Project Waste Treatment Plant flow sheet. Slurries were stirred at this rate for one week. The rheology of the mixed slurries were examined at 1 hr, 1 day and 1 week. The yield and viscosity of the AZ-102 slurry decreased over the one week mixing period consistent with the previous observations of irreversible shear thinning in this slurry. By contrast the yield and viscosity of the C-104 slurry increased over the one week mixing period. The C-104 slurry yield increased from 28 Pa after one hour to 56 Pa after one week. Over this same period, the viscosity of the C-104 slurry increased from 910 cP to 1700 cP at 33s⁻¹.

Following the mixing study, the 15 wt% AZ-102 and 25 wt% C-104 slurries were allowed to settle for one week. The AZ-102 sample contained standing liquid, which was removed, while the C-104 sample contained no standing liquid. The rheology of the settled solids were then examined. The yield and viscosity of the AZ-102 settled solids were higher than similar testing after one week of mixing. This increase was expected and attributed to increased solids loading

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¹ In this report, wt% solids are based on residual mass after 24 hours at 105°C.

resulting from removal of the standing liquid. The viscosity of the C-104 settled material was similar to the results after one week of mixing, but the yield increased to approximately 80 Pa.

The results of the mixing and aging studies suggest that while the AZ-102 initial feed and final melter feed material may be very difficult to mix and transport, irreversible shear thinning significantly reduces the yield and viscosity. Therefore, exposing this material to some initial shearing may be an option for reducing these critical transport properties. By contrast, the yield and viscosity of the initial C-104 material did not display significant irreversible shear thinning. The yield and viscosity of the C-104 melter feed increased with mixing and the yield increased further with aging. These results suggest the final C-104 melter feed could be very difficult to mix and transport on a 25 wt% basis.

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1.0 Introduction

The scope of the present work was to obtain physical and rheological data on actual high-level waste melter feed samples. The physical and rheological properties of the high level waste melter feed are important considerations in the selection of the melter feed preparation flowsheet and processing equipment such as mixers, pumps, piping and sampling. Measurements on actual waste are required to validate and qualify results obtained with simulants. Measurements were conducted to the quality requirements in PNNL's Standards-Based Management System (SBMS).

Actual samples from tanks AZ-102 and C-104 were used in this testing. Multiple samples from each tank were received from Hanford's 222-S laboratory. Using this material, a composite was prepared for each of the tanks. Each of these composites were then processed through caustic leaching, washing and dewatering steps as described in Brooks et al. (2000a, 2000b).

Solids concentration, settling rate, density and shear stress versus shear rate were measured on the samples after adjusting the samples to 3 solids concentrations (nominally 5, 15 and 25 wt%)². The solids content was first adjusted by decanting standing liquid and then evaporation under a flow of air as needed for the more concentrated samples. The same measurements were repeated on the C-104 samples following the addition of simulated Sr/TRU secondary waste. Analyses were repeated again following addition of glass formers to both AZ-102 and C-104 samples. The original work scope included testing of the AZ-102 evaporated feed following addition of secondary waste products. However, given the small volume of secondary waste products to be added, this testing was deleted as detailed in the Appendix A to Test Plan 29953-073 contained in Appendix B.

Mixing and aging studies were conducted on the 15 wt% solids AZ-102 and 25 wt% solids C-104 slurries with glass formers and secondary waste products. The slurries were placed in a mixing vessel at a shear rate consistent with that expected in the River Protection Project Waste Treatment Plant. Glass formers and secondary waste products were added and the mixing continued for 1 week. During this week, shear stress versus shear rate analyses were conducted after 1 hour, 1 day and 1 week. The slurries were then left undisturbed for 1 week before a shear stress versus shear rate analysis was conducted on the settled solids.

Following addition of secondary waste products and glass formers, the resulting melter feed slurries had a higher solids content. However, in this report, samples will be referred to according to the target solids content for the evaporated feeds (e.g., the feed evaporated to 25 wt% solids is still referred to as the 25 wt% solids slurry event after the addition of dry glass formers.

This report describes the experimental approach and results of the testing. Specifications for this work were provided to Battelle by BNFL under Task Specification Numbers TS-W375HV-PR00011, and TS-W375HV-PR00012. This report also provides a means of transmitting to BNFL the completed test plan and analytical data³.

² In this report, wt% solids are based on residual mass after 24 hours at 105°C.

³ Results presented in this report are based on work conducted under Technical Procedure 29953-010, and Test Plan 29953-73.

2.0 Experimental Approach

2.1 Simulated Secondary Waste Products

Glass formulations provided by Catholic University of America's Vitreous State Laboratory (VSL) required significant quantities of secondary waste products that were not available from the actual waste pretreatment testing. Therefore, AZ-102 testing was conducted with the actual secondary waste products from pretreatment studies on actual waste while testing on C-104 material was conducted with simulated secondary waste products. This section provides details on the synthesis of the simulated secondary waste products.

2.1.1 Cs Eluant Simulant

The Cs eluant simulant composition was generated based on the concentrations of materials as reported in, "Estimation Of Physical Properties Of Tank 241-AN-107 Cesium And Technetium Eluate Concentrate Blend" by Alexander S. Choi, Savannah River Technology Center. In the document's appendix the evaporated Cs eluant speciation is described in terms of moles of component generated per hour. Using this information a simulant spreadsheet was created where the individual components reported (metals, anions, and water) were summed to give the total amount of moles for each of the individual metals, anions, and the total water generated per hour. To compose the simulant, it was assumed initially that the bulk of metals would be introduced as nitrate salts, the total acid concentration would be generated by nitric acid and HCl, and the total chloride would be supplied solely through the addition of HCl. A later check on the total amount of anions introduced by this assumption agreed well with the total amounts present in the spreadsheet. In the actual simulant preparation, the total amounts of each component needed then were scaled so that ca. 100 to 150 mLs of total solution would be prepared (1/40th of the per hour spreadsheet amount). Table 2.1 summarizes the individual components needed and the quantities actually added.

Table 2.1. Components in Evaporated Cs Eluant Simulant

Component	Species	Source	Targeted Amount (g)	Added Amount (g)
Al(NO ₃) ₃ -9H ₂ O	Al	Baker Analyzed	3.19	3.20
H ₃ BO ₃	В	Spectrum Chemical	1.69	1.69
Ca(NO ₃) ₂ -4H ₂ O	Ca	Aldrich ACS Reagent	0.454	0.457
Na ₂ CrO ₄ -2H ₂ O	Cr	Baker	0.368	0.370
Cs(NO ₃)	Cs	Research Chemicals	0.499	0.500
Cu(NO ₃) ₂ -2.5H ₂ O	Cu	Aldrich ACS Reagent	0.488	0.485
Fe(NO ₃) ₃ -9H ₂ O	Fe	Fisher	3.47	3.47
HNO ₃ (conc.)	Н	Fisher Certified ACS Plus	17*	17*
KNO ₃	K	Mallinckrodt	0.621	0.621
Mn(NO ₃) ₂ (50% aqueous solution)	Mn	Baker Analyzed	2.16**	2.16**
NaNO ₃	Na	Aldrich ACS Reagent	26.2	26.2
Ni(NO ₃) ₂ -6H ₂ O	Ni	Aldrich	13.3	13.3
Pb(NO ₃) ₂	Pb	Baker Analyzed	0.105	0.110
Na ₂ SiO ₃ -9H ₂ O	Si	Baker	0.904	0.906
UO ₂ (NO ₃) ₂ -6H ₂ O	U	Alfa Ventron	3.25	3.30
HCl (conc.)	Cl	Fisher Certified ACS Plus	1.23*	1.23*

^{*} mL of concentrated acid

With the exception of uranyl nitrate, the individual amounts of all the listed solid sources were placed in a 250 mL glass beaker (wt. = 118.57 grams) together with a magnetic stirring bar (wt. = 4.500 grams). The appropriate amount of the 50% Mn(NO₃)₂ solution was added by pipette along with approximately 150 mL of deionized water. Most of the solids dissolved. The concentrated acids were then added to the stirring suspension by pipette yielding a clear solution. The solution was stirred overnight at room temperature and transferred to a radiological fume hood where the uranyl nitrate solid was added. The uranyl nitrate quickly dissolved. The solution was heated and concentrated until just over 100 mL total volume. The beaker was weighed at this point and a small amount of water added until the weight of the simulant approached the targeted weight of 142 g (measured weight = 118.57 + 4.50 + 142 = 265.07 grams). The solution was stirred overnight and allowed to cool to room temperature. The final dark green solution was reweighed the following morning and gave a total solution weight of 264.2 grams.

^{**} mLs of 50% aqueous solution

One mL aliquots of the simulant were weighted to determine the simulant's density. The results are shown in Table 2.2. The DI water control indicates that the pipette was delivering as much as 1% high so a 1% uncertainty probably should be associated with the density of 1.372 g/mL for the simulant. Finally, the simulant (stir bar and all) was transferred to a capped 250 mL polypropylene bottle for storage.

Table 2.2.	Density N	1easurements	for S	Simulant	Solution
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Aliquot number	Weight of 1 mL	Weight of 1 mL
	aliquot of DI water	aliquot of simulant
1	1.010	1.372
2	1.010	1.373
3	1.005	1.372
4	1.004	-
Ave.	1.007 ± 0.003	1.372

2.1.2 Sr/TRU Precipitate Simulant

The simulated Sr/TRU precipitate was prepared using an AN-107 filtrate simulant created during the Savannah River Technical Center (SRTC) pilot scale testing. The Sr/TRU precipitate was prepared under Test Instruction 29953-082 contained in Appendix C. Table 2.3 lists compositional data from Test Instruction 29953-082 for the AN-107 filtrate simulant obtained from SRTC.

During pilot scale testing at SRTC, the waste was treated with $Sr(NO_3)_2$ and $NaMnO_4$. The resulting precipitate was filtered to remove the solids. A volume of 7.7 L of this AN-107 filtrate simulant was transferred to a reaction vessel at Battelle. To return the material to the original composition, $Fe(NO_3)_3$, $Ca(NO_3)_2$, $Cr(NO_3)_3$, $MnCl_2$, and $Pb(NO_3)_2$ were added. While stirring, 600 mL of 1.0 M $Sr(NO_3)_2$ were added at a rate of 60 mL per minute. Five minutes after the $Sr(NO_3)_2$ addition, 400 mL of 1 M $NaMnO_4$ solution was added at rate of 40 mL per minute. The new solution was stirred for 30 minutes then heated to $50 \pm 5^{\circ}C$ over a period of 1 hour. The solution was then stirred at $50^{\circ}C$ for 4 hours. The solution was cooled to $25^{\circ}C$ and then filtered. The solids were then washed seven times with ~ 500 ml of 0.01 M NaOH.

The resulting filtered solids were used as the Sr/TRU Precipitate simulant for rheology testing. Approximately 1200 g of filtered solids were collected. Subsamples (SM-05 and SM-06) were dried at 105°C to determine wt% water. The subsamples SM-05 and SM-06 were found to be 63.4 and 64.0 wt% water respectively. These dried subsamples were then submitted for ICP analysis using an acid digestion to dissolve the solids. Table 2.4 lists the compositional results from the ICP analysis.

Table 2.3 Compositional Data on AN-107 Filtrate Simulant

Analyte	Test 1	Test 2	Units
рН	14	14	N/A
Density	1.272	1.270	kg/L
Al	220	219	mg/L
В	20.8	21.1	mg/L
Ba	< 0.02	< 0.02	mg/L
Ca	124	128	mg/L
Cd	< 0.02	< 0.02	mg/L
C1	1188	1229	mg/L
Co	< 0.05	< 0.05	mg/L
Cr	0.49	0.53	mg/L
Cu	9.2	12.1	mg/L
F	347	360	mg/L
Fe	35	41	mg/L
K	1553	1523	mg/L
La	1.3	1.2	mg/L
Li	< 0.7	< 0.7	mg/L
Mg	0.41	0.41	mg/L
Mn	9.4	14.5	mg/L
Mo	20.3	20.5	mg/L
Na	127500	126500	mg/L
Ni	283	285	mg/L
P	318	319	mg/L
Pb	<1.0	<1.0	mg/L
Si	10.2	11.0	mg/L
Sn	< 0.4	< 0.4	mg/L
Sr	87	95	mg/L
Ti	< 0.05	< 0.05	mg/L
V	< 0.12	< 0.12	mg/L
Zn	17	17	mg/L
Zr	0.85	0.79	mg/L
TIC	15320	15699.74	mg/L
TOC	12234	12542.52	mg/L
Formate	5591	5820	mg/L
Nitrate	130202	131115	mg/L
Nitrite	34089	37431	mg/L
Oxalate	2024	1449	mg/L
Phosphate	1534	1549	mg/L
Sulfate	4830	4883	mg/L

Table 2.4. Sr/TRU Precipitate Simulant ICP Results for Dried Solids from Subsamples SM-05 and SM-06. Results are in μg/g of Dried Solids

Analyte	SM-05	SM-06	SM-06 Duplicate	Average
Ca	3.3E+03	3.4E+03	3.4E+03	3.4E+03
Cr	5.8E+02	5.9E+02	6.0E+02	5.9E+02
Fe	2.6E+04	2.7E+04	2.7E+04	2.7E+04
Mn	1.6E+05	1.6E+05	1.6E+05	1.6E+05
Na	3.6E+04	4.0E+04	4.0E+04	3.9E+04
P	7.3E+02	6.5E+02	7.5E+02	7.1E+02
Pb	1.2E+03	1.1E+03	1.2E+03	1.2E+03
Sr	3.9E+05	4.0E+05	3.9E+05	3.9E+05

2.2 Evaporation and Settling Study

The actual waste samples used in this testing were prepared under conditions similar to those anticipated in the River Protection Project Waste Treatment Plant flow sheet. Both the AZ-102 and C-104 wastes were received for this task following ultrafiltration, caustic leaching and solids washing steps.

The AZ-102 feed was received for this task containing 9.54 wt% solids. At this solids concentration, no standing liquid was observed in the AZ-102 feed. The C-104 feed was received with 20 wt% solids and contained roughly 15 vol% supernatant liquid. Following receipt, each waste was partitioned into four subsamples. Three of the subsamples were adjusted to the target solids concentrations (5 wt%, 15 wt%, and 25 wt%) and the fourth was retained for the mixing/aging study. The AZ-102 5 wt%, C-104 5 wt% and 15 wt% solids samples were prepared by diluting with deionized water. The remaining samples were initially concentrated by decanting standing liquid. Additional water was later evaporated by flowing air over the sample surface at ambient temperature.

Following the evaporation step, the samples were hand stirred with a spatula and subsamples were transferred in duplicate to 10 ml graduated centrifuge cones. Additional subsamples were removed for rheological testing. The rheological testing is described later in this report. The cones were agitated and allowed to settle for 3 days at ambient hot cell temperature (nominally 34°C). During this settling period, the volume of settled solids was recorded as a function of time. The total mass and volume was also recorded and used to calculate the density of the bulk slurries at 34°C. The samples were then transferred to an oven at 50°C for ~12 hours. The cones were then agitated and returned to the oven and allowed to settle for an additional 3 days. During this settling period, the volume of settled solids was recorded as a function of time. The total mass and volume was also recorded and used to calculate the density of the bulk slurries at 50°C.

The material in the centrifuge cones was then returned to the respective bottles along with material used in rheological testing. In most cases deionized water was used to aid the transfer. The samples were then readjusted to the respective solids contents (5, 15 and 25 wt%) by decanting and evaporation using a flow of ambient air. Simulated secondary waste products were added to the samples as detailed in Appendix A to Test Plan 29953-073 contained in Appendix B. The masses of the samples of secondary waste products are listed in Table 2.5. The samples were then stirred using an overhead mixer for approximately 30 minutes. A four bladed impeller, 3.8 cm in diameter, was used at a rotational rate of ~8000 RPM.

Following secondary waste product addition to the C-104 samples, subsamples were transferred in duplicate to 10 ml graduated centrifuge cones. Additional subsamples were removed for rheological testing. The cones were agitated and allowed to settle for 3 days at ambient hot cell temperature (nominally 34°C). During this settling period, the volume of settled solids was recorded as a function of time. The samples were then transferred to an oven at 50°C for \sim 12 hours. The cones were then agitated and returned to the oven and allowed to settle for an additional 3 days. During this settling period, the volume of settled solids was recorded as a function of time. The samples were then cooled to ambient temperature and centrifuged for approximately 10 minutes at \sim 1000 times the force of gravity (1000 x g). The total mass and volume were then recorded and used to calculate the density of the bulk slurries at 34°C. The samples where then placed in an oven at 50°C for approximately 12 hours and the density measurements were repeated.

The material in the centrifuge cones (AZ-102 evaporated feeds, and C-104 evaporated feeds with secondary waste products) were then returned to the respective sample bottles using water to aid in the transfer. Material from rheological testing was also returned to the respective bottles. Given the presence of dissolved solids in the secondary wastes, excess supernatant was not decanted from the C-104 feeds. The C-104 samples were readjusted to their appropriate water contents though evaporation by passing a flow of air over their surfaces. The AZ-102 feeds were readjusted to their appropriate water contents though decanting and evaporation. Glass formers were added to the samples as detailed in Appendix A to Test Plan 29953-073 contained in Appendix B. The mass of the evaporated slurries (before addition of secondary waste products) and mass of glass formers are listed in Table 2.6 and Table 2.7 for AZ-102 and C-104 samples respectively. The samples were then stirred using an overhead mixer for approximately 15 minutes. A four bladed impeller, 3.8 cm in diameter, was used at a rotational rate of ~8000 RPM.

Given the high viscosity and yield point for the AZ-102 25 wt% sample, glass formers were not added to this sample. Instead, the AZ-102 25 wt% sample was diluted to 20wt% solids, and the rheology of this new concentration was examined at 25°C.

Following glass former addition, subsamples of both C-104 (5, 15 and 25 wt%) and AZ-102 feeds (5 and 15 wt% only) were transferred in duplicate to 10 ml graduated centrifuge cones. Additional subsamples were removed for rheological testing. The cones were agitated and allowed to settle for 3 days at ambient hot cell temperature (nominally 34°C). During this settling period, the volume of settled solids was recorded as a function of time. The samples were then transferred to an oven at 50°C for \sim 12 hours. The cones were then agitated and returned to the oven and allowed to settle for an additional 3 days. During this settling period, the volume of settled solids was recorded as a function of time. The samples were then cooled to ambient temperature and centrifuged for approximately 10 minutes at \sim 1000 times the force of gravity (1000 x g). The total mass and volume were then recorded and used to calculate the density of the bulk slurries at 34°C. The samples where then placed in an oven at 50°C for approximately 12 hours and the density measurements were repeated.

Glass formulations in this report for AW-101 and AN-107 are considered to be proprietary by VSL/Duratek

Table 2.5. Mass of Samples and Secondary Waste Products For C-104 Tests

Secondary Waste	5 wt%	15 wt%	25 wt%
Slurry Mass (g)	102.7	68.1	68.0
Simulated Sr/TRU (g)	6.1	12.3	20.3
Simulated Cs Eluant (g)	0.74	1.44	2.45

Table 2.6. Mass of Samples, Glass Formers and Secondary Waste in Grams Added to AZ-102 Samples. Sample 15 wt%-2 Was Used for Mixing and Aging Study

Sample	5 wt%	15 wt%	15 wt%-2
Slurry Mass	79.83	77.59	86.70
Sr/TRU Precipitate (25 wt% solids basis)	1.841	5.367	5.997
Na ₂ B ₄ O ₇ +10H ₂ O	1.031	3.01	3.359
LiOH+H ₂ O	1.486	4.33	4.842
Na ₂ SiO ₃ +5H ₂ O	3.075	8.96	10.017
SiO ₂ (Sil-co-Sil 75)	3.807	11.1	12.402
Sugar (Granular)	0.128	0.374	0.418

Glass formulations in this report for AW-101 and AN-107 are considered to be proprietary by VSL/Duratek

Table 2.7. Mass of Samples and Glass Formers Added to C-104 Samples

Sample	5 wt%	15 wt%	25 wt%-1	25 wt%-2
Slurry Mass (g)	102.7	68.1	68.0	68.2
Sr/TRU Precipitate Simulant (26.8 Wt% Solids Basis)	6.1	12.3	20.3	20.5
Cs Eluant Simulant	0.737	1.436	2.451	NA
Na ₂ B ₄ O ₇ +10H ₂ O	3.723	7.406	12.325	12.361
LiOH+H ₂ O	2.362	4.699	7.820	7.843
Na ₂ CO ₃	0.226	0.450	0.749	0.751
SiO ₂ (Sil-co-Sil 75)	7.463	14.848	24.710	24.782
ZnO (KADOX-920)	0.316	0.630	1.048	1.051

NA, Cs Eluant not added to C-104-25-2

2.3 Shear Stress Versus Shear Rate Analysis (Rheology)

As described in Section 2.2, shear stress versus shear rate analyses were conducted on the evaporated feeds as well as following addition of secondary waste products and glass formers. These measurements were conducted at 25°C and 50°C using a Haake M5. The M5 head was modified for operation in a high radiation field by relocating the printed circuit boards from the head to a remote box as well as extending the signal cables and adding a secondary heat exchanger to the recirculating loop. Other minor modifications were made to the water jacket and measuring sensors to aid in operations using master-slave manipulators.

Measurements were made using an SV I sensor. The recommended range for this sensor is from 300 to 100,000 cP with a maximum torque of 1240 Pa and a maximum shear rate of 445 s⁻¹. This was found to be an appropriate sensor for the 15 and 25 wt% samples, but was not sensitive enough for some of the 5 wt% samples. However, the SV I was used for all samples since there was insufficient material available to use the more sensitive MV sensors. The SV I requires approximately 10 ml while the MV I requires 40 ml.

During this work a 95.5 cP Brookfield viscosity standard was used to check the calibration of the instrument. Calibration checks were performed a minimum of once a month when the instrument was in use. All calibration checks were within 10% of the certified value.

Shear stress versus shear rate rheograms were obtained by measuring the shear stress produced at a specific shear rate. The increasing shear rate curve was generated by gradually increasing the shear rate from 0 to 300 s⁻¹ over a 2 minute period. The decreasing shear rate curve was then

generated by reducing the shear rate back down to 0 s⁻¹ over 2 minutes. The shear rate analysis was conducted again at least once with the same sample still in the instrument. A difference between duplicate runs would indicate potentially unusual behavior in the samples including (but not limited to) settling of the solids within the instrument, the sample being effected by shearing in the instrument, or water loss through evaporation.

2.4 Mixing and Aging Study

As described in Section 2.2, the initial AZ-102 and C-104 material received for this work were each partitioned into 4 subsamples. Three of the subsamples were used for evaporation and settling studies while one sample from each tank was retained for the mixing and aging studies. The retained AZ-102 sample was adjusted to 20 wt% solids and subjected to a shear stress versus shear rate test prior to the mixing and aging study. The C-104 sample was not subjected to any testing prior to the mixing and aging study.

The AZ-102 sample was diluted from 20wt% solids to the 15 wt% using deionized water. The C-104 sample was evaporated to 25 wt% solids. Both samples were then placed in 250 ml round bottom flasks with side tubes.

Both samples were stirred using an overhead mixer while glass formers were added to the AZ-102 sample, and glass formers and secondary waste products were added to the C-104 sample. The flasks were then sealed using a Teflon stirrer bearing. The sample was then continually stirred for 1 week using a 1-inch (2.54 cm) diameter blade at approximately 400 rpm. The rate of the mixer was checked approximately every day and adjusted as needed to maintain the rate of 400 rpm. The volume of the slurries was approximately 6.1 in³ (100 ml). The 400 rpm mixing rate provides roughly the same energy per volume as anticipated in the River Protection Project Waste Treatment Plant. The following equation (provided by BNFL) was used to calculate the proper rotational rate:

$$N^3 = 1.85 \times 10^7 \text{ V/D}_i^5$$

For this equation, N is the impeller rotational rate in rpm, V is the sample volume in cubic inches and D_i is the impeller diameter in inches.

Samples of each of the slurries were removed from the mixing vessel after 1 hour, 1 day and 1 week. These samples were immediately analyzed for shear stress versus shear rate at 25°C. These analyses were conducted as described in section 2.3.

After one week of mixing, the AZ-102 and C-104 slurries were transferred to graduated glass jars. The sample was left to settle undisturbed for 1 week. During the settling time, the samples were monitored for any gas retention and releases. Visual observations were supplemented with time lapse video. No gas bubbles were observed in these samples during this study.

After one week of settling, the standing liquid was removed from the slurries, and the settled solids were immediately analyzed for shear stress versus shear rate at 25°C. As described in section 2.3, the analyses were conducted by increasing the shear rate from 0 to 300 s⁻¹ over 2 minutes generating the increasing shear rate curve, and then back down to 0 s⁻¹ over 2 minutes generating the decreasing curve.

3.0 Experimental Results

This section details the results of tests conducted on actual AZ-102 and C-104 samples following adjusting to target feeds with solids concentrations of 5, 15, and 25 wt%. The initial AZ-102 and C-104 feeds were 9.54 and 20 wt% solids respectively. The feeds were adjusted to the targets using a combination of decanting supernatant liquid, evaporation at ambient temperature (~34°), and addition of deionized water. Following addition of secondary waste products and glass formers the resulting melter feed slurries had a higher solids content. However, in this report, samples will be referred to according to the target solids content for the evaporated feed (e.g. the feed evaporated to 25 wt% solids is still referred to as the 25 wt% solids slurry even after the addition of dry glass formers).

3.1 Density and Settling Study

The densities of the evaporated samples, samples with secondary waste products and, samples following the addition of glass formers are provided in Table 3.1.

As expected, the densities of the initial feeds prior to glass former or secondary waste product additions increase with increasing sample concentration and decreases very slightly with temperature. No temperature trend is seen in the C-104 samples following secondary waste product additions. No significant temperature trends are seen in either the AZ-102 or C-104 samples following glass former additions. For untreated Hanford tank waste slurries, temperature related density trends are usually observed and are the result of solids dissolution. The lack of temperature trends suggests that there is no significant solids dissolution occurring between 34 and 50°C. This is not surprising since the AZ-102 and C-104 solids were washed and leached prior to this feed testing.

As described in Section 2.2, the graduated centrifuge cones were agitated and then allowed to settle at ambient (approximately 34°C) and 50°C over a 2 to 3 day period. Due to the Hanford brush fire during the week of June 25, 2000, the settling study on the C-104 samples with glass formers was terminated after 30 hours.

For most samples, the solids settled leaving a clear supernatant above with a distinct interface between the settling solids and the clarified supernatant. The level of this interface in the graduated centrifuge cone was measured as the volume of settled solids and divided by the total sample volume to calculate the volume percent (vol%) settled solids. Table 3.2 lists the vol% settled solids for the samples in this study. The 15 and 25 wt% AZ-102 samples were not examined since these samples did not settle to form a standing liquid layer after one week undisturbed in the primary sample jars. The standing liquid in the 5 wt% C-104 evaporated feed did not clarify over the three days of settling and an accurate measure at 34°C could not be made. At 50°C, a settled solids layer at ~8 vol% was observed for these duplicate samples.

Table 3.1. Density of AN-107 and AW-101 Samples at 25°C and 50°C With and Without Addition of Glass Formers in g/ml.

		Evapora	ted Feed		condary ste ^b		Glass ners ^a
Feed	Sample	34°C	50°C	34°C	50°C	34°C	50°C
5 wt% AZ-102	Primary	1.03	1.02	NM	NM	1.08	1.06
	Duplicate	1.05	1.04	NM	NM	1.09	1.08
	Average	1.04	1.03	NM	NM	1.09	1.07
	Relative % Difference	2%	2%	NM	NM	1%	2%
15 wt% AZ-102	Primary	1.15	1.11	NM	NM	1.23	1.23
	Duplicate	1.13	1.12	NM	NM	1.22	1.22
	Average	1.14	1.12	NM	NM	1.23	1.23
	Relative % Difference	2%	1%	NM	NM	1%	1%
25 wt% AZ-102	Primary	1.26	1.20	NM	NM	NM	NM
	Duplicate	1.22	1.23	NM	NM	NM	NM
	Average	1.24	1.22	NM	NM	NM	NM
	Relative % Difference	3%	2%	NM	NM	NM	NM
5 wt% C-104	Primary	0.99	0.99	1.01	1.01	1.09	1.08
	Duplicate	0.99	0.99	1.01	1.01	1.07	1.07
	Average	0.99	0.99	1.01	1.01	1.08	1.07
	Relative % Difference	1%	1%	0%	0%	2%	0
15 wt% C-104	Primary	1.04	1.02	1.12	1.12	1.30	1.27
	Duplicate	1.06	1.06	1.10	1.10	1.33	1.27
	Average	1.05	1.04	1.11	1.11	1.32	1.27
	Relative % Difference	2%	4%	2%	2%	2%	0
25 wt% C-104	Primary	1.10	1.08	1.20	1.20	1.41	1.40
	Duplicate	1.14	1.12	1.17	1.17	1.41	1.40
	Average	1.12	1.10	1.19	1.19	1.41	1.40
	Relative % Difference	4%	4%	3%	3%	0%	0
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a. C-104 density measurements made after addition of secondary waste products and glass formers

b. secondary waste products were not added to AZ-102 slurries

Table 3.2. Volume Percent Settles Solids for the AZ-102 Samples

	Sample	Evaporated Feed		With Secondary Waste		With Glass Formers ^a	
Feed		34°C	50°C	34°C	50°C	34°C	50°C
5 wt% AZ-102	Primary	58	60	NM	NM	49	59
	Duplicate	56	62	NM	NM	51	58
	Average	57	61	NM	NM	50	58.5
	Relative % Difference	4%	3%	NM	NM	4%	2%
5 wt% C-104	Primary	50 ^b	7.6	19	24	26	32°
	Duplicate	48 ^b	8.3	19	22	24	31 °
	Average	49 ^b	7.95	19	23	25	31.5 °
	Relative % Difference	4%	9%	0%	9%	8%	3%
15 wt% C-104	Primary	67	73	76	82	80	89°
	Duplicate	69	78	71	77	79	88°
	Average	68	75.5	73.5	79.5	79.5	88.5 °
	Relative % Difference	3%	7%	7%	6%	1%	1%
25 wt% C-104	Primary	92	94	NM	NM	NM	NM
	Duplicate	93	99	NM	NM	NM	NM
	Average	92.5	96.5	NM	NM	NM	NM
	Relative % Difference	1%	5%	NM	NM : f	NM	NM

a. C-104 Glass formers were added to C-104 samples after addition of secondary waste products

b. Incorrect interface measured due to cloudy supernatant layer. Supernatant in 5 wt% C-104 initial feed samples did not clear after 3 days of settling

c. Only allowed to settle for 30 hours. Slope of settling curves (Figure 3.13) strongly suggest final vol% settled solids at 50°C would have been higher than at 34°C.

Surprisingly for every sample examined, the samples at 50°C did not compact as well as the same samples at 34°C. The trend of increasing settled solids volume with temperature was between 4 and 8 vol%. This is probably the result of the test methodology. The cones were loaded and agitated prior to the 34°C study. The samples were then allowed to settle, and then the cones were agitated again before the 50°C study. This agitation probably broke some of the aggregate structure in the settled solids resulting in a slightly looser settled solids volume. This is supported by shear stress versus shear rate tests in which the viscosity of the slurries decrease over duplicate analyses with the same sample. Future settling studies should include a repeat of the 34°C settling study after the 50°C test to confirm this behavior.

For the AW-101 and AN-107 low activity waste (LAW) samples reported in a previous study (Bredt and Swoboda, 2000) the 50°C tests contained a smaller vol% settled solids compared to the duplicates at 25°C. This trend of decreasing vol% settled solids with increasing temperature for the LAW samples was attributed to either the dissolution of soluble species leading to a lower volume of solids or a decrease in the viscosity and yield stress resulting in greater compaction of the solids. These factors should not affect the C-104 and AZ-102 wastes since these feeds contain little to no soluble solids and no significant change in viscosity or yield stress was observed between 34 and 50°C.

As expected, the data shows the vol% settled solids increased with solids content. The vol% settled solids increased with increasing solids contents in the evaporated feeds (5 wt% < 15 wt% < 25 wt%), and the vol% settled solids increased with the addition of solids from secondary waste products and glass formers. This trend is not surprising since the initial tank solids and Sr/TRU secondary waste products were rinsed during previous testing, removing soluble solids. In addition, all of the glass formers with the exception of sugar and boric acid are highly insoluble.

Figure 3.1 and 3.2 plots the vol% settled solids (interface height/sample height x 100%) versus time for the 5 wt% AZ-102 evaporated feed. Figure 3.1 uses a linear scale while Figure 3.2 is semi-log scale. The linear scale is provided to show stability in the final vol% settled solids while the semi-log scale is useful for examining the behavior over the first few hours. Both duplicates reached a stable settled solids layer at 34 and 50°C within approximately 30 hours. Figure 3.3 plots the settling rate as a function of time using a log scale. The settling rate was calculated by dividing the change in settled solids height by time. Minor parallax errors can be magnified by this calculation and result in significant scatter. To minimize scatter the data plotted in Figure 3.3 have been smoothed using a four point moving average.

Three settling mechanisms are generally observed for this type of sample matrix: free settling, hindered settling, and compression settling. Free settling is settling of discrete particles or flocculated particles without interaction from other particles or the wall. Free settling is denoted by a linear decrease in vol% settled solids over time as the particles fall with fixed velocities. Since the settling rate is simply the slope of the vol% settled solids versus time plot time, a linear decrease in settling velocity would be seen as a flat portion of the settling rate versus time plot. For flocculating systems, the velocity generally increases as the mass of the particles increase, although particle shape changes can also decrease the settling velocity. Hindered settling occurs when the when particle-particle and particle-wall interactions effect the settling velocities. In an ideal system, hindered settling is denoted by the break from a linear decrease in vol% settled solids with time (i.e. a decrease in the settling rate). Compression settling is the final portion of the vol% settling curve as the system approaches the stable value. Two or even all three of these mechanisms usually occur simultaneously.

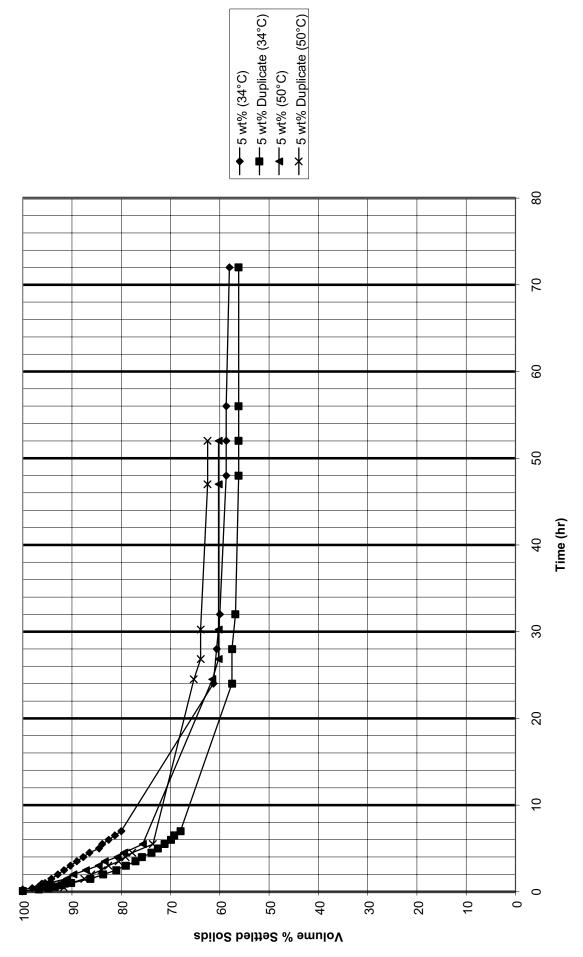


Figure 3.1. Volume Percent Settled Solids Versus Time for AZ-102 Evaporated Feed Using a Linear Scale

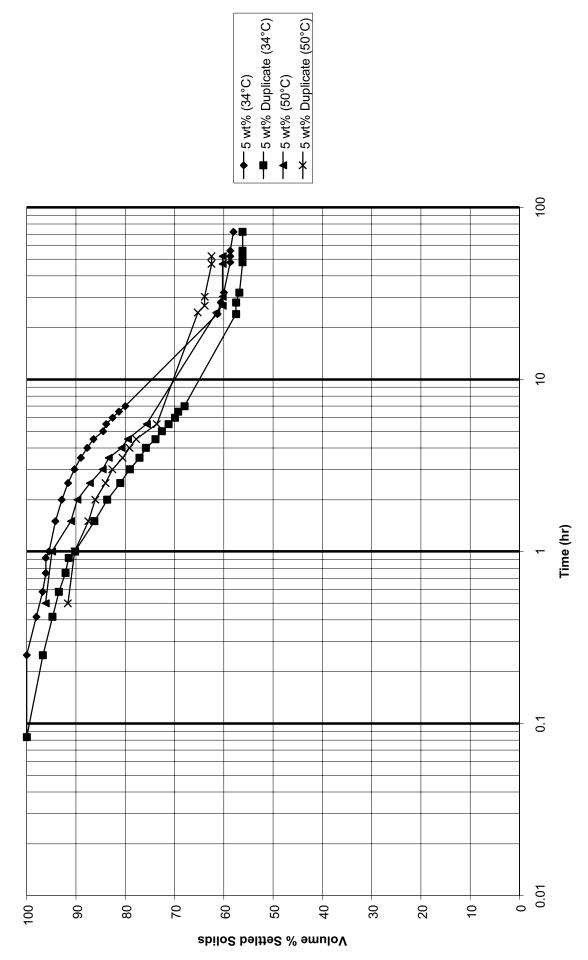


Figure 3.2. Volume Percent Settled Solids Versus Time for AZ-102 Evaporated Feed Using a Semi-Log Scale

The 34°C samples in Figure 3.3 show an initially constant settling rate between 0.001 and 0.004 cm/min for the first 18 minutes. This region was not observed in the samples at 50°C because the 50°C samples were only monitored after 30 minutes of settling. This region with constant settling rate is probably a combination of free as well as some hindered settling. Free settling of the smaller particles is dominating the behavior of the observed solids interface. However, the majority of the solids are at a much higher concentration at the bottom of the column where hindered settling is the dominant mechanism.

After approximately 18 minutes of settling, the settling rate for all of the samples drop steadily as seen in Figure 3.3. This drop indicates the end of any free settling, and a transition to hindered and compression settling. This region of the settling curve is probably a mixture of compression settling and hindered settling. From this settling study it is difficult to determine the transition from the combination of both hindered and compressive settling to only compression settling. This could be possible in future work by use of a microbalance technique in which the solids settle onto a balance pan suspended in the solution.

Figures 3.4 and 3.5 plots the vol% settled solids versus time for the AZ-102 5 wt% samples after glass former addition. Figure 3.6 plots the settling rates versus time. The same initial free settling behavior is seen in the material after glass former addition as before glass former addition. Comparing Figure 3.3 to 3.6 one sees the samples with glass former exhibit constant settling rates for approximately the first 30 minutes, the rate then drops as hindered and compressive settling become the dominant behaviors. The settling rates for the AZ-102 material increases by approximately a factor of four following glass former addition, from between 0.001-0.003 cm/min to 0.005-0.11 cm/min. This shows some flocculation of the AZ-102 sludge particles with the glass formers.

Settling data for the C-104 samples are similarly presented in Figures 3.7 through 3.15. As with the AZ-102 samples, no temperature trends are observed in the C-104 settling rates between 34 and 50°C. Comparing Figures 3.9 and 3.12, one sees addition of secondary waste products greatly increases the initial settling rate. The initial rate for the evaporated feeds (Figure 3.9) are between 0.0004 and 0.004 cm/min. The rates following secondary waste product addition increases by a factor of 10 to between 0.004 and 0.04 cm/minute. This increase is most likely the result of flocculation of the sludge particles with the secondary waste. Most notably, the supernatant in the 5 wt% initial feed remained cloudy throughout the settling period. Following addition of secondary waste, the 5 wt% samples settled with clarified supernatant. Similar high settling rates (between 0.004 and 0.04 cm/minute) were observed for the samples after glass former addition, see Figure 3.15. Since the glass formers were added after secondary waste products, it is not known whether glass formers alone would induce similar flocculation.

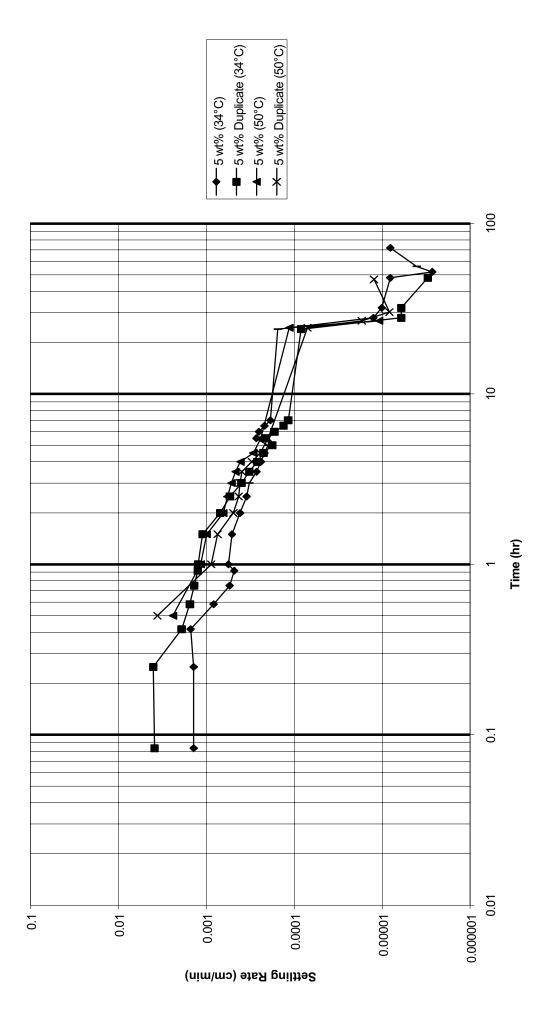


Figure 3.3. Settling Rates for AZ-102 Evaporated Feed

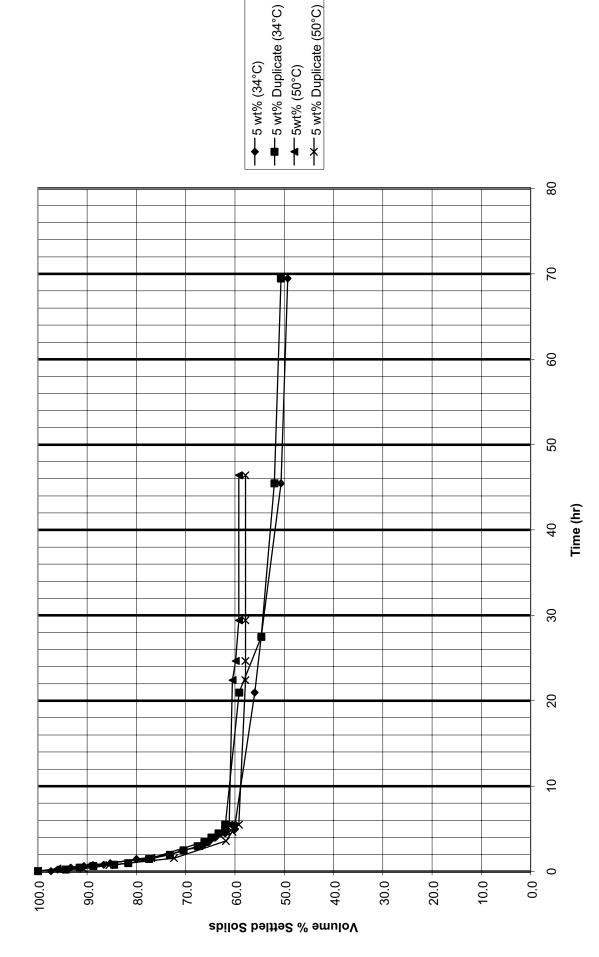


Figure 3.4. Volume Percent Settled Solids Versus Time for AZ-102 Evaporated Feed With Glass Formers Using a Linear Scale

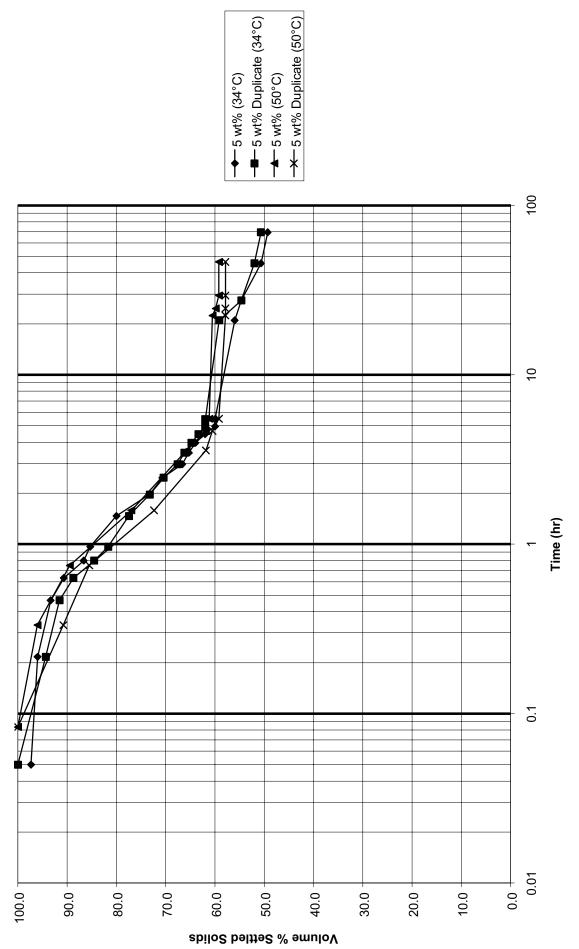
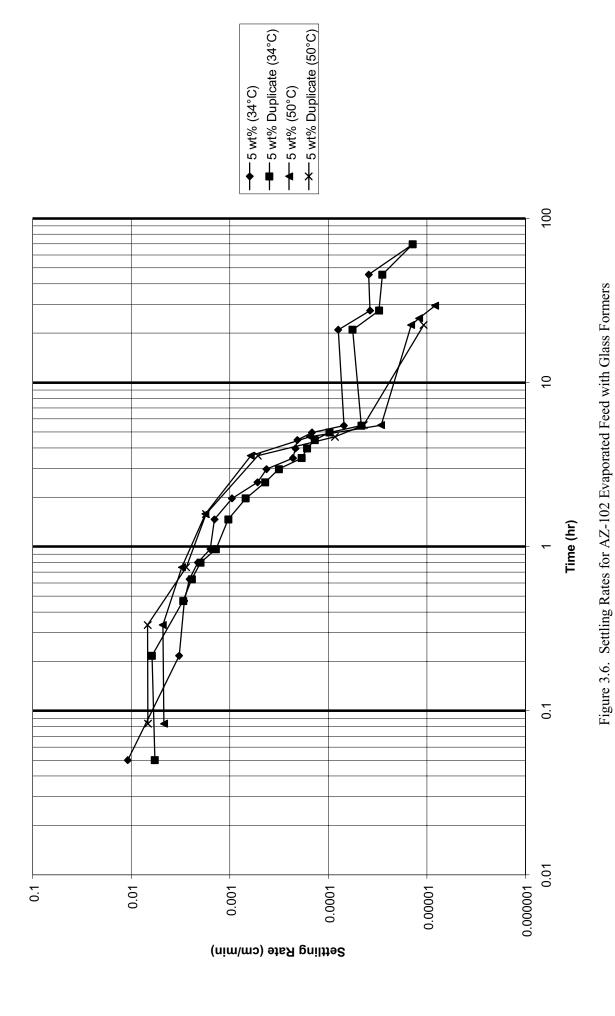


Figure 3.5 Volume Percent Settled Solids Versus Time for AZ-102 Evaporated Feed With Glass Formers Using a Semi-Log Scale



3.11

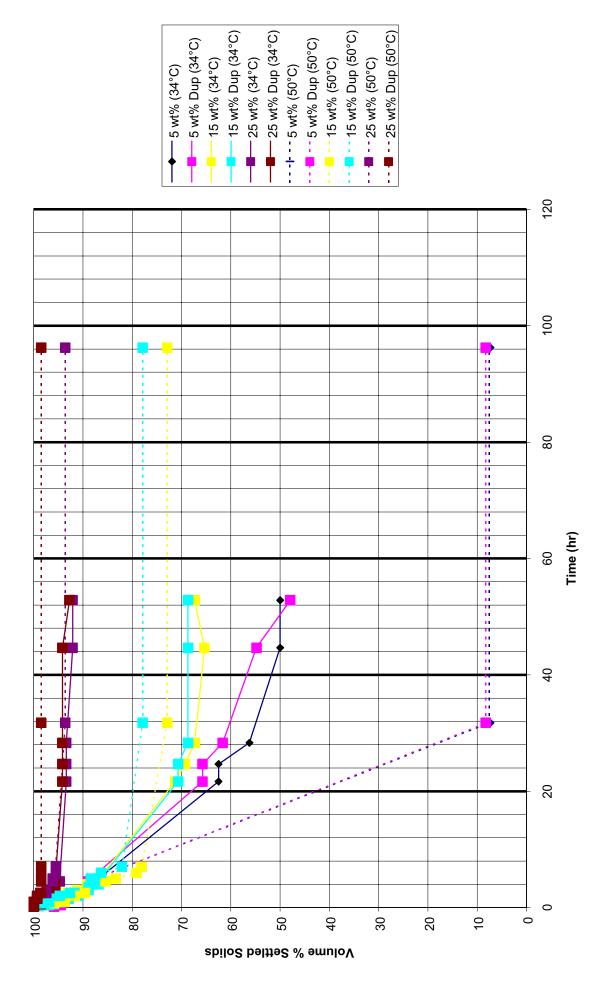


Figure 3.7. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed Using a Linear Scale

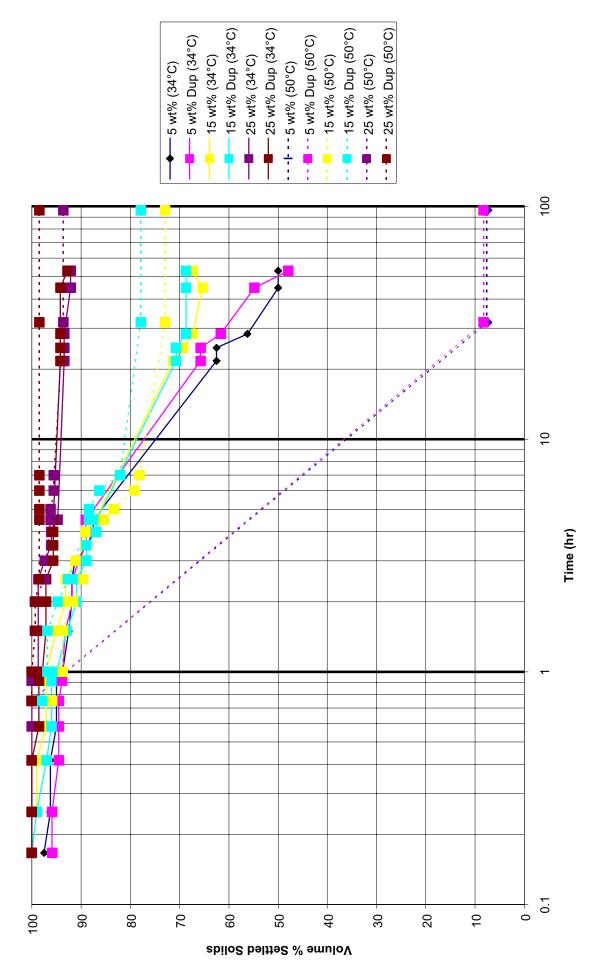


Figure 3.8. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed Using a Semi-Log Scale

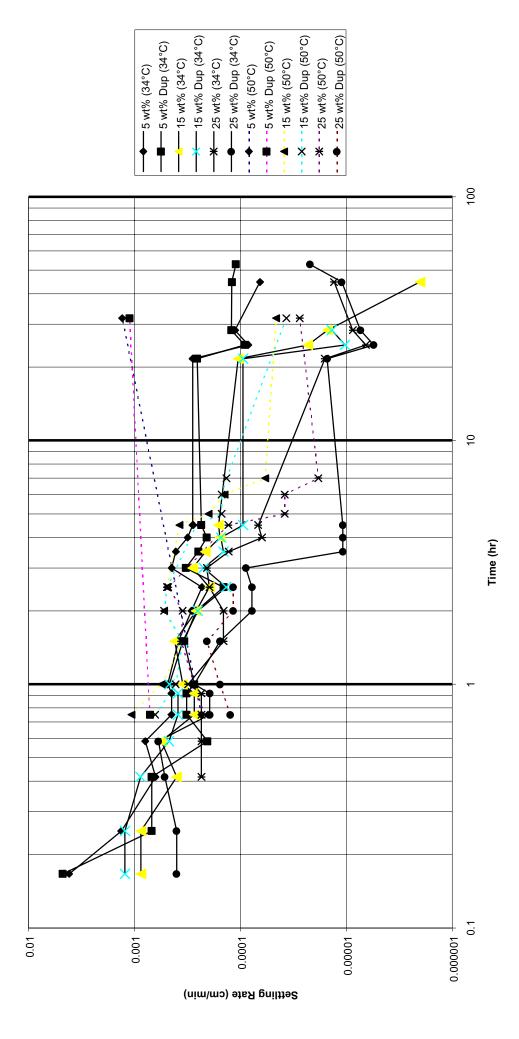


Figure 3.9. Settling Rates for C-104 Evaporated Feed

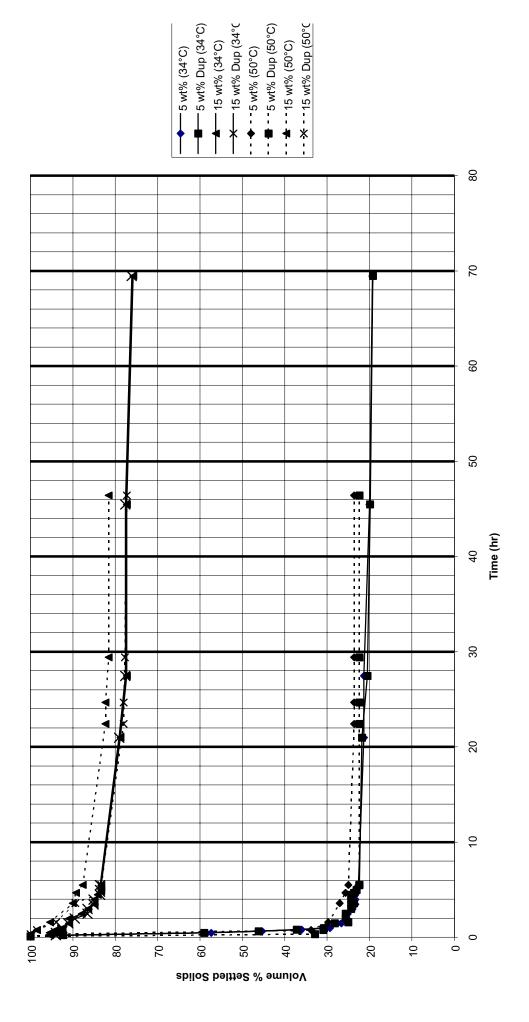


Figure 3.10. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed With Secondary Waste Using a Linear Scale

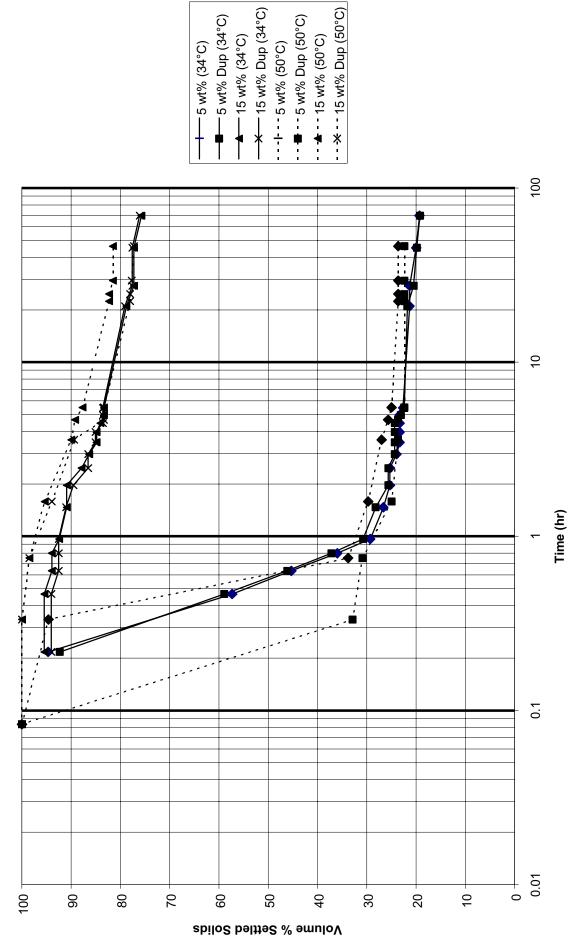


Figure 3.11. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed With Secondary Waste Using a Semi-Log Scale

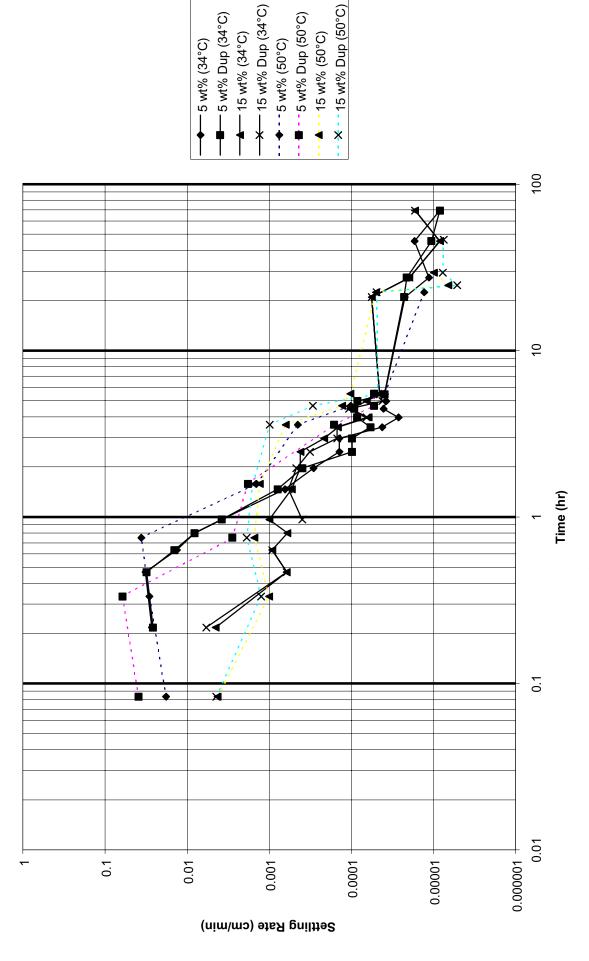


Figure 3.12. Settling Rates for C-104 Evaporated Feed With Secondary Waste Products

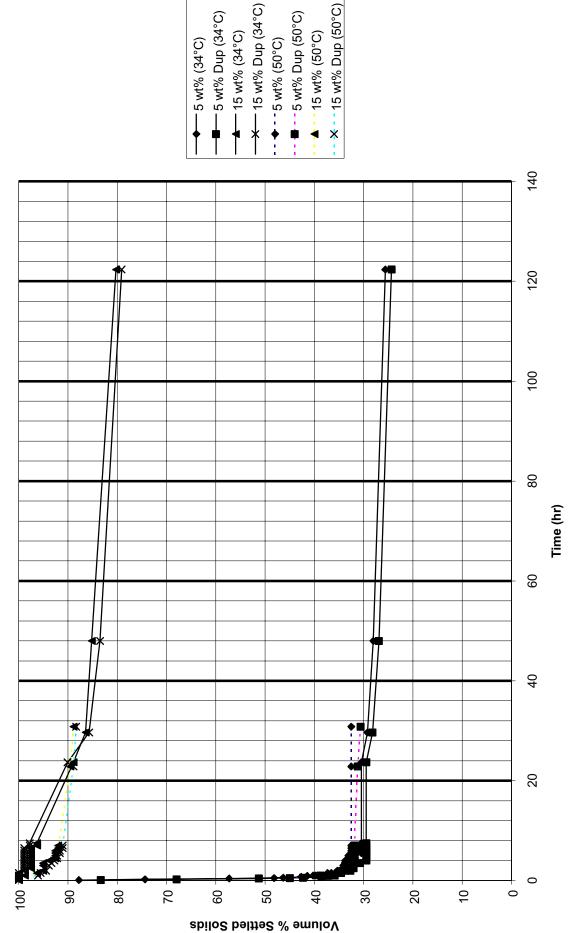


Figure 3.13. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed With Secondary Waste and Glass Formers Using a Linear Scale

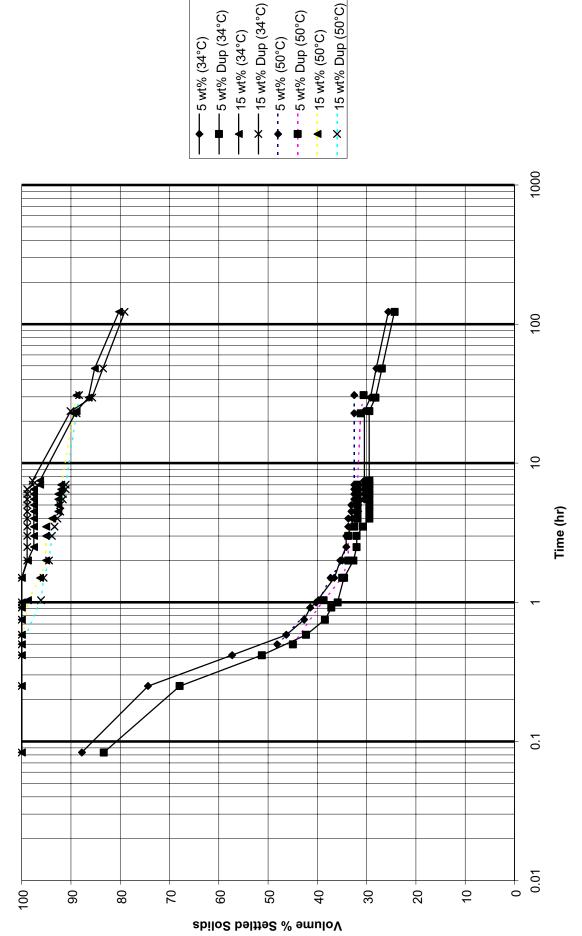


Figure 3.14. Volume Percent Settled Solids Versus Time for C-104 Evaporated Feed With Secondary Waste and Glass Formers Using a Semi-Log Scale

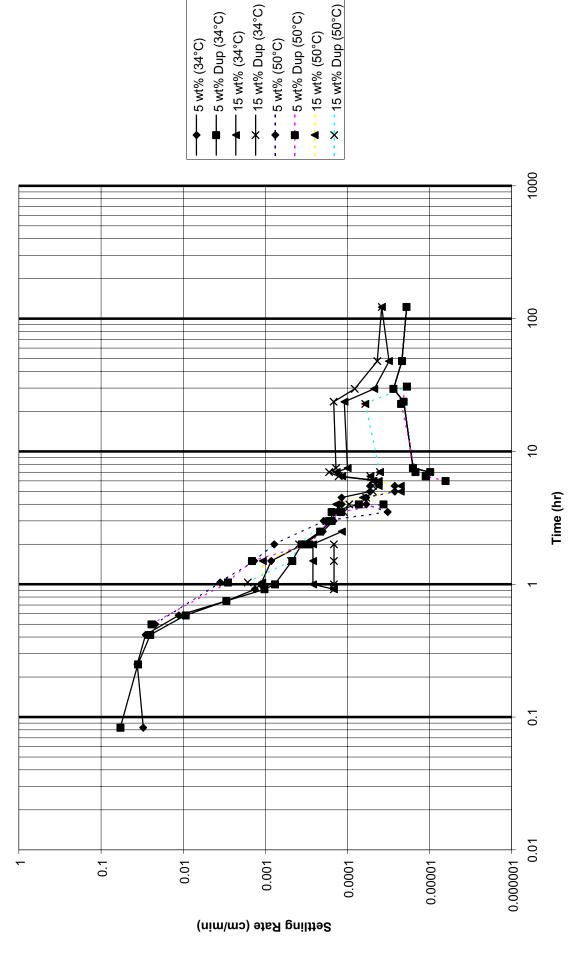


Figure 3.15. Settling Rates for C-104 Evaporated Feed With Secondary Waste Products and Glass Formers

3.2 Rheology

Viscosity is the internal resistance to flow of a fluid against external forces. Viscosity is mathematically defined as the shear stress divided by the shear rate. For a Newtonian fluid this ratio is constant. For non-Newtonian fluids this ratio can change based on flow conditions and shear history. The rheological data most often requested and provided is a rheogram. Rheograms provide flow data over a range of conditions rather than at one point. A rheometer ramps up the shear rate to chosen value while measuring and recording the resulting shear stress. From a rheogram viscosity data, yield stress data and flow curve information are obtained. There are several types flow curves that have been well studied and have defined mathematical curve fits assigned to them. These curve fits are usually used to describe and predict flow behaviors of fluids. The three that best describe most slurries and consequently tank waste are as follows:

Newtonian Equation

Tau = ETA*D

Ostwald Equation (pseudoplastic or power law fluid)

 $Tau = A*D^n$

Herschel-Bulkley Equation (yield pseudoplastic)

 $Tau-Tau(o) = A*D^n$

Tau = Shear Stress ETA = viscosity D = Shear Rate

n = power law factor n=1 fluid is Newtonian

n>1 fluid is dilatant

n<1 fluid is pseudoplastic

A = a coefficient related to flow resistance, similar to apparent viscosity. For Newtonian fluids A=viscosity.

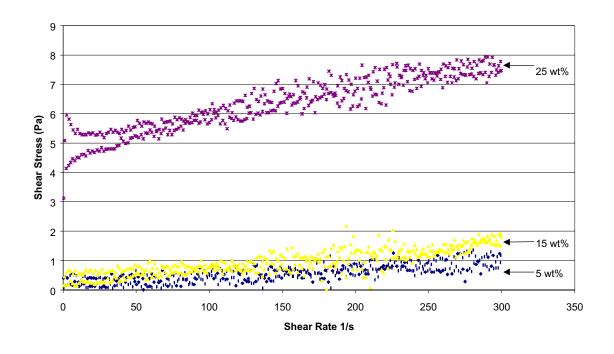
For the C-104 and AZ-102 materials, a standard 0-300 S⁻¹ ramp over 2 minutes was used to collect the increasing shear rate curve immediately followed by a 300-0 S⁻¹ ramp down over 2 minutes to collect the decreasing shear rate curve. Each sample was run at least twice. The pertinent resulting rheograms and viscosity curves are included in either this section or the appendix.

3.2.1 Rheology of Evaporated Feed Samples

C-104 Feed

Shear stress vs. Shear rate curves were obtained for the C-104 waste feed at 5, 15, and 25 wt% concentrations at both 25°C and 50°C.

Rheograms for the feeds at 25°C are presented in Figure 3.16. Yield stresses and viscosities at 33, 150, and 298 S⁻¹ are presented in Table 3.3. The viscosity of the 5 and 15 wt% samples was low, 15 cP or less at 25°C. The material showed predominately Newtonian behavior, with only a slight indication any yield or pseudo-plastic behavior, usually exhibited only during the first analysis. This slight non-newtonianism is most likely due to the fact that at these low viscosities the material being tested is below the recommend range for SV1 sensor utilized to obtain the data. And is therefore probably an artifact of loading stresses and initial startup machine inertia.



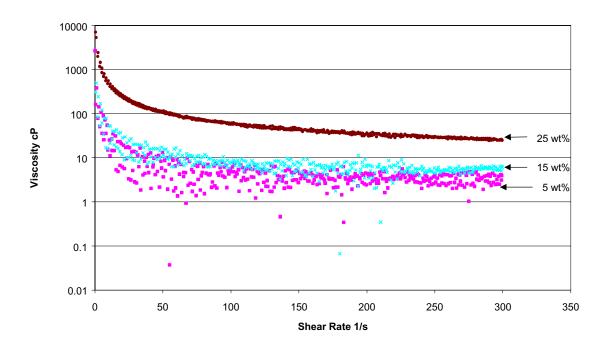


Figure 3.16. Rheograms for C-104 Initial Evaporated Feeds at 25°C

Table 3.3. Viscosity Data for Evaporated Feeds

	25°C				50°C			
Material	Yield ^a (Pa)	$33 s^{-1b}$	150 s^{-1}	298 s ⁻¹ b	Yield ^a (Pa)	$33 S^{-1b}$	150 s^{-1b}	298 s ⁻¹ b
C-104 5 wt%	<1	9.8	5.2	4.7	<1	3.8	4.1	3.2
C-104 15 wt%	<1	15.4	6.2	5.7	<1	14.6	5.4	4.9
C-104 25 wt%	~5	164.9	45.5	25.9	~8	193.8	49.2	26.7
AZ-102 5 wt%	<1	12.1	5.7	5.2	<1	11.7	4.7	4.3
AZ-102 15 wt%	~14	525.2	144.1	78.7	~17	556.2	148.3	81.3
AZ-102 20 wt% ^c	~20	903.8	233.1	128.6	NA	NA	NA	NA
AZ-102 25 wt%	~190	4597.2	1263.5	702.6	NA	NA	NA	NA

- a. Yield data is in Pa and is based on visual estimates from the graph and/or various curve fits. When there is a disparity between multiple runs the highest yield is reported 1 Pa was the limit for quantification.
- b. Viscosity data is in cP and is an average of multiple runs at each shear rate given.
- c. AZ-102 20 wt% data was obtained with new sample from material originally set aside for the mixing study.

The 25 wt% material showed a small yield stress with little pseudo-plastic behavior over the rest of the testing range. It most closely resembles a Bingham Plastic material.

Temperature Effects: The 5 and 15 wt% feeds exhibited large amounts of scatter in the data resulting from use of the SV1 sensor. No temperature effects were measurable within the range of this system.

The 25 wt% material showed an unexpected small rise in viscosity with the increased temperature. This rise is well within the range of error for this system with a change of sample, however since it was consistent it may be a real effect. This effect could also be a result of a small amount of dehydration during testing, even though visually the material did not appear to have dried out. If more material had been available a second sample would have been run at each temperature.

AZ-102 Feed

Shear stress vs. Shear rate curves were obtained for the AZ-102 waste feed at 5, 15, 20, and 25 wt% concentrations at 25°C. Yield stresses and viscosities at 33, 150, and 298 S⁻¹are presented in Table 3.3. Due to limited amounts of sample, only data for 5 and 15 wt% was obtained at 50°C.

The original test plan did not call for a 20 wt% measurement, however since the apparent yield and viscosity for the 25 wt% material greatly exceeded design values for processing, a 20 wt% feed was also tested. In the process of acquiring these data an important discovery was made concerning the nature of AZ-102 feed that may have later played a role in the mixing study. The AZ-102 feed appears to be irreversibly shear sensitive. The longer it is sheared or mixed the lower the apparent viscosity and yield stress may become. This was determined when the 25 wt% material was diluted down to 20 wt% and tested. The 20 wt% material showed a lower apparent viscosity and yield than the 15 wt% material. Since this was counter intuitive, the measurement was repeated two days later with a fresh aliquot from the same 20 wt% bulk sample. This resulted in even lower values. Since the material from the viscometer is returned to the bulk sample after each measurement, the bulk sample gains an increasing shear history. An untouched bottle of AZ-102 feed had been set aside for the mixing study, it was utilized as a source for fresh sample. The 20 wt% material data obtained from fresh material fell within the expected range of yield and viscosity. Thus it is most likely that the previous testing on the

material originally used for the 20 wt% testing was the cause of the anomaly. This leads to the hypothesis that the AZ-102 feed may be irreversibly shear sensitive. This property could be an asset to processing. More testing would need to be done to validate this observation.

Rheograms results for the AZ-102 feeds at 25°C are presented in Figure 3.17 and does not include the highly sheared 20 wt% sample. The rheograms for this sample are in Appendix B.

The viscosity of the 5 wt% sample was mostly Newtonian in behavior, with only a slight indication any yield or pseudo-plastic behavior. This slight non-Newtonian behavior is most likely due to the fact that at low viscosities the material being tested is below the recommended range for the SV1sensor. Therefore the non-Newtonian behavior is possibly an artifact of loading stresses and inertia associated with instrument start up.

The 15, 20 and 25 wt% material displayed characteristic pseudoplastic flow behavior, each with an apparent yield stress. The data most often fit one to three of the classic curves, presented in Section 3.2, with an R² of 0.8-1.0. As would be expected, the yield stress and apparent viscosity increased with solids loading in a nonlinear fashion.

Temperature Effects: The 5 wt% feed exhibited large amounts of scatter in the data resulting from use of the SV1 sensor. No temperature effects were measurable within the range of this system.

As observed for the C-104 feeds, the C-104 15 wt% material showed an unexpected small rise in apparent viscosity and yield with the increased temperature. This rise is well within the range of error for this system with a change of sample, however since it was consistent it may be a real effect. This effect could also be a result of a small amount of dehydration during testing, even though visually the material did not appear to have dried out. If more material had been available a second sample would have been run at each temperature.

3.2.2 Rheology of Melter Feed with Secondary Waste Products

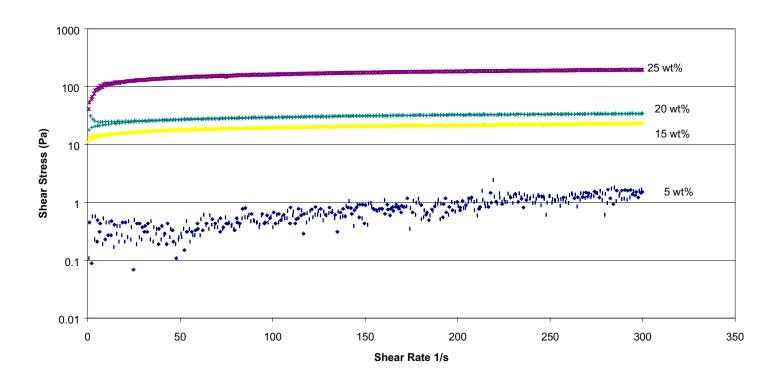
C-104

Rheology data was gathered after adding secondary waste products to the C-104 5, 15 and 25 wt% slurries. Yield stress and viscosities at 33, 150, and 298 S⁻¹² are presented in Table 3.4. Comparing Table 3.3 and 3.4, one notes there was little change between the initial evaporated feed and the feed after addition of secondary waste. The only slight change was observed in the apparent yields of the 15 wt% samples. These yields are slightly higher after adding the secondary waste. Temperature seems to have no additional effect on the C-104 sample with secondary waste.

Table 3.4. Viscosity Data (cP) for C-104 with Secondary Waste

	25°C				50°C			
Material	Yield ^a (Pa)	$33 s^{-1b}$	150 s ^{-1b}	298 s ^{-1b}	Yield ^a (Pa)	$33 s^{-1b}$	150 s ^{-1b}	298 s ^{-1b}
C-104 5 wt%	<1	9.6	3.5	3.4	<1	7.6	3.8	2.5
C-104 15 wt%	~2	28.7	8.0	5.6	~2.5	28.4	7.5	5.8
C-104 25 wt%	~5	158.5	44.5	27.0	~8	193.5	56.7	30.1

- a. Yield data is in Pa and is based on visual estimates from the graph and/or various curve fits. When there is a disparity between multiple runs the highest yield is reported 1 Pa was the limit for quantification.
- b. Viscosity data is in cP and is an average of multiple runs at each shear rate given.



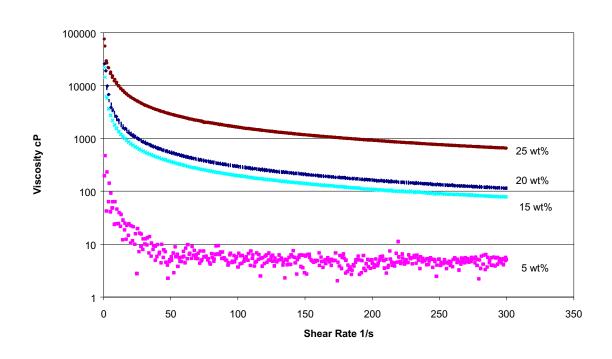


Figure 3.17. Rheograms for AZ-102 Initial Feeds at 25°C

AZ-102

As planned in Addendum 1 to Test Plan 29953-073, rheology measurements on the AZ-102 material with secondary waste products were not completed because the small amount of secondary waste products added was not expected to impact the rheology.

3.2.3 Rheology of Melter Feed with Glass Formers

C-104

The C-104 5 wt% waste shows little change with the addition of secondary waste and glass formers. Yield stress and viscosities are presented in Table 3.5. All the 5 wt% data is within the range of scatter for low viscosity materials using the SV1 sensor. The C-104 15 and 25 wt% wastes increased in both apparent yield stress and viscosity once the glass formers were added. As seen in Figure 3.18, most significant increase occurred in the 25 wt% slurry where the yield stress jumped from ~5 to ~30 Pa. These data should be considered carefully if 30 Pa is near the range of potential process constraints. Again there is the slight increase in yield stress and viscosity at the 50°C temperature range. The slurry still displays yield pseudoplastic behavior after the addition of glass formers.

Table 3.5. Viscosity Data	for Evaporated Feeds with Sec	condary Waste and Glass Formers
---------------------------	-------------------------------	---------------------------------

	25°C				50°C			
Material	Yield ^a (Pa)	$33 \text{ s}^{-1\text{b}}$	150 s ^{-1b}	298 s ^{-1b}	Yield ^a (Pa)	33 s ^{-1b}	150 s ^{-1b}	298 s ^{-1b}
C-104 5 wt%	<1	8.2	4.2	4.2	<1	9.0	2.0	3.1
C-104 15 wt%	~4	138.3	45.6	29.2	~5	195.4	53.0	32.6
C-104 25 wt%	~25-30	835.2	221.7	126.1	~30-33	1075.8	265.1	146.0
AZ-102 5 wt%	<1	11.2	4.6	7.3	<1	9.2	3.8	5.0
AZ-102 15 wt%	~5	180.6	63.6	42.2	~6-7	227.0	73.4	47.7

a. Yield data is in Pa and is based on visual estimates from the graph and/or various curve fits. When there is a disparity between multiple runs the highest yield is reported 1 Pa was the limit for quantification.

AZ-102

The AZ-102 5 wt% slurry maintained or slightly dropped in viscosity with the addition of the secondary wastes and glass formers, again the change was well within the error band of the equipment. However the 15 wt% slurry experienced a significant, around 50% decrease in both yield stress and viscosity as seen in Figure 3.19. Since glass formers contain no liquid, glass former addition should have resulted in an increased viscosity (although addition of certain solids could decrease viscosity). It was noted in the AZ-102 feed discussion, that it is highly probable that this material is irreversibly shear thinning, the observed decrease is probably the result increased shear history and not addition of glass formers alone.

b. Viscosity data is in cP and is an average of multiple runs at each shear rate given.

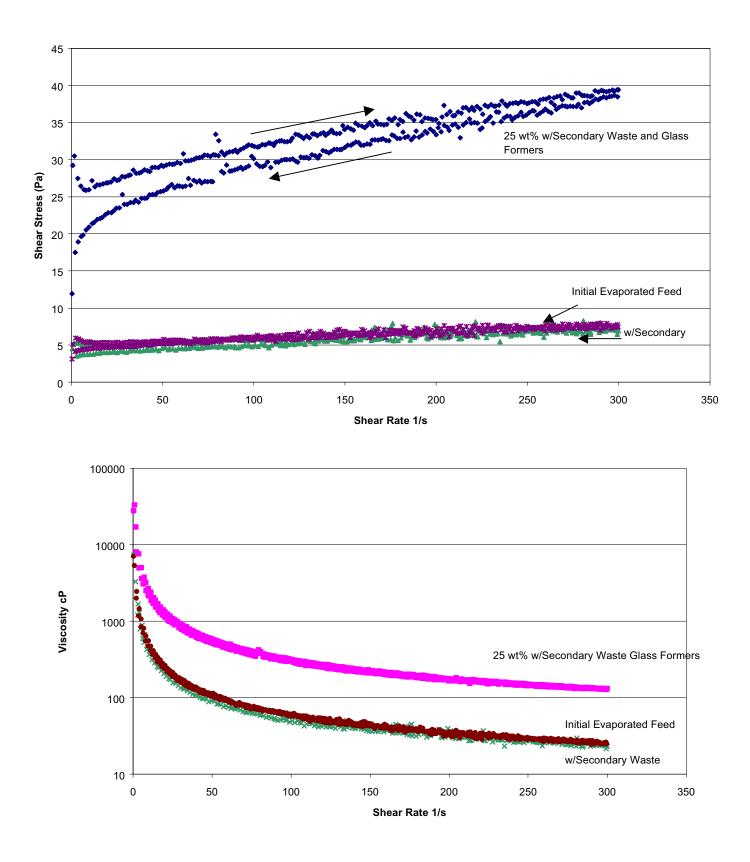
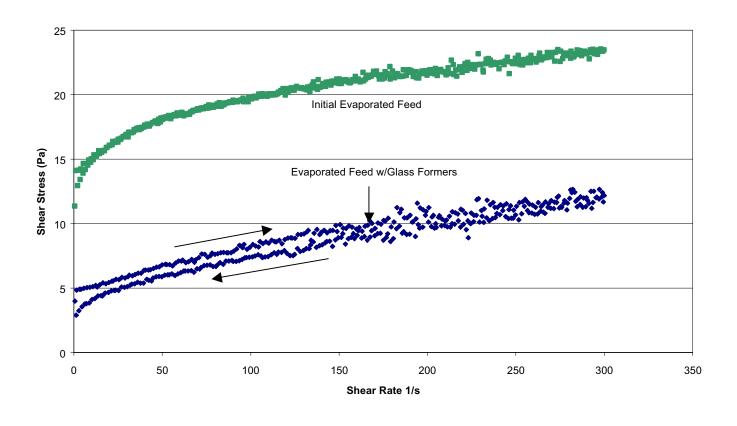


Figure 3.18. Comparison of C-104 25 wt% Feed Initial Alone, With Secondary Waste and With Glass Formers and Secondary Waste at 25°C



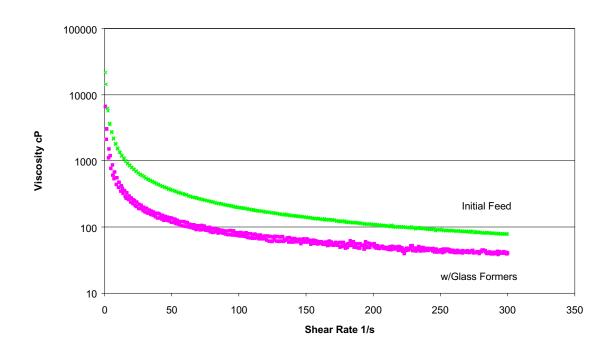


Figure 3.19. Comparison of AZ-102 15 wt% Feed Alone and With Glass Former at 25°C

3.3 AZ-102 Mixing and Aging Study

A fresh sample of AZ-102 15 wt% solids, with both secondary wastes and glass formers added, was mixed for over for a week at ambient temperature (34°C). Rheology measurements were taken at 1 hour, 1 day and 1 week at 25°C. The AZ-102 slurry decreased significantly in both yield stress and viscosity with time while mixing as seen in Figure 3.20. This decrease with mixing fits well within the irreversible shear thinning observed previously for the AZ-102 material.

The material was then rinsed into a graduated bottle and the excess water added to it in the transfer process was evaporated off. The slurry was then allowed to settle for 1 week at ambient temperature (34°C) and observed for gas retention and release. No gas retention or release was observed. At this point the test plan called for any excess liquid to be drained and a rheology measurement made of the settled solids. The standing liquid was removed from the AZ-102 and the solids were measured. Rheograms are presented in Figure 3.21. Yield stress and viscosity data are presented in Table 3.6.

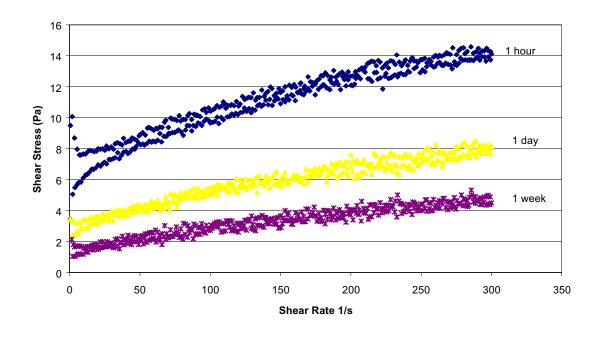
One will note a drastic increase in the viscosity and yield after settling for one week. While this seems to contradict irreversible shear thinning, one must remember this data was collected on the settled solids following removal of standing liquid. There was no standing liquid on the initial 15 wt% evaporated feed, so standing liquid on the same feed after addition of dry glass formers shows a significant change in solids structure.

Table 3.6. Viscosity Data for AZ-102 Mixing and Aging Study Measured at 25°C

Material	Yield ^a (Pa)	33 s ^{-1b}	150 s ^{-1b}	298 s ^{-1b}
AZ-102 1 hr	~6-7	252.5	80.3	49.5
AZ-102 1 day	~3	123.5	41.5	27.1
AZ-102 1 week	~1	51.9	18.7	14.8
AZ-102 Settled 1 week	~6-12	276.6	92.2	58.7

a. Yield stress data is in Pa and is based on visual estimates from the graph and/or various curve fits. When there is a disparity between multiple runs the highest yield is reported. The limit for quantification was 1 Pa.

b. Viscosity data is in cP and is an average of multiple runs at each shear rate given.



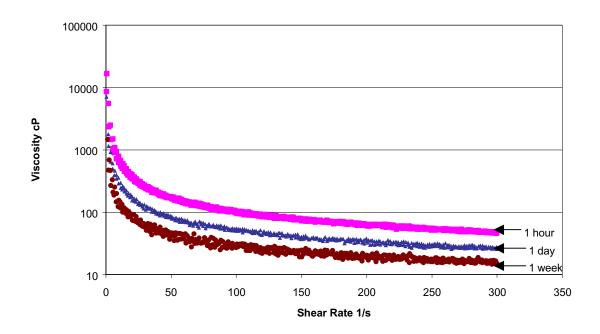
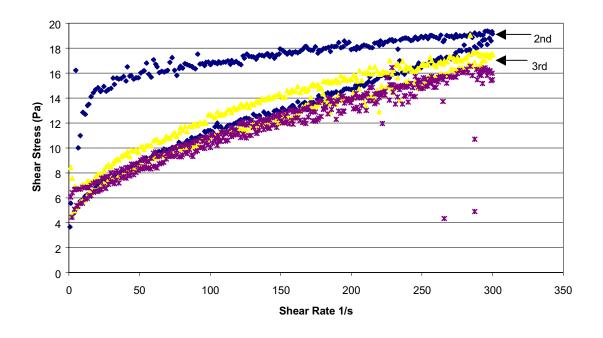


Figure 3.20. Rheograms for AZ-102 15 wt% Mixing Study, Measurement Performed at 25°C



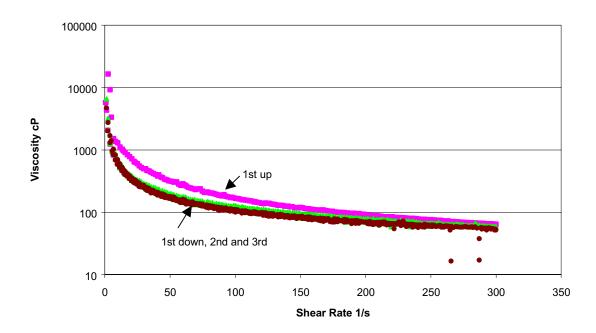


Figure 3.21. Rheograms for AZ-102 15 wt% Aging Study Measurements Performed at 25°C

3.4 C-104 Mixing and Aging Study

A fresh sample of C-104 25 wt% solids with both secondary wastes and glass formers added was mixed for a week at ambient temperature (34°C). Rheology measurements were taken at 1 hour, 1 day and 1 week at 25°C. Yield stress and viscosity data are summarized in Table 3.7. As seen in Figure 3.22, the C-104 slurry increased in both yield stress and viscosity with time while mixing. The material started out with a yield of ~28 Pa which is already close to many processing/design limitations and climbed to over 55 Pa by the end of the week.

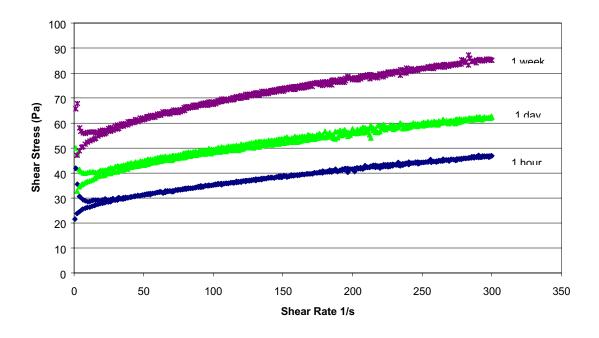
The material was then rinsed into a graduated bottle and the excess water added in the transfer process was evaporated off. The slurry was then allowed to settle for 1 week at ambient temperature (34°C) and observed for any gas retention and release. No gas retention or release was observed. At this point the test plan called for any excess liquid to be drained and a rheology measurement made of the settled solids at 25°C. There was no extra liquid to remove from the C-104 material after the 1-week aging period. As seen in Figure 3.23, yield stress of the aged settled solids spiked at over 80 Pa before settling down to ~40 Pa on repeat analysis. Materials with a yield stress this high could be difficult to pump and process.

Table 3.7. Viscosity Data for C-104 Mixing and Aging Study Measured at 25°C

Material	Yield ^a (Pa)	33 S ^{-1b}	150 S ^{-1b}	298 S ^{-1b}
C-104 1 hr	~28	914.5	258.9	157.2
C-104 1 day	~38	1264.5	351.3	209.1
C-104 1 week	~56	1740.5	479.7	282.3
C-104 Aged 1 week	~ 80	1621.3	421.8	240.7

a. Yield data is in Pa and is based on visual estimates from the graph and/or various curve fits. When there is a disparity between multiple runs the highest yield is reported. The limit for quantification was 1 Pa.

b. Viscosity data is in cP and is an average of multiple runs at each shear rate given.



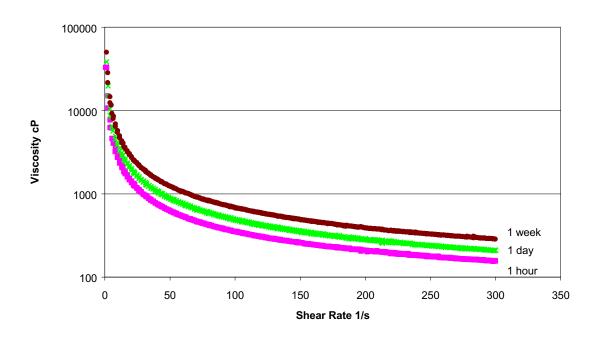
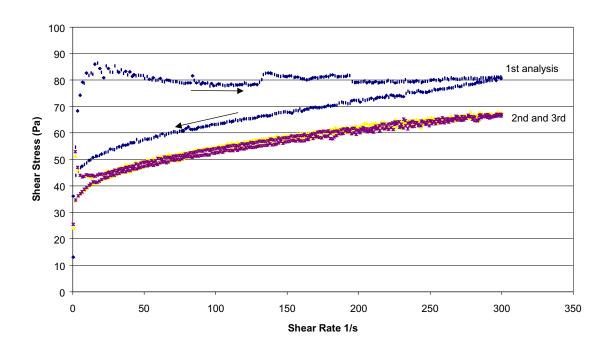


Figure 3.22. Rheograms for C-104 15 wt% Mixing Study Measurement Performed at 25°C



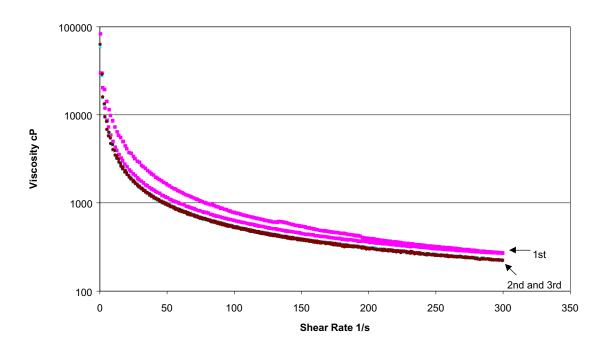


Figure 3.23. Rheograms for C-104 25 wt% Aging Study Measurement Performed at 25°C

4.0 Conclusions

The following conclusions were made based on the rheology and physical properties of the AZ-102 and C-104 evaporator and melter feeds. These conclusions have been divided into categories for clarity.

Concentration/Evaporation

- The AZ-102 initial feed was received at 9.54 wt% solids with no standing liquid. Therefore, concentration of the feed to 15 and 25 wt% resulted in thick slurries with no standing liquid.
- The C-104 initial feed was received at 20 wt% solids with roughly 15 vol% standing liquid. Evaporation of this feed to 25 wt% resulted in a slurry with little to no standing liquid after extended settling periods of greater than 3 days.

Density and Settling Behavior

- As expected, the densities of the samples increased with solids concentration $(\rho_{25\text{wt}\%} > \rho_{15\text{wt}\%})$ and increased following the addition of secondary waste products and increased again after the addition of glass formers.
- No significant temperature trends were observed in sample densities between 34 and 50°C. This is attributed to a lack of soluble solids.
- Samples did not compact as effectively at 50°C as at 34°C. This increase in settled solids volume ranged between 4 and 8 vol%. This is probably the result of the test methodology breaking up the aggregate structure during sample agitation between the 34°C test and the 50°C test.
- Addition of secondary waste products (primarily Sr/TRU precipitate) to the C-104 evaporated feeds increased the initial solids settling rate by an order of magnitude. This is most notable in the 5 wt% feed supernatant, which remained cloudy after 3 days of settling. However, after secondary waste product addition, this sample settled with a clarified supernatant. This behavior is most likely the result of flocculation of the sludge particles with the Sr/TRU secondary waste product.
- Addition of glass formers to the AZ-102 samples appears to have increased the settling rate by approximately a factor of four. However, the increase in settling rate for the AZ-102 samples in much less dramatic than the increase for the C-104 samples.

Rheology of Evaporated Feeds

- No significant temperature effects were seen for the C-104 or AZ-102 samples measured at 25 and 50°C.
- The AZ-102 feed displayed initial viscosities of 12, 530, 900, and 4600 cP for the 5, 15, 20, and 25 wt% feeds. In addition, the AZ-102 feeds displayed significant irreversible shear thinning.

Rheology with Secondary Waste Products and Glass Formers

- Very little change in rheological properties were observed following secondary waste products (Sr/TRU precipitate and Cs eluants) and glass former addition to the C-104 feed.
- The yield and viscosity the AZ-102 feed dropped following glass former and secondary waste addition (Sr/TRU precipitate). The observed decrease is most likely the result of the increasing shear history of the AZ-102 samples as the testing progressed.

Melter Feed Mixing and Aging

- The yield stress and viscosity of the AZ-102 slurry decreased over the one week mixing period consistent with the previous observations in this report of irreversible shear thinning in this slurry.
- Following one week of settling, the yield stress and viscosity of the AZ-102 settled solids
 were higher than similar testing after one week of mixing. This increase was expected
 and attributed to increased solids loading resulting from removal of the standing liquid
 from the aged sample.
- The results of the mixing and settling studies suggest that while the AZ-102 initial feed and final melter feed material may be very difficult to mix and transport, irreversible shear thinning significantly reduces the yield and viscosity. Therefore, exposing this material to some initial shearing may be an option for reducing these critical transport properties.
- The yield stress and viscosity of the C-104 slurry increased over the one week mixing period. The C-104 slurry yield stress increased from 28 Pa after one hour to 56 Pa after one week. Over this same period, the viscosity of the C-104 slurry increased from 910 cP to 1700 cP at 33s⁻¹.
- After standing for one week, the viscosity of the C-104 solids did not settle into a separate layer, so no liquids were decanted. The viscosity of the C-104 settled material was similar to the viscosity after one week of mixing, but the yield stress increased to approximately 80Pa.
- The yield stress and viscosity of the C-104 melter feed increased with mixing and the yield increased further with aging. These results suggest the final C-104 melter feed could be very difficult to mix and transport on a 25 wt% basis.

5.0 References

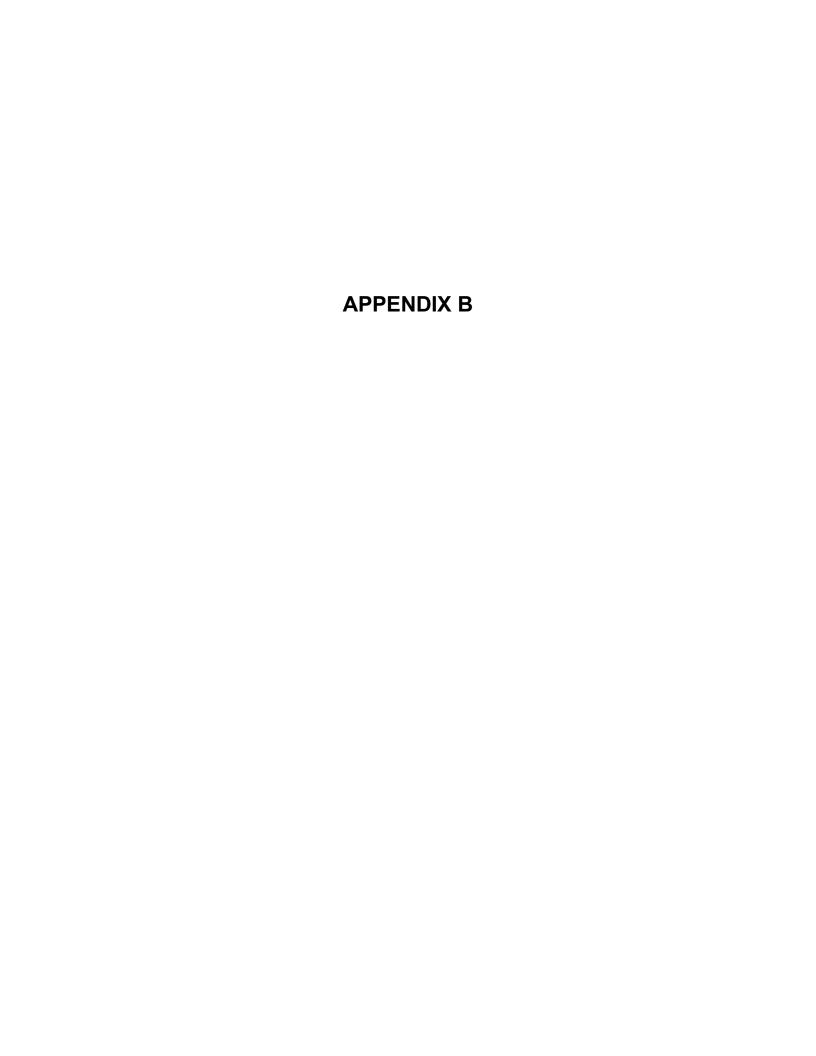
Bredt, PR and RG Swoboda. 2000. "Rheological Studies on Pretreated Feed and Melter Feed From AW-101 and AN-107," PNWD-3034, Revision 0, Battelle Pacific Northwest Division, Richland, Washington.

Brooks, KP, PR Bredt, GR Golcar, SA Hartley, LK Jagoda, KG Rappe, MW Urie. 2000. "Characterization, Washing, Leaching, and Filtration of C-104 Sludge," PNWD-3024, Battelle Pacific Northwest Division, Richland, Washington.

Brooks, KP et al. 2000. "Characterization, Washing, Leaching, and Filtration of AZ-102," PNWD-3045, Battelle Pacific Northwest Division, Richland, Washington.

APPENDIX A

Appendix A: Test Plans



Appendix B: Rheograms



Appendix C: Test Instruction

Distribution

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Appendix A: Test Plans

PNNL Test Plan

Document No.: BNFL-TP-29953-073

Rev. No.: 0

Document Control: Only the original signed copy is controlled

Title: High Activity Melter Feed Rheological and Phy	sical Properties Measurements
Work Location: Radiochemical Processing Laboratory	Page 1 of 60
Author: Paul Bredt	Effective Date: Upon Final Approval
Use Category Identification: Reference	Supersedes Date: New
Identified Hazards: Radiological Hazardous Materials Physical Hazards Hazardous Environment Other:	Required Reviewers: X Technical Reviewer X Building Manager Radiological Control ES&H X Quality Engineer X Project Manager X RPL Manager SFO Manager SFO Manager
Are One-Time Modifications Allowed to this Proce NOTE: If Yes, then modifications are not anticipated to in see SBMS or the controlling Project QA Plan as appropriat	edure? X Yes No npact safety. For documentation requirements of a modification e.
On-The Job Training Required? Yes orX_N	О
FOR REVISIONS: Is retraining to this procedure required?YesX Does the OJT package associated with this procedure requiredYesNoXN/A	
Approval Signature	Date
Author Pand Building Manager RPL QE Taffy Allman	12/6/99 $12/20/99$ $12/16/99$ $12/16/99$ $1/20/00$ $1/20/00$ $1/21-00$ $1/21/00$

Battelle Test Plan: BNFL-TP-29953-073 Page 2 of 60

High Activity Melter Feed Rheological and Physical Properties Measurements

Scope

Physical and rheological properties will be measured for the waste sample from tanks AZ-102 and C-104. Solids settling rate, density and shear stress versus shear rate rheograms will be measured on the samples after concentration to three undissolved solids concentrations (typically, 5wt%, 15wt% and 25wt%, i.e. including dilution and evaporation of the pretreated sample) at ambient temperature and at 50°C. The same measurements will be conducted on the three mixtures after addition of the prescribed quantities of intermediate waste products (137°Cs, 99°Tc and 90°Sr/TRU) and then glass formers (typically 300 g/l, or 500 g/l). The viscosity of one slurry will also be measured after 1 hour, 1 day and 1 week; the slurry will be mixed to provide a shear rate consistent with that expected in the facility. The viscosity of this slurry will be further measured after 1 week with no mixing.

This document satisfies the requirements of a test instructions which provides specific details for the implementation of Technical Procedure 29953-010, "Measurement of Physical and Rheological Properties of Solutions, Slurries and Sludges". Client expectations for successful achievement of project data needs have already been established via the "HLW Melter Feed Rheology" test specifications, numbered TS-W375LV-TE00002 and TS-W375HV-TE0006, provided to Battelle by BNFL.

Justification of Use Category

This procedure is reference use. Reference use was selected as the use category since this analysis is not a complex process and there are no safety impacts to the order of events. In addition, we may wish to modify the order of analyses or eliminate some analyses depending on the needs at the time of the operation.

Applicability

This test plan applies to RPL staff performing work on BNFL Privatization samples under Project 29953.

Work with actual samples is to be performed in hot cells in the RPL by staff under the direction of a cognizant scientist.

Page 3 of 60

Prerequisites

1) Keep the sample in a sealed glass container as much as possible to prevent it from drying and reduce the potential for organic contamination.

2) Cross-contamination between samples and contamination of samples from outside sources must be minimized at each step. Use new tools and bottles for each sample as much as possible. Those tools which are reused should be washed and rinsed prior to reuse.

3) Secondary containment is to be used whenever practical to minimize sample loss in the

event of a spilled sample or broken sample bottle.

4) This Test Plan requires work in an oven or viscometer at 50°C. Unless otherwise indicated, a value of ±5°C is acceptable.

Quality Control

M&TE List:

Quality control has been implemented in Technical Procedure 29953-010, "Measurement of Physical and Rheological Properties of Solutions, Slurries and Sludges". Work shall be performed in accordance with the current revision of Battelle's quality assurance plan, BNFL-QAPjP.

Balance 1:		
Calib ID 384-06-01-004	Calib Exp Date_	8/2000
Location Front face	HLRF	
Balance 2:		
Calib ID 366-06-01-020	Calib Exp Date	8/00
Location c-cell		
Thermocouple:		
Calib ID 03003	Calib Exp Date_	8/00
Location A-Coll		
Digital Thermometer:		
Calib ID PNL000 2927	Calib Exp Date	3/01
Location Fort Sca 32	SHLRF	

Page 4 of 60

Work Flow

- 1) Load 5 subsamples of a waste in graduated centrifuge tubes and place in vacuum jar.
- 2) Evacuate jar and monitor sample masses. To accelerate the evaporation, it may be necessary to heat the samples. Heating should be done in an oven at 50°C (±10°C).
- 3) At predetermined mass loss intervals, remove one centrifuge tube at a time from the jar and cap.
- 4) After a predetermined time interval, centrifuge the cones and measure the vol% and wt% centrifuged solids. Use this data to plot correlation between mass loss and wt% solids.
- 5) Load three graduated jars with same waste type.
- 6) Apply a vacuum to the jars and monitor the mass/volume loss until the three desired loss levels have been reached. To accelerate the evaporation, it may be necessary to heat the samples. Heating should be done in an oven at 50°C (±10°C).
- 7) Measure the density of the material in the graduated jars and record the ambient cell temperature.
- 8) Stir the jars and monitor the settled solids volumes over a 3 day period at ambient (record the ambient cell temperature.
- 9) Place the jars in an oven at 50°C (±5°C) for 1 day.
- 10) Measure the density of the material in the graduated jars at 50°C (±5°C).
- 11) Stir the jars and monitor the settled solids volumes over a 3 day period at 50°C (±5°C).
- 12) While stirring, remove subsamples from each of the three graduated jars in duplicate and analyze for shear stress versus shear rate at ambient cell temp and 50°C.
- 13) Add the prescribed quantities of intermediate waste products (137Cs, 99Tc and 90Sr/TRU) and stir for one hour using an overhead mixer.
- 14) Repeat steps 7 through 12.
- 15) Add the prescribed quantities of glass formers to each of the three jars and stir for one hour using an overhead mixer.
- 16) Repeat steps 7 through 12.
- 17) Transfer one of the three samples prepared in step 15 to an airtight mixing vessel with sampling port.
- 18) Mix this sample for one week.
- 19) During the week of mixing, measure the shear stress as a function of shear rate on this samples after 1 hour, 1 day, and 1 week.
- 20) After the week of stirring, transfer the material back to the graduated jar and leave undisturbed for 1 week.
- 21) During this one week, monitor for gas retention/release behavior.
- 22) After one week, measure the shear stress versus shear rate on the sample.

Work Instructions

AZ-102

1) Record the solids concentration of the AZ-102 feed.

Wt% solids=9.5 4 % (C1)

Data Source BNFL-TI-29953-079
Rev. 1 addedon 3

2) Record the Wt% solids targets provided by BNFL.

Wt% solids = $\frac{15}{25}$ Wt% solids = $\frac{25}{25}$ (C2b)

3) Load 8 ml of AZ-102 material into 5 preweighed centrifuge cones. Record the new weight.

AZ 2 AZ3 Total Total Total Cone Cone g ____ g Cone Slurry Slurry g Slurry AZ4 AZ 5 skipped as per Encil
with Stunt Arm on
4 3/30/00 pres Total Total Cone Cone g Slurry Slurry

(C2c)

- 4) Remove the caps, and place the centrifuge cones in a vacuum jar. If necessary to accelerate evaporation, place the jar in an oven at 50°C (±10°C).
- 5) At intervals determined by the cognizant scientist, remove the cones from the vacuum jar, replace the caps, and record the new weight.

AZ 1 AZ 2 AZ3 Total Total Total Cone Cone Cone Slurry Slurry Slurry AZ4 AZ 5 Total Total Cone _____g Cone Slurry Slurry

Attachment to BNEL-Tr-29953-073 PRB 4/3/00

Bredt, Paul R

From: Stuart Arm [sarm@bnflinc.com]

Sent: Thursday, March 30, 2000 12:46 PM

To: Bredt, Paul R Cc: Smith, Gary

Subject: Re: AZ-102, C-104 Evap for Melter Feed Rheology Testing

Paul,

Good idea, please proceed as you describe.

Stuart.

"Bredt, Paul R" wrote:

Stuart,

Given that the supernatant associated with the AZ-102, and C-104 samples have little to dissolved solids, we were hoping to get your concurrence on a simplification of Test Plan 29953-073.

Under steps 3-7 and 66-70 we were planing on running 5 test samples for each waste to determine the amount of moisture that must be evaporated to reach the 5, 15, and 25 wt% solids levels. Instead, we would like to use the current wt% solids numbers for our basis for solids content and assume no solids will precipitated during the evaporation. We would then evaporate the samples by applying a vacuum and flowing air over the material though a pinhole in the lid.

Please let me know as soon as possible if this approach is acceptable, and we will start the evaporation (I still owe you an addendum for glass formers, but I have put it off a until next week as we are collecting more information on AZ-102 and the Sr/TRU ppt).

Thanks, Paul 6) Centrifuge the cones at ~1000 x g for one hour. Record the solids and liquid volumes.

	AZ 1			AZ 2		2	AZ 3	
Total Solid Liquid	\equiv	ml ml ml	Total Solid Liquid		ml ml ml	Total Solid Liquid		ml ml ml
	AZ 4			AZ 5			•	
Total Solid Liquid		ml ml ml	Total Solid Liquid		ml ml ml			

7) Decant the centrifuged liquid to a preweighed graduated cylinder. Record the mass and volume of liquid in the graduated cylinder.

·	AZ 1	<i>8</i>		AZ2	5 . 1 - 7	75 86	AZ 3	•0
Total Grad Liquid Liquid		g g g ml	Total Grad Liquid Liquid		g g g ml	Total Grad Liquid Liquid		g g ml
	AZ 4			AZ 5				
Total Grad Liquid Liquid		g g g ml	Total Grad Liquid Liquid		g g ml			

- 8) Based on the results from AZ 1 through AZ 5, determine the amount of water on a wt% basis to evaporate from the three samples to reach the target solids concentrations. Attach the calculations to this Test Plan. See attached PAB 4/3/00
- 9) Weight three appropriately sized glass graduated jars or cylinders labeled AZ EVAP A, AZ EVAP B, and AZ EVAP C. Jars Labeled AZ-102 washed solids." Rheol-5 Rheal-15 Rheal-25-1 AZ EVAPA AZ EVAP B

AZ EVAP C

Rhed-25-2

Date: 4/3/00

Project: BNFL 19953

Prepared By: PR Bre St

AZ-101. Eurporation under stap 8 of Test plan 29953-073

Samples were prepared (subsampled) under BNFL -TI - 29953-079 Ru. 1 addedun \$2 PRB Sample solids content is 9.54 out % under addendum 3

5 ht's sample:

Current mass = 41.849 C,M, = CZMZ 5 · 41-84 x = 41.84 · 9.54 x = 41.84-9.54/5 x = 79.83

Water to add = 79.83 - 41.84 = 37.999

15 ht % sample :

x=122.00.9.54/15 = 77.59

water to end = 122.00-77.59 = 44.4/g

25-1 Sample: Correct mass = 136.53 a x = 136.53.09.54/25 = 52.10

water to evap = 136.53-52.10 = 84.43.

25-2 sample :

current mass = 136.32 x= 13632.9.54/95 x = 52.02

vater to evap = 136.32-52.02 = 84.30

calculations elected by SARS

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Page 9 of 10

pumping process. When the target weight of the AZ-102 pretreated waste has been transferred, stop the pump, and reverse the peristaltic pumping direction to pump the composited AZ-102 pretreated waste that is in the tube back into the AZ-102 washed sludge jar. Finally, after all samples have been taken, clamp the end of the tube that was discharging into the stainless steel beaker or glass jar(s), remove the tubing from the peristaltic pump, and, after raising the clamped end of the tubing above the level of the jar, unclamp it allowing any remaining pretreated waste slurry to drain back into the jar.

Weight of AZ-102 pretreated waste transferred from "AZ-102 Washed Solids Comp" to:

470.97 g "AZ-102 Washed Sludge Vit-1" stainless steel beaker

134,58 g "AZ-102 Washed Sludge: Rheol-5" 125 mL wide mouth glass jar

134.16 g "AZ-102 Washed Sludge: Rheol-15" 250 mL wide mouth glass jar

217. 49 g "AZ-102 Washed Sludge: Rheol-25-1" 250 mL wide mouth glass jar

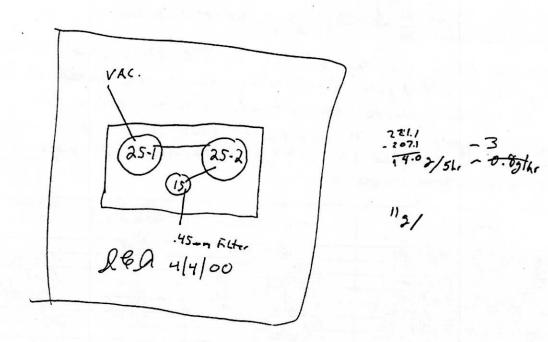
217.50 g "AZ-102 Washed Sludge: Rheol-25-2" 250 mL wide mouth glass jar

Sign and date Michael Shweige Note: enter above data into Addendum 2, Table 1 below.

Observations: After sampling of the 2 AZ-102 washed Solidar Comp - ICP-1 (\$2) plus the archieve sample on March 13, 2000, the AZ-102 Comp waste was stored with a Teffon Ird the AZ-102 Comp waste was stored with a Teffon Ird tightly capping it. On March 14, 2000, at ~ 10:00 am the container was weighed (2020. 477) to determine if evaporation OVER

Sample ID	Sample Application	Nominal Sample Size (g)	Actual Sample Size (g)	
AZ-102 Washed Solids Comp	Source material	954.57	1144	
AZ-102 Washed Studge Vit-1	Glass Batching	507.57	499.25	
AZ-102 Washed Sludge: Rheol-5	Rheology properties	40 -	41.84	
AZ-102 Washed Sludge: Rheol-15	Rheology properties	122	122.00	136-
AZ-102 Washed Sludge: Rheol-25-1	Rheology properties	135 }	+ 138.53	1362
AZ-102 Washed Sludge: Rheol-25-2	Rheology properties	135/L	-135.84	1364
AZ-102 Washed Solids Comp-ICP-1	wt% solids, ICP-AES	5 \ .	5,53	-
AZ-102 Washed Solids Comp-ICP-2	wt% solids, ICP-AES	5	6.21	1
AZ-102 Washed Sludge: Arch-1	Archiving	5/	7,54	ا

200 3/16/00



ruler.

ru	ler.		, ,		ed look glass graduated
	Iliah	•	COALS USAN		
	High	ml	for seffling		ylinde: al from 10 to -3.5 al
	Low	ml			- from 10-4-1 = 4.2cm
	Distance	cm			
11) Tr	ansfer the required mas	s of mate	rial into the three gradu	ated glas	sware. 9/17/00
	AZ EVAP A		AZ EVAP B		AZ EVAP C
Total Tare Slurry	g g g	Total Tare Slurry	g g g	Total Tare Slurry	g placed in vacuum train
ام مدی 12) Ap	oply a vacuum to the sai	astalled nples.	filter to keefout is some effect as B	Drilled dirt.	hole in first B. Hles. ir over samples) PRBY5/0.
13) Mo	onitor the mass of each	sample o	n a regular basis to asse	ss the rat	e of evaporation. If necessary to
acc	celerate evaporation, pla	ace the ja	r in an oven at 50°C (±1	0°C).	
*	AZEVAPA		-25-1 AZ EVAP B		AZ EVAP C
Date Mass	255.453	Date Mass	4/4/00 353.022	Date Mass	4/4/00 Starty mss
Date Mass	4/5/00 7:504m 244.720;	Date Mass	4/5/60 8:00 Am 342.642	Date Mass	4/5/00 8:05mm Restant 8:20mm4/5/0
Date Mass	4/5/00 2:00pm 227.558g	Date Mass	315.706	Date Mass	4/6/00 8:05am Rester 8:25 41
Date Mass	4/5/00 7:45A4 221. 1128	Date Mass	4/7/00 9:30 mm 295. AGI	Date Mass	215.037,
Date Mass	4/6/00 12:50pm 207./64	Date Mass	282.987	Date Mass	4/1/00 3:40 pm 277.592
Date Mass		Date Mass	269.787	Date Mass	4110/00 7:45pm 257.886 257.886 164/10/00
Date Mass		Date Mass		Date Mass	
				25%	suph s look fin with cracked surfaces but

10) Measure the distance between the highest and lowest graduation on the graduated glassware using a

Page _____ of_____

Pacific Northwest Laboratories

ENGINEERING WORKSHEET

Prep	pared By: Pa-1	Bredt	Date: 4/11/00	Project: BN	FL T1- 29	9953- 673	
T:	Subject: W_+	er additions	to A2-102	simples	Rhe.1-5	-15 -251	- 25-2
						, ,	7

	1-5	1-15	-25-1	- 25-2
plostip 9 Taratacss	214.41	211.75	269.59	269.52
Corrent mass (g)	175.987	206.909	269.592	257.778
water to add (g)	36.42	4.84	0.008	11.74
water edded (g)	38.638	5.087	0	11.725
F.n-1 m-55 w/5-1(5)	214.625	211.96 211.996 PR 54/2/00	269.582	269.503

The about table documents water additions to AZ-10Z Samples following evaporation stop 13 of Test plan work performed on 4/12/00
PRB4/12/00

> Used Type 2 reget water from Nonopie system in 165 201. 717.6 M 04-5

cefter find addition 7

Rheal-25-2

Tea 269.503

Tea 217.50

Slurry 52.003

5

PR Bredt Battelle Test Plan: BNFL-TP-29953	3-073
12/6/99 - Page 8	
AZEVAPA AZEVAPB AZEVAPC	\$
Date Date Date	
Mass Mass	
Date Date Date	
Mass Mass	
14) When the most of each of the above	
14) When the mass of each of the slurries reaches the targets calculated above, remove them from the	e
vacuum and cap the sample. Record the mass. following wateradditon, see attach	ELS IRA
AZEWADA	77/7
-15 ALEVAIC	41.2/
Total 214.625 g Total 211.996 g Total 269.582 g	Par Conver
Tare 134.58 g Tare 134.16 g Tare 217.49 cite s	durit Arm
Slurry 80.045 g Slurry 77.836 g Slurry 52.092 g	110100 PRB
25~1(~89)	4
15) If the samples are in glass jars, transfer them to appropriately sized preweiged graduated cylinder	ere ca
with caps or plugs. Record the mass and volume of material in each of the graduated cylinders.	
Centrifuge et 1000x3 for 5min.	
Rheol- 5 A Rhe-1-15 A 0-1.153 Rhe-1-25-1 A	
- 1771	
S Total g Total Kr. 66 g	
Conc Grad 19.968 g coneGrad 19.777 g (concGrad 19.848 g	
Slurry 7.7920 g Slurry 9.805 g Slurry 6.81 g Volume 7.67.55 ml Volume 7.28.5 ml Volume 5.4 ml 5.6	= 1.26
Totalite 3:7 mil	,
16) Preweigh 3 teffon coated magnetic stir hars in 1 Study conduct to (Steps 2	21-25
(5 A)p= 1.03 g / PRB 4/20/00 B	, -, ,
(5 A) P= 1.03 g/m A /20/00 B	/00
g · g	
17) Preweigh 3 appropriately sized volumetric flasks.	
	•
A B C	
gg	
10) 11	
18) Place one stir bar in each of the volumetric flasks and fill to the mark with DI water. Record the	
mass of the volumetric flasks. Calculate the volume of the stir bars by the displacement of water	
A B C	
Flask (g Totalg Flask (g)	
Bar ()g Bar ()g Bar ()g	
Water g Water g Water g	
s waterg	
19) Place stir bar A in graduated cylinder AZ A, stir bar B in AZ B, and stir bar C in AZ C.	

)				Page 8 of B
Date	AZ EVAP A	Deser	AZ EVAP B		AZ EVAP C
Mass		_ Date		Date	* :
171455		_ Mass	/	Mass	
Date		Date		Date	
Mass		Mass		Mass	•
					1
14) W	en the mass of each	ch of the slurri	es reaches the target	s calculated a	above, remove them from the
vac	cuum and cap the s	sample. Recor	d the mass.		
	AZ EVAP A		AZ EVAP B		AZ EVAP C
			THE EVILLE		AZ EVAL C
Total		g Total	g	Total	g
Tare		g Tare	g	Tare	g
Slurry		g Slurry	g	Slurry	g See \$1
					cones
15) If th	he samples are in g	glass jars, trans	sfer them to appropr	iately sized p	reweiged graduated cylinders wit
B cap	s or plugs. Record	d the mass and	volume of material	in each of the	e graduated cylinders.
	Rha.H	a the mass and	volume of material	in each of the	e graduated cylinders.
	AZA		AZ-B-		A7.C
		RH			AZ-C
Total	27.65 gB		222720	T1	Rh.1 - 250
Grad		g Total	- C. 2.4	Total	26.58 g
	20.0.3	g con corau	19,836 g	ConcoGrad	19.871 g
Chirm		~ Cl			1 71
Slurry	7.563	g Slurry	10.510 g	Slurry	6.71 g
-	7.563 7.2 n	nl Volume		Slurry	6.7/ g e 5.5 ml
Volume P	7.563 7.2 1.05	nl Volume	10.510 g e 9.3 ml	Slurry	6.71 g e 5.5 ml
Volume <i>f</i>	7.563 7.2 n	nl Volume	10.510 g e 9.3 ml	Slurry Volum	6.7/ g e 5.5 ml
Volume <i>f</i>	7.563 7.2 1.05 weigh 3 teflon coa	nl Volume (a/) ted magnetic s	10.510 g e 9.3 ml 1.131 2 tir bars.	Slurry Volum	6.71 g e 5.5 ml 1.22 J/ac
Volume <i>f</i>	7.563 7.2 1.05	nl Volume g/ / / ted magnetic s	10.510 g e 9.3 ml 1.131 2 tir bars.	Slurry Volum	6.71 g e 5.5 ml 7 1.22 Z
Volume <i>f</i>	7.563 7.2 1.05 weigh 3 teflon coa	nl Volume (a/) ted magnetic s	10.510 g e 9.3 ml 1.131 2 tir bars.	Slurry Volum	6.71 g e 5.5 ml 1.22 J/ac
Volume P 16) Pre	7.563 7.2 n 1.05 weigh 3 teflon coa	ted magnetic s	10.510 g e 9.3 ml 1.131 2 tir bars. B g	Slurry Volum	6.71 g e 5.5 ml 7 1.22 Z
Volume P 16) Pre	7.563 7.2 1.05 weigh 3 teflon coa	ted magnetic s	10.510 g e 9.3 ml 1.131 2 tir bars. B g	Slurry Volum	6.71 g e 5.5 ml 7 1.22 Z
Volume P 16) Pre	7.563 7.2 n weigh 3 teflon coa	ted magnetic s	10.510 g ml 1.731	Slurry Volum	6.71 g e 5.5 ml 1.22 J/w
Volume P 16) Pre	7.563 7.2 n 1.05 weigh 3 teflon coa	ted magnetic s	10.510 g g g ml z tir bars. B g g metric flasks. B	Slurry Volum	C C C
Volume P 16) Pre	7.563 7.2 n weigh 3 teflon coa	ted magnetic s	10.510 g ml 1.731	Slurry Volum	6.71 g e 5.5 ml 1.22 J/w
Volume P 16) Prev 17) Prev	7.563 7.2 n Weigh 3 teflon coa	ted magnetic s	10.510 g 9.3 ml 1.131	Slurry Volum	C g
Volume P 16) Pres 17) Pres	7.563 7.2 n weigh 3 teflon coa weigh 3 appropriate	ted magnetic stated was generally sized voluments.	### 10.510 g ### 9.3 ml 1.131 2 tir bars. ### B ### g metric flasks. ### B ### g metric flasks and file	Slurry Volume	C g with DI water. Record the mass
Volume P 16) Pres 17) Pres	7.563 7.2 n weigh 3 teflon coa weigh 3 appropriate	ted magnetic stated was generally sized voluments.	### 10.510 g ### 9.3 ml 1.131 2 tir bars. ### B ### g metric flasks. ### B ### g metric flasks and file	Slurry Volume	C g
Volume P 16) Pres 17) Pres	weigh 3 teflon coal weigh 3 appropriate A ce one stir bar in each of the volumetric flash	ted magnetic stated was generally sized voluments.	metric flasks and fil he volume of the stir	Slurry Volume	C g with DI water. Record the mass displacement of water.
Volume P 16) Prev 17) Prev 18) Plac of th	weigh 3 teflon coal as weigh 3 appropriate the one stir bar in each evolumetric flash	g gach of the volumes. Calculate t	metric flasks and fil he volume of the stin	Slurry Volum I to the mark bars by the	C g with DI water. Record the mass
Volume P 16) Prev 17) Prev 18) Plac of th	weigh 3 teflon coal as weigh 3 appropriate the one stir bar in each evolumetric flash	ted magnetic so get ach of the volumes. Calculate to get a Total	metric flasks and fil he volume of the stin	Slurry Volum F	C g with DI water. Record the mass displacement of water.
Volume P 16) Prev 17) Prev 18) Place of the	weigh 3 teflon coal as weigh 3 appropriate the cone stir bar in each of the volumetric flash	ted magnetic so general general volumes. Calculate to general general general general volumes. Calculate to general ge	metric flasks and fil he volume of the sting B	Slurry Volum I to the mark bars by the	C g with DI water. Record the mass displacement of water. C g C g with DI water. C g c g with DI water. Record the mass displacement of water.
Volume P 16) Prev 17) Prev 18) Place of the	weigh 3 teflon coal weigh 3 appropriate the one stir bar in each of the volumetric flash A	ted magnetic so general genera	metric flasks and fil he volume of the stir bg ()g ()g	Slurry Volume I to the mark bars by the Total Plask Bar	C g with DI water. Record the mass displacement of water.
Volume P 16) Prev 17) Prev 18) Place of the	weigh 3 teflon coal weigh 3 appropriate the one stir bar in each of the volumetric flash A	ted magnetic so general general volumes. Calculate to general general general general volumes. Calculate to general ge	metric flasks and fil he volume of the sting B	Slurry Volum I to the mark bars by the	C g with DI water. Record the mass displacement of water. C g C g with DI water. C g c g with DI water. Record the mass displacement of water.

cones prohyon

20) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

RL)-SA AZA Ti	me 7:42:30	Date 4/14/00		
AZ B	me	Date	15 Lt% 225 Lt%	
AZ C Ti	me	Date	17 1. + settle 18 4/11/00	

21) After turning off the stirrer, record the ambient temperature volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient 34 °C Rhesl-5A

AZA without glass formers at ambient temperature

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min	4/14/00	2:47	7.75	7.75	0
15 min		2:57	,	7.75	
25 min		3:07		7.6	
35 min		3:17		75	
45 min		3:27		7. 5 7.5 7.45	
55 min		3:37		745	
1 hour		3:42		7.4	
1.5 hour		43:12		7.45	
2 hour		43:42		7.2	
2.5 hour		54:12		7.1	
3 hour		54:42		7.0	
3.5 hour		68:12		6.9	
4 hour		68:42		6.8	
4.5 hour		76:12		6.7	
5 hour		76:42		6.55	
5.5 hour		4:12		6.5	
6 hour		8:42		64	
6.5 hour		98:12	-	6.4	
7 hour		9:42		67	
24 hour	4115/00	2:42		4.75 4.75	
28 hour	4/15/0	6:42		47	
32 hour	4/15/00	10:42/2		4.65	-
48 hour	4/16/00	2:42		4.55	
52 hour	4/16/00.	6:421-		4.55	
56 hour	4/1400	10:42pm	U	455	
7241.	4/17/00	2:42		4.5	

5 B 5 A

Bottom of

miniscus = 7.6 ml

top-fminiscus = 7.75 ml

6 liss comes used for the

Study minisure 4.2 cm

from 10-4 ml

4.2 cm - 0.8 th colad

pro

(61-55 comes)

(61-55 comes)

PR Bredt 12/6/99

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PRB 4/11/00

20) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

Rhe.1-5B	Time 2:42:30	PAB Date	4/14/0-	
AZ B		-4/14/00 Date		12 + 52 1748
AZC	Time	Date		will not settle

21) After turning off the stirrer, record the ambient temperature volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient 34 . °C Rheol-5B

AZ A without glass formers at ambient temperature

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min	4114/00		7.65	7.65	
15 min		2:57		7.4	
25 min		3:07		7.25	
35 min		3:17		7.25	
45 min		3:27		7.05	
55 min		3:37		7.0	
l hour		3:42		6.9	
1.5 hour		48:12		6.6	
2 hour		4:42		6.4	
2.5 hour		5:12		6.2	
3 hour		5:42		76.05	
3.5 hour		6:12		56.9	
4 hour		6:47		5.65	
4.5 hour		7:12		5.65	
5 hour		7:42		5.55	
5.5 hour		8:12		5.45	
6 hour		8:42		5.35	
6.5 hour		9:12		5.3	
7 hour	1	9:42		5.2	
24 hour	415/00	2:452		4.4	
28 hour	1	6:452		4.4	•
32 hour	J	10:452		4.35	
48 hour	4/16/00	2:452		4.3	
52 hour	\Box	6:42		4.3	
56 hour	0	10:42	1	4.3	

B. top. of missing = 23 top. of miniscos = 7.65

(glass cones)

Battelle Test Plan: BNFL-TP-29953-073

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Target	Date	time	ambient tem Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min					
15 min					
25 min					
35 min					
45 min					
55 min					
1 hour		X			
1.5 hour					
2 hour					
2.5 hour					
3 hour					
3.5 hour					
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour					
6.5 hour					
7 hour				/	
24 hour					
28 hour					
32 hour					
48 hour				1	
52 hour					
56 hour					V

Will not sattle PRB 4/4/02

AZ C with Target	Date	time	Total	Solid	Liquid	
5			(ml)	(ml)	(ml)	
5 min						
15 min						
25 min						
35 min						
45 min						
55 min						
1 hour						
1.5 hour			1			
2 hour						
2.5 hour						
3 hour						
3.5 hour						
4 hour						
4.5 hour		***************************************			 	111 010 1
5 hour						w.11
5.5 hour						- H-
6 hour						w:11 N. + Settle 4/4/6
6.5 hour						41410
7 hour						7/71
24 hour						
28 hour				+	1	
32 hour		¥.			 	
48 hour			-	+	 	
52 hour						
56 hour						

centrifige cars 22) Place the graduated cylinders in an oven at 50°C (±5°C) for 1 day. Remove the samples and record the mass and volume. after Rhol-5A - 15 A 3 days@ 50°C AZ B 76.326 27.712 29.018 Total Total Total Tare 19.87 19.968 19.777 Tare Таге g 7.744 Slurry Slurry Slurry Volume 7.6 Volume Volume ml ml 1-1.02 1,20 P= 1.11 relus 15 B 25 A 77.189 Total 26361 19.848 20.095 19.836

PR Bredt 12/6/99

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23) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

01 1 - 1			
AZA	Time _9:00a2	Date_ 5/2/00	
AZB	Time	Date	15 7 25 wt% will
AZC	Time	Date	not settle
Deturn the a	endusted exilinders to the ever	-+ 50°C	4/11/00

24) Return the graduated cylinders to the oven at 50°C.

25) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

Rhol:5A

AZ A without glass formers at 50°C

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min	5/2/00	9:30	7.8	7.5	0.3
60 min		10:00	7.8	7.4	0.4
90 min		10:30	7.8	71	0.7
120 min		11:00	7.8	7.0	0.8
150 min 180 min		11:30	7.8	6.8	1.0
		12:0-	7.8	6.6	12
210 hour ??		12:30	7.8	6.5	1.3
240 hou r 🐪		1:00	7.8	63	15
270 hour .:		1:30	2.8	6.2	1.6
300 hour A	1	2:25/10	7.8	5.9	1.9
24 hour	5/3/00	9:30	7.8	4.8	3.0
28 hour	1	11:50	7.8	4.7	3.1
32 hour	<u> </u>	3:15	7.6	4.7	3.1
48 hour	5/4/00	8:00	7.8	4.7	3./
52 hour		1:00	7.8	4.7	3.1
56 hour	V		7.8	4.7	2.1

tot 1-78-1 togofmeniscus 7.6 Bitton of maniscus PR Bredt 12/6/99

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Fut% cones

23) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

AZA Time 9:00am	Date_ 5/2/00	
AZ B Time	Date	15 2256t% 1511
AZ C Time	Date*	Not SHL PRB

24) Return the graduated cylinders to the oven at 50°C.

25) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

Rhu.15B

AZA without glass formers at 50°C

Target	Date	time	Total (ml) /16	Solid (ml)	Liquid (ml)
30 min	5/2/00	9:30	6.297.3	6.6	
60 min	1	10:00	T	6.5	
90 min		10:30		6.3	
120 min		11:00		6.2	
150 min		11:30		6.05	
180 min		12:00		5.95	
210 hour	1 2 2 2	12:50		5.8	
240 hour		1:00		5.7	
270 hour		1:30		5.6	
300 hour		2:96,00		5.3	
24 hour	5/3/00	9:30		4.7	
28 hour		11:56		4.6	
32 hour	1	3:15		46	
48 hour	5/4/00	8:00am		4.5	
52 hour		1:00/		4.5	
56 hour	7		V	4.5	

top of manscos: 6.7ml
Better of maiseus: 6.7ml

1

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4 7	D	without	alaca	formers		5000
AΔ	D	without	giass	iormers	at	50°C

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min					` '
60 min					
90 min					
120 min			J-11 (8)		
150 min					
180 min					No. year.
210 hour					1
240 hour					Have T
270 hour					
300 hour	1		100,000		10000
24 hour	- 1				
28 hour			E 100 S. 00		10.00
32 hour					
48 hour					
52 hour					
56 hour		1			

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min			1		1
60 min	1 1 1		1.		
90 min					
120 min					
150 min		1			
180 min				/	- 1
210 hour				1	
240 hour					
270 hour					
300 hour					
24 hour		1			
28 hour				1	
32 hour					1
48 hour					
52 hour					+
56 hour		7			+

will not settle PRB 4/4/00

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Rh.1-25-1

26) If not performed in the last 30 days, analyze one standard between 10 and 100 cP for shear stress as a function of shear rate at 25°C from 0 to 1000 s⁻¹. Print out a copy of the rheogram and attach to this test plan.

Viscometer MS

Location A-Cell 5.2 Geometry MVI

PNL 000

2727"

Viscosity 95.5 CP Lot 1111 99

Manufacturer Context 3/01

Rock Field File name <u>0502004</u> Date analyzed 5/2/00

27) Remove the graduated cylinders from the oven and allow to cool overnight.

28) While stirring the samples on a magnetic stir plate remove subsamples from each of the graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s⁻¹ over 2 minutes and then returning from 300 to 0s⁻¹ over 2 minutes

confined on 4/7/00 with S.A. Print out a copy of the rheograms and attach to this test plan. That 300 5-1 is appropriate 5000 0508004 File name 050800 A Date analyzed mox sher rate PRB AZA Duplicate 0508001File name 050800 Date analyzed 4/11/00 ososo JFile name o 508000 Date analyzed AZ B C-104 Saphs, Not AZ-10-Should be listed under stip 91 AZB Duplicate 050800KFile name 050800E Date analyzed Date analyzed AZC Duplicate 50800 MFile name 550800C Date analyzed

29) Return this material to the respective graduated cylinders.

75) Rince this material Back into sample jars.
30) Also Ringe contests of contrology comes Back into respective jars.

31) Reveigh the sample Jars.

Rh.1-25-1 Ahrol-5

32) evaporate samples back to target weights listed under sty in page 6. Record new masses

RL1-15 Rh.1-5

See thechant following

on 6/5/00 +h AZ-102-75-1 was

dilutal to 25 20 wt 6, total mass = 282. to grass 6/5%.

282. to 282. to 282. to 270.1 g

cop and most of meterial most from Rhometer mes 1.55 on dick.

total 1.55 = 282.7-270.1 g

= 12.6 g of dilutal

12.6 g · 0.2 solid = 2.5 g 50/50/5

During Rhology on 25°C 20 wt 6 solids

- material struck to siles of Jar

so which to get a good sibsolyte

- Run File

Simple 1 060500A

Sample 2 060500A

Sample 2 060500C

0-300 see-1 our zain

300-0 see-1 our zain

25°C

Pal Brog /5/00

Test Plan 29953-073 Back of Page 14

-	A	8	ပ	٥	В	4	9	Ŧ	_
1	water adjust 052300.xls								
2	36669								
3	Paul Bredt		Slurry wt% solids						
4 4			9.535						
9					Rheol-25-1		Rheol-25-2		
2	Sample	Slurry Basis Rheol-5	s Rheol-5	Rheol-15	For 25 wt%	For 20 wt%	For 25 wt%	For 20 wt%	For 15 wt%
8	Slurry Mass (g)	436.69	41.84	122	136.53	136.53	136.32	136.32	136.32
5	Sr/TRU Precipitate (25 wt% solids basis)	19.21	1.841	5.367	900.9	900.9		5.997	5.997
0	10 Actual Cs Eluant (Diluted Basis)	137.83	13.206	38.506	43.092	43.092		43.026	43.026
-	Actual Tc Eluant (Diluted Basis)	76.67	7.346	21.42	23.971	23.971		23.934	23.934
100	12 Na2B4O7•10H2O	10.76	1.031	3.006	3.364	3.364	3.359	3.359	3.359
<u>ا</u>	IOH•H2O	15.51	1.486	4.333	4.849	4.849		4.842	4.842
14	Va2SiO3•5H2O	32.09	3.075	8.965	10.033	10.033		10.017	10.017
5	15 SiO2 (Sil-co-Sil 75)	39.73	3.807	1:1	12.421	12.421		12.402	12.402
9	16 Sugar (Granular)	1.34	0.128	0.374	0.419	0.419	0.418	0.418	0.418
~ l«					The second secon				
16	nitial solids		=C8*0.0954	=D8*0.0954	=E8*0.0954	=F8*0.0954	=G8*0.0954	=H8*0.0954	=18*0.0954
<u>=</u>	20 Initial Water		=C8-C19	=D8-D19	=E8-E19	=F8-F19	=G8-G19	=H8-H19	=18-119
F	Total water needed	-	=(1-0.05)*C19/0.05	=(1-0.15)*D19/0.	=(1-0.05)*C19/0.05 =(1-0.15)*D19/0.15 =(1-0.25)*E19/0.25	=(1-0.2)*F19/0.2	=(1-0.25)*G19/0.25	=(1-0.2)*H19/0.2	=(1-0.15)*119/0.15
<u>></u>	Vater to add		=C21-C20	=D21-D20	=E21-E20	=F21-F20	=F21-F20 =G21-G20 =H21-H20 =I21-I20	=H21-H20	=121-120
No.	Vajusted mass		=C8+C22	=D8+D22	=E8+E22	=F8+F22	=G8+G22	=H8+H22	=18+122
4 B	3ottle Tare		134.58	134.16	217.49	217.49	217.5	217.5	217.5
5	Total Target		=C24+C23	=D24+D23	=E24+E23	=F24+F23	=G24+G23	=H24+H23	=124+123

to deticatine the water orgained
to reach the chiral specified

whis solids values.

food Bree-

ELO-ES602 -11

Glass formulations in this report for AW-101 and AN-107 are considered to be proprietary by VSL/Duratek

water adjust 052300.xls 5/23/2000 Paul Bredt						5	-	-
5/23/2000								
		Slurry wt% solids	% solids		***			
		9.535			. 2			
				Rheol-25-1		Rheol-25-2		
Slun	Slurry Basis	Rheol-5	Rheol-15	For 25 wt%	For 20 wt%	For 25 wt%	For 20 wt%	For 15 wt%
Slury Mass (g)	436.69	41.84	122	136.53	136.53	136.32	136.32	136.32
Sr/TRU Precipitate (25 wt% solids	19.21	1.841	5.367	900'9	900.9	5.997	5.997	5.997
Actual Cs Eluant (Diluted Basis)	137.83	13.206	38.506	43.092	43.092	43.026	43.026	43.026
Actual Tc Eluant (Diluted Basis)	76.67	7.346	21.42	23.971	23.971	23.934	23.934	23.934
Na2B407•10H20	10.76	1.031	3.006	3.364	3.364	3,359	3.359	3.359
	15.51	1.486	4.333	4.849	4,849	4.842	4.842	4.842
14 Na2SiO3•5H2O	32.09	3.075	8.965	10.033	10,033	10.017	10.017	10.017
SiO2 (Sil-co-Sil 75)	39.73	3.807	11.1	12.421	12.421	12.402	12.402	12.402
16 Sugar (Granular)	1.34	0.128	0.374	0.419	0.419	0.418	0.418	0.418
•		,	,					
		14						
		3.992	11.639	13.025	13.025	13.005	13.005	13.005
		37.848	110.361	123.505	123.505	123.315	123.315	123.315
Total water needed		75.839	65.953	39.075	52.100	39.015	52.020	73.695
		37.991	-44.408	-84.430	-71.405	84.300	-71.295	-49.620
Adjusted mass		79.831	77.592	52.100	65.125	52.020	65.025	86.700
		134.580	134.160	217.490		217.500		217.500
		214.411	211.752	269.590	(282.615	269.520	282.525	304.200

270-82865 .119 425+ 676/8 484 NFL- 29953-073

Glass formulations in this report for AW 101 and AN-107 are considered to be proprietary by VSI / Duratek

| Section 25 | m. fr.: a) 242.515g \$ 282.525 5.997 43.026 123.315 23.934 3,359 4.842 12.402 0.418 52.020 65.025 217.500 10.017 -71.295 loss of sone For 25 wt% For 20 wt% as described instrution 39.015 -84.300 52.020 217.500 269.520 136.32 5.997 43.026 23.934 3.359 13.005 4.842 12.402 0.418 10.017 Rheol-25-2 -40.153 70.158 217.490 287.648 19.367 2.718 3.918 4.853 8.106 10.036 0.338 10.524 99.787 59.634 test Colcolotions I performed following For 15 wt% Rheol-25-1 after spill サナナ 270.108) 34.817 19.36Z 2.718 3.918 8.106 0.036 0.338 99.787 42.095 -57.693 52.618 10.524 110.31 for 20wt% 12.421 13.025 123.505 52.100 -71.405 65.125 217.490 282.615 136.53 6.006 43.092 23.971 3.364 4.849 10.033 For 20 wt% 3/~~5 39.075 -84.430 52.100 217.490 269.590 3.364 4.849 10.033 13.025 12.421 For 25 wt% Rheol-25-65.953 -44.408 77.592 134.160 211.752 21.42 3.006 4.333 8.965 11.639 5.367 8.506 11.1 Rheol-15 46.127 i Slurry wt% solids 9.535 37.848 75.839 37.991 79.831 1.486 41.84 3.807 0.128 3.992 214.411 .841 Rheol-5 436.69 19.21 137.83 76.67 10.76 32.09 39.73 1.34 Slurry Basis Sr/TRU Precipitate (25 wt% solids basis) Actual Cs Eluant (Diluted Basis) Actual Tc Eluant (Diluted Basis) SiO2 (Sil-co-Sil 75) Total water needed Na2B40710H20 Sugar (Granular) Slurry Mass (g) Na2SiO35H2O Adjusted mass Bottle Tare Water to add water adjust 052300.xls Initial Water Total Target Initial solids LIOHH20 3 Sample Paul Bredt

Sluing Mass

SI/TRU

Slurry

water

AN-107 Sr/TRW for AZ-102

The AN-107 SI ITRU was tested for Wt 6 Solids under Test Instruction BNFL-TI-29953-079-1 Rev 1 addendum 6. The util solids were determined to be 46.26%. Thèse solds were Jar "AN-107 DF Solids". This jar tare is During with solids work, the jer weighed 227.84 227.84 - 217.309 = 10.53 g The jer wighed on 5/25/00 226.642 726.64 - 217.309 = 9.33 g So... Values for SrITRU 9.33 Adition to AZTOZ weed to be corrected by 10.53 = 0.886 In appointing addintion to TP 29953-079 the miss to edd to AZ-10Z Field was 10.38 This should Now be 10.38; 0.886 = 9.20 New solids content is 52.20 wt% The Following table is to be used for the addition of SI ITRU += AZ-102 samples in grans. SITRU solils will be added and supplimented with water. Slurry Busis Rheol-5 | Rheol 15 | Rheol 25-1 | Rheol 25-2 436.69 41.84 122.00 136.53 136.32 20 × 4626/25=17.02 1.63 4.75 5.32 PRB 9.20 x 52.20/25 = 19.21 1.84 5.37 6.01 6.00 5/25/00 9.20 2.57 2.881.33 0.88 SI/TRU 30/45 2.87 2.18 Calculations of Method reviewed by Achi PRO 10.01 5/25/00 Harry V. Smills 5/2/00

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30) Add the BNFL prescribed quantity of intermediate waste products to each of the three graduated cylinders and stir for 1 hour. Use the space below to record the quantity of intermediate waste products added and the time and date stirring started and stopped.

Rhol-5 AZA Stir Start (time/date) 10:15 Stir Stop (time/date) 10:48

Source Chemical	Target wt%	Amount (g)	Actual Added (g)
Actual ST/TV		0.88(0)	0.872
Glass folper mix		7.5270	9,454
How for softru		0.96	Sic belog
170 total		2.019	2.25
			0
Mr. S. S. Levinson and M. S. S.			

Rhed-15
AZB Stir Start (time/date) 11:20 Stir Stop (time/date) 11:55

Source Chemical	Target wt%	Amount (g)	Actual Added (g)
Actual St Aru		2,5700	2.495
Glass Former Mix		27.778	27.428
Hzo for Sr/Fro		2.80	SEE below
Hzo total		5.053	5.06
No.	2 2		
	1 6		

314,290 314,290 315,162 Att. G.F. 324,616 0.9 + 0.96 + 70. 323,736 325,436

> 211.73 Stort word 5 211.340 Stort word 5 213.835 Stort wix add 213.835 Stort wix add 213.835 Stort wix add 213.835 Stort word 5 St

120	1-25	
10	1- (-)	

AZE	Stir Start (time/date)	Stir Stop (time/date)

Source Chemical	Target wt%	Amount (g)	Actual Added (g)
· ne Lu		er descent and	
2	NECTOR OF THE		n.t no

3 N Cap	the gra	duated cy	linders	and reco	ord the n	nass and	volume.

	AZ A	AZ B		AZ C	
Total	g	Total	g	Total	g
Tare	g	Tare	g	Tare	g
Slurry	g	Slurry	g	Slurry	g
Volume	ml	Volume	ml	Volume	ml

32) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

I ime		Date			
Time		Date			
Time	b broken o	Date			
		DATE STORY	1 Control	ted con	tritige con
		Not	and Courses	1. Sac	008
		Nu	PRE		5/3/
	Time	Time	Time Date	Time Date	Time Date

91.FZ

Bredt, Paul R

From: Sent:

Stuart Arm [sarm@bnflinc.com] Tuesday, May 23, 2000 9:56 AM

To:

Bredt, Paul R

Cc: S

Smith, Gary; Morrey, Eugene V; Kurath, Dean E; Jagoda, Lynette K

Subject:

Re: Sr/TRU Simulant

Paul.

Yes, please proceed as you describe.

Thanks, Stuart.

"Bredt, Paul R" wrote:

Stuart,

We had planned to repeat the AZ-102 25wt% rheology at 50°C. We could omit this data point (25°C results are coming out similar to 50°C) and instead run the sample diluted at 20wt%.

If this sounds acceptable, please confirm this summary of modifications:

1) Omit the AZ-102 25wt% rheogram at 50°C

- 2) Dilute the AZ-102 25wt% sample to 20wt% and analyze for shear stress versus shear rate at 25°C
- Omit AZ-102 25wt% sample from glass former addition testing.

Use AZ-102 15 wt% sample for mixing and aging study

5) Leave C-104 testing as planned with 25wt% sample for mixing and aging study.

Thanks,

Paul

----Original Message-----

From: Stuart Arm [SMTP:sarm@bnflinc.com]

Sent:

Tuesday, May 23, 2000 9:41 AM

To: Bredt, Paul R

Cc: Smith, Gary; Morrey, Eugene V; Kurath, Dean E

Subject: Re: Sr/TRU Simulant

Paul,

Please conduct the mixing and aging study with the 15 wt% slurry and dilute the 25

wt% slurry to 20 wt% and determine the yield stress and viscosity (if no cost impact).

Thanks,

Stuart.

"Bredt, Paul R" wrote:

Stuart,

We have finished the AZ-102 and C-104 melter feed testing (no glass formers or

secondary waste products). The table below summarizes some of the rheology results at 25°C. Data at 50°C is virtually identical. We are becoming a bit concerned about adding glass formers to the AZ-102 25wt% sample. This may become too thick to handle (it is almost already too thick to handle). Do you want us to continue as planned with mixing and aging studies on the 25wt% AZ-102, or switch to the 15wt% sample? My feeling is we may want to eliminate the AZ-102 25wt% sample from the test matrix altogether or dilute it down significantly given this rheology data.

Thanks, Paul

Sample Yield Stress (Pa) Viscosity 100 s-1 (cP) C-104 5wt% < 0.5 <5 C-104 15wt% 0.5 6 C-104 25 wt% 6 63 AZ-102 5wt% 0.5 7 AZ-102 15wt% 200 15 AZ-102 25 wt% 190 2000

----Original Message-----

From: Stuart Arm [SMTP:sarm@bnflinc.com]

Tuesday, March 14, 2000 3:14 PM Sent:

To: Bredt, Paul R

Subject: Re: Sr/TRU Simulant

Paul,

Use 25 wt% solids concentration (this should be the same as the waste).

Stuart.

of

"Bredt, Paul R" wrote:

Stuart.

As we discussed a few weeks ago, we have made a Sr/TRU precipitate simulant from

the AN-107 simulant. We are having this analyzed by ICP and should have results

in a week or so. Based on the VSL formulation, we plan to add 25.674 grams

this Sr/TRU precipitate on a dry basis for every 400 g C-104 waste (20wt%) during the rheological testing.

Question: What wt% water should we shoot for in the Sr/TRU precipitate?

(i.e. how much water should we use to suspend our 25.674 grams of precipitate)

Thanks,

Paul

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33) After turning off the stirrer, record the ambient temperature, volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient____°C

AZ A with waste products at ambient temperature

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min					
15 min					
25 min					
35 min					
45 min					
55 min					
1 hour					
1.5 hour					
2 hour					
2.5 hour					
3 hour				1	
3.5 hour					uncil
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour					V
6.5 hour					
7 hour					
24 hour					
28 hour					
32 hour					
48 hour					
52 hour		The Land			1484
56 hour					

51 Step 94 513/100 5/3/100

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Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
5 min		1	()	(111)	(1111)
15 min				+	
25 min		-		-	
35 min					
45 min				+	
55 min					
1 hour					
1.5 hour					
2 hour					
2.5 hour					
3 hour					
3.5 hour					
4 hour					
4.5 hour			\		
5 hour					
5.5 hour					
6 hour					
6.5 hour					1
7 hour					
24 hour				1	
28 hour					
32 hour					
48 hour					
52 hour					
56 hour				1	

5 - 5 PRB 100

AZ C with waste products at ambient temperature

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min					
15 min					
25 min					
35 min			194	12	
45 min					
55 min					
1 hour					
1.5 hour				1	
2 hour					
2.5 hour					
3 hour					
3.5 hour					
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour					
6.5 hour				No.	
7 hour					
24 hour				1	
28 hour					
32 hour			100		
48 hour					
52 hour					
56 hour					

34) Place the graduated cylinders in an oven at 50°C (±5°C) for 1 day. Remove the samples and record the mass and volume.

	AZ A	AZ B		\ AZ C	
Total	g	Total	g	Total	g
Tare	g	Tare	g	Tare	g
Slurry	g	Slurry	g	Slurky	g
Volume	ml	Volume	ml	Volume	ml

35) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

AZ A	Time	Date	
AZ B	Time	Date	
AZ C	Time	Date	

See Stel 31

36) Return the graduated cylinders to the oven at 50°C.

37) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min			, ,	1, /	1
60 min					
90 min					
120 min					
150 min					
180 min					1
210 hour					
240 hour					
270 hour			1		
300 hour					
24 hour					
28 hour					1
32 hour					
48 hour					1
52 hour			1		
56 hour				1	

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min				()	()
60 min					+
90 min					4
120 min					\wedge
150 min				46-4	
180 min					
210 hour					
240 hour				100	+ \
270 hour			-		
300 hour		1			
24 hour					
28 hour					·
32 hour					
48 hour					+
52 hour					
56 hour					

Not Norskl 31

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Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min	\				
60 min					
90 min					
120 min					
150 min					
180 min					
210 hour		X			
240 hour					
270 hour					
300 hour					
24 hour					
28 hour				10:	
32 hour					
48 hour					
52 hour			\		
56 hour					

38) If not performed in the last 30 days, analyze one standard between 10 and 100 cP for shear stress as a function of shear rate at 25°C from 0 to approximately 1000 s⁻¹. Print out a copy of the rheogram and attach to this test plan.

Viscometer	-	Location	Geometry
Viscosity	cP	Lot	Manufacturer
File name		Date analyzed	

- 39) Remove the graduated cylinders from the oven and allow to cool overnight.
- 40) While stirring the samples on a magnetic stir plate remove subsamples from each of the graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s⁻¹ in 2 minutes and then returning from 300 to 0s⁻¹ in 2 minutes. Print out a copy of the rheograms and attach to this test plan.

-	
File name	Date analyzed
	File name File name File name

5- 34 pp 31 (00)

12/6/99			Вап	elle Test Plan: Br	NFL-TP-29953-073
				•	Page 22 of 60
AZ © Dup1ica	ate File name	Da	ate analyzed		
41) Return this	s material to the resp	ective graduated	d cylinders.		
\	\				-
for 1 hour.	NRL prescribed quar Use the space belo	ntity of glass for	mers to each of the	e three graduated	cylinders and stir
stirring sta	irted and stopped.	to record the c	qualitity of glass it	officis added and	the time and date
A 7 A Stin St	(: (À)	C: C: (
ALA SIII SI	art (time/date)	Stir Stop (time/date)		
		ass Formers:			
Source Chemical	Manufacturer	Lot#	Target wt%	Amount (g)	Actual Added
Chemical		\		-	(g)
			<u> </u>		
	-		1		
			1		
			1.	10	
			+		

PR Bredt 12/6/99					NFL-TP-29953-073 Page 23 of 60
AZ B Stir's	tart (time/date)	Stir Sto	op (time/date)	Charles In	
		Glass Formers			
Source Chemical	Manufacturer	Lot#	Target wt%	Amount (g)	Actual Added (g)
		100 82			
		 	7_ 401 7 105		
					1
		\			
			1.		-) -)
		1			
AZ C	C	lass Formers			
Source Chemical	Manufacturer	Lot#	Target wt%	Amount (g)	Actual Added (g)
			<u> </u>		
					•
			 		
				4	
				Λ	

5 ch 18 100

43) Cap the graduated cylinders and record the mass and volume.

	AZ A	AZ B		AZ C	
Total	g	Total	g	Total	g
Tare	g	Tare	g	Tare	g
Slurry	g	Slurry	g	Slurry	g
Volume	ml	Volume	ml	Volume	ml

44) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

AZ A	Time _	Date
AZ B	Time _	Date
AZ C	Time _	Date
		lac

- 500 kg q 4 - 60 kg | 10 kg |

45) After turning off the stirrer, record the ambient temperature, volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient___°C

AZ A with glass formers at ambient temperature

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
5 min		1			s de ties
15 min		1			
25 min			\		63 1.12
35 min			1		
45 min	•				
55 min					
1 hour					9 4
1.5 hour					
2 hour					
2.5 hour				777	
3 hour					
3.5 hour	100			1	
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour				1	
6.5 hour					
7 hour					1
24 hour					
28 hour					
32 hour					
48 hour					
52 hour					
56 hour					

See 5/2/100 8/3/100

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AZ B with	formers at ambient temperature				
Torgot	Data	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \		17.1	

Target	Date	time	Total	Solid	Liquid
5 min		\	(ml)	(ml)	(ml)
	ļ	1			
15 min					
25 min					
35 min		_ \			
45 min					
55 min			1		
1 hour					
1.5 hour					
2 hour					
2.5 hour					
3 hour		- A			
3.5 hour				7	
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour		,			
6.5 hour					
7 hour				1	
24 hour					
28 hour					
32 hour					
48 hour					
52 hour					1
56 hour				-	1

5 ph 3 100 -

Target	Date	· time	Total (ml)	Solid (ml)	Liquid
5 min					
15 min					
25 min					
35 min				1/	
45 min				/	

52° 64 5/31/00

Target	Date	· time	Total	Solid	Liquid
<i>6</i> !	 		(ml)	(ml)	(ml)
5 min		-			4
15 min					
25 min					
35 min					
45 min					
55 min					
1 hour					
1.5 hour					
2 hour					
2.5 hour					
3 hour					
3.5 hour					
4 hour		1/			
4.5 hour		/			
5 hour	/				
5.5 hour					
6 hour					
6.5 hour					
7 hour /					1
24 hour/					
28 hour				1	-
32 hour					
48/hour					
\$2 hour	¥2				
56 hour		T			

46) Place the graduated cylinders in an oven at 50°C for 1 day. Remove the samples and record the mass and volume.

AZ A		AZ B		AZ C	
Total	g	Total	g	Total	g
Tare	g	Tare	g	Tare	g
Slurry	g	Slurry	g	Slurry	g
Volume	ml	Volume	ml	Volume	n
				á .	GI

See step 94

Samples analyzed with
a batch of Cloy samples
and data is recorded
to gether PRB
18/10/00

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47) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

Time ____ Date AZR Time _____ AZ C Time Date

48) Return the graduated cylinders to the oven at 50°C.

49) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min			1	()	- ()
60 min					
90 min					
120 min					
150 min					
180 min					
210 hour			1		
240 hour			1		
270 hour				1	
300 hour					
24 hour				+	
28 hour					
32 hour					
48 hour					1
52 hour					
56 hour					4

Sec step 4/2

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min					1
60 min					
90 min					
120 min					
150 min					+
180 min					
210 hour	1				
240 hour		1			
270 hour	P	1			
300 hour					
24 hour					
28 hour				1	
32 hour					
48 hour		1			
52 hour					+
56 hour		1			+

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min			1	()	(111)
60 min					
90 min			 		
120 min			 		
150 min				1	
180 min	1		1	1	
210 hour				1	
240 hour				1	
270 hour					
300 hour		1			
24 hour				1	
28 hour				+ +	
32 hour				1	
48 hour					\
52 hour					
56 hour					+

See sty 46

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50) If not performed in the last 30 days, analyze one standard between 10 and 100 cP for shear stress as a function of shear rate at 25°C from 0 to approximately 1000 s-1. Print out a copy of the rheogram and attach to this test plan.

Location A-CI Geometry & MILT Viscometer H.k. MS Viscosity 95.5 cP Lot 111199 Manufacturer Broskfield

File name 66010cA Date analyzed 6/11co

51) Remove the graduated cylinders from the oven and allow to cool overnight.

52) While stirring the samples on a magnetic stir plate remove subsamples from each of the graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s⁻¹ in 2 minutes and then returning from 300 to 0s⁻¹ in 2 minutes. Print out a copy of the rheograms and attach to this test plan.

File name _____ Date analyzed AZ A File name _____ Date analyzed AZ A Duplicate File name AZ B Date analyzed 50°C 50°C 50°C 156°C 060700C File name _____ Date analyzed AZ B Duplicate AZ C File name ____ Date analyzed AZ/C Duplicate File name _____ Date analyzed 53) Return this material to the respective graduated cylinders.

54) Assemble a mixing vessel using the following parts or equivalent. Attach impeller to a stirring motor capable of maintaining a constant rotational rate from 100-1400 rpm.

Part	Vendor	Catalog number	
500 ml O-ring Sealed Kettle, 3.75 inch OD, 5 3/8 inch flange	Labglass	LG-8071-100	
Clamp	Labglass	LG-7316-106	
O-ring	Labglass	LG-1022-476	
Kettle top with three 24/40 necks	Labglass	LG-8072-100	
2 3/8 diameter 4 blade impeller	Fisher Scientific	14-505-20G	

The 168.05 g Labeled "1"

Con to hold round bottom 67.76 g Labeled mix

Stopper Labeled "1" 15.45 g

168.19 for vessel	3-6481
PR Bredt 12/6/99 PR Bredt 12/6/99 322.6 + 34 + 6 Battelle Test Plan: 322.6 + 34 + 6 Battelle Test Plan: 322.5 Transfer the sample specified by BNEL to the mixing vessel (do not transfer the	BNFL-TP-29953-073 Page 31 of 60
55) Transfer the sample specified by BNFL to the mixing vessel (do not transfer the which sample was transferred as well as the day and time transferred below.	stir bar). Record
Sample transferred A2-/32 Rhal-25-2 Date 6/13/99 Time 9:30an	<u> </u>
and speed below. vsch NON. INNL NEST trackle Technology Fig. 200 05-028-24 sec. 2 L 710985	cord the time, date
Speed 32/ rpm Date 6/11/00 Time 2:10pm To click al, I held to the Floringth lamps and red 720 57) After 1 hour of stirring, remove a sample through the sampling port and immediate shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C Print out a copy of the rheograms and attach to this test plan.	ately analyze for former my C from 0 to 300 s ⁻¹ .
Run 1 File name <u>06/900 A</u> Date analyzed <u>6/19/00</u> 3:16	Pr~
Run 2 File name 061900 B Date analyzed 6/19/00	
58) After 1 day of stirring, remove a sample through the sampling port and immedia shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C Print out a copy of the rheograms and attach to this test plan.	tely analyze for C from 0 to 300 s ⁻¹ .
Run 1 File name 06 2000 A Date analyzed 6/20/00 Run 2 File name 06 2000 B Date analyzed 6/20/60	
Run 2 File name 06 2000 B Date analyzed 6/20/63	
59) After 1 week of stirring, remove a sample through the sampling port and immediahear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C Print out a copy of the rheograms and attach to this test plan.	
Run 1 File name obletoo Date analyzed 6/26/00	of the to target by
Print out a copy of the rheograms and attach to this test plan. Run 1 File name <u>662606</u> Date analyzed <u>6/26/00</u> Run 2 File name <u>062606</u> Date analyzed <u>6/26/00</u> 60) After removing the last sample (after 1 week of stirring), transfer the sample back of the sample of the sample back of the sampl	الم الم
60) After removing the last sample (after 1 week of stirring), transfer the sample bac cylinder. Record sample ID, volume and mass of material.	k to the graduated
AZ-12 3 1/2010 Slory mass 8	1.12
Total g Total 00 ml Tare 217.61 g Solids 20 ml Slurry g Liquids 20 ml	36.73 11.13 7.63 35.41 = together
61) Focus a video camera on the solids-liquid interface of the sample and collect vide taking care not to disturb the sample. Report any observed gas retention and/or rethe cognizant scientist.	eo for one week
62) After the sample has remained undisturbed for 1 week, remove the standing liqui	d using a glass
· SEMPLE IN JOY agitated on 7/20/00@ 2:020	m 21 C 212
- Semple in jor agitated on 7/20/00@2:02 p - Semple in jor agitated on 7/20/00@2:02 p - 7/25/00 5-1:15 -+ 92 of mark, recorded interference on 7/26/00 solids of 92 of mark, mo retained Bubbles of 1/27/00 solids @ 291-92 mark - no bubbles @ 291-92 mark - no bubbl	bks abserved -

PR Bredt 12/6/99

Battelle Test Plan: BNFL-TP-29953-073

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pipette:

63) Gently collect a subsample of the settled solids and immediately analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C from 0 to 300 s⁻¹. Print out a copy of the rheograms and attach to this test plan. Run 2 File name 072800 B Date analyzed 7/28/w
072800 C

		•	ind tron	a vin Tas	~ · ~ 4/27/	٠٠.	9
		ks . 12 " & . 12	4 washer	l solids R	he-1 - 5"		
DD D .	104 5	101811	1	Vi-	-25-1		
PR Bredt 12/6/99	Samp	4,5		Battelle Test	Plan: BNFL-TP	-29953-073	
12/0/99	4	weightsale m Indum 1 1:5	of availal	ole, but TI	PBNF4-29953	ige 33 of 60	
•	a di	Indon 1 1:5	+ Masse	s es fol	11.05	14 Rev. 1	
C-104			-5,17.	45 -1	25-1, 8:	5.0.	
64) Bassada	L 1' 1		-15, 51	· Fg - 2	15-1, 8: 5-2, 8.	c 30	
04) Record t	ne solias concen	tration of the C-104	feed.		, 0.	7	
	Wt% solids=	20 (CI	l) Data	Source TP-29	953-79 Rev.	1	
		`					
65) Record to	he Wt% solids ta	rgets provided by E	BNFL.	DUL TO 12	to New J	2073,54	->h
	337407 11 1	6	1 - 1 - 144				
	Wt% solids =		(C2a)		133	(3)	
	Wt% solids =	. 15	(C2h)				
	W C/O Solids		(C2b)	_ , _ ,	134	1.2137	
	Wt% solids =	16	(C2c)	10425	-1 135	1.2422	
		4		C104 35	-1 135	95 58	
66) Doad 8 m	il of C-104 mate	rial into 5 preweigh	ed centrifuge	cones. Record	the new weight	PKB	/
C 6 1		C6 2		66.3	DI wa-	her used!	24/
do		C0 2		C6 3	wash	to used to	4
Total	g	Total	g	Total	σ	New Jars	
Cone	g	Cone	s	Cone	S	•	
Slurry	g	Slurry	g	Slurry	g		
C6 4		C6 5					
001		C0 3					
Total	g	Total	g				
Cone	g \	Cone	g				
Slurry	g	Slurry	g				
67) Remove t	the cans, and place	ce the centrifuge co		16			
evaporati	on, place the jar	in an oven at 50°C	(+10°C)	um jar. II neces	ssary to accelerat	e	
68) At interva	als determined by	y the cognizant scie	entist, remove	the cones from	the vacuum jar,	replace the	
caps, and	record the new	weight.				\$2000 B 1000 CARDAN, TO SECONDO	
C6 1		662		66.3			
Col		C6 2		C6 3			
Total	g	Total	g	Total	σ		
Cone	g	Cone	2	Cone	5 g		
Slurry	g	Slurry	g	Slurry	s		
C6 4		06.7	. /				
C6 4		C6 5			ctep 3	>	
Total	g	Total	g	500	stp 3	4/24/00	
Cone	g	Cone	s g		PKL	1/2/100	
Slurry	g	Slurry	g				
69) Centrifug	e the cones at ~1	000 x g for one hou	ur. Record the	e solids and liqu	uld volumes.		

PR	Bredt
12/	6/99

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									450 5 1 01 00	
1	C61			C6 2			C6 3			
	1.			C0 2			C03			
Total		ml	Total		1	T-4-1		1000		
Solid		ml	Solid	*	ml	Total		ml		
Liquid	_			-	ml	Solid		ml		
Liquid		ml	Liquid	-	ml	Liquid		ml		
	C64			C6 5						
Total		ml	Total		ml					
Solid		m)	Solid		ml					
Liquid		m	Liquid		ml					
	5.7.5.0196.411-12	1		1-			*)			
70) Dec	cant the centrifu	ged liau	idto a p	reweighed or	aduated c	vlinder Re	cord the m	acc and a	volume of	
lia	uid in the gradua	ated cyli	nden	reweighed gr	addated C	yınıdçı. Re	cord the h	iass allu v	volume of	
		ned eyn	nder /							
	C6 1		/	C6 2		No.	C6 3			
				60.			C0 3			
Total		g	Total		g	Total		~		
Grad	——————————————————————————————————————	5 g	Grad	$\overline{}$		Grad		g		
iquid	:	_5 g	Liquid	_	g	Liquid		g		
iquid		5 ml	Liquid		g ml	The second secon		g		
nquiu		_''''	Liquid		—m	Liquid _		ml		
	C6 4			C65				3		
							1	1	124/00	
otal		_g	Total		g \		. 57			
rad		_5 g	Grad		s \	52	_	RB	. /	
iquid		_5 g	Liquid		5 g		1	"4)	124/00	
iquid	6 8/100/100/100/100/100/100/100/100/100/10	_s ml	Liquid		s ml			" /		
rquiu			Liquid			\				
71) Bac	ed on the recult	a from (76 1 4b			chen Statistical Victor of Madera III				
i i j Das	sed on the result	s Hom (ugn Co 5, de	termine th	e amount o	i water on	a wt% ba	asis to	
eva	porate from the	inree sa					ions. Atta	ch the cal	culations to	
tnis	Test Plan.			see at	Heche	٦	2			
2) 117			,			U use o				
11 11/-	L 4 4 L									

72) Weight three appropriately sized glass graduated jars or cylinders labeled C6 EVAP A, C6 EVAP B, and C6 EVAP C.

ENGINEERING WORKSHEET

Prepared By: Paul Bredt Date: 4/24/00 Project: BNFL 29953

6-104 Eugention under stop 71 of Test Plan 29953-073

Samples were prepared under
BNFL-TI-29953-79 Rev. 1 addenden /
Solids content is 20 wt% under

Test plan 29953-79 Ru. 1

5 wt is sample:

8 with miss = 17.4 g

6, m = Cz Mz

5 x = 17.4 g

8 sample spilled 5/1/00

PRB

8 x = 69.6 g = New miss torget

15 wt: 5-npk:

Corrent mass = 51.1 g

X = 51.1.20

X = 68.1 g

25-1 25 wt & sangle:

x = 85.0.20 = 68.0

25-2 256th somple:

Correct m.ss = 85.2g $X = 85.2 \cdot 20 = 68.2g$

Sut's sample current mis = 25.6715 x = 25.6715.820 = 102.69 g

73) M	leasure the distance betw	een the h	nighest and lowest gradu	uation on the graduated glassware using a	
IU	Jet.			5-pl =1045"5pill 50	
	Highr	nl	4461	O New Sample transformed from "C-104 Romainder"	
	Lown	nl 5	er of	1124/00 Now scaph pland in	
	Distance	cm\	4	1/29/0 " 1045" .~ 5/100	
74) Tr	ransfer the required mass	of mater	rial into the three gradua	ated glassware. glass Jars 4	
	2101695		C10615	C10/425-1 C10/625-	2
	-C6 EVAP A		C6 EVAP B	C6 EVAP C 238.79	
Total Tare	159.563 g 133.1263 g MB	Total Tare	239.36 134.2137 g	Total 237.33 g	3
Slurry	177.66	Slurry		Tare 134.2422 g 133.9558 Slurry 1-55.368 g 104.834	<
	These mass.	s in	chode water used	t to rinse solids	
75) A _l	oply a vacuum to the sam	iples.	during traster	to New Jars. PRB 4/24/00	
76) M	onitor the mass of each s	ample or	n a regular basis to asses	ss the rate of evaporation. If necessary to	
ac	celerate evaporation, pla		r in an oven at 50°C (±1)	0°C).	
	C6 EVAP A		C6 EVAP B	-C6 EVAP C	
Date	5/1100011.	Date	5/1100 @11-	Date 5/1100011an	
Mass	239.36 >5.7y	Mass	239.55	Mass 238.79 = sterting	-
Date	5/1/00@2:30pm	Date	S/1100 @ 2:30,	Date 5/1100 2:30/m	
Mass	233.67	Mass	235.14	Mass 235.87	
Date Mass	5/2/00@4:50 209.08	Date Mass	5/2/00 8:50.	Date 5/2/00@ 8:50 mm Mass 228.07	
			221.2		
Date Mass	5/2/00 @ 1:40pm 203.8	Date Mass	5/2/00@1:40p-	Date 5/2/00@ 1:40/- Mass 220.	
	(5/2/00@9:30)				
Date Mass	202.7	Date Mass	5/3/co 12:00 213.3	Date $\frac{5/3/06}{2/2.8}$	
Date	Final	Date	\$/3/0: 3:25	Date <u>5/3/c</u> 3.21	
Mass		Mass	208.9.	Mass 207.1	
Date		Date /	5/4/00 @ 1 pm	Date 5/4/00@1p~	
Mass		Mass	102.33	Mass /98.15	
tora	+	(F:m1	Fin-1	
2	at				
La. +4C	to edd				

PRP 5/31/00 allition to C-104 samples Water Step 76 under 210425-1 (C10425-Z C1045 C10415 Current mass Total for Stp 76 7/11/00 Forget Mass from stop 72 236.5815 202.3 Rysiad Water 77.018 Adlition New Mass Not reversal after water 9F 77.0 water add-d weighed into 125 d onto sample PRD 5/4/-PRB 5/4/00 C104 25-1 used for density / Settling / Rheology study

C10425-2 to be reserved for Mixing laging staly

DE LET National Brane

12/6/99				_	Page 36 of 60
C6 EVAP A Date	Data	C6 EVAP B		C6 EVAP C	
Mass	Date		Date		
141455	Mass	****	Mass		
Date	Date	-	Date		
Mass	Mass	-	Mass		- PRB
77) When the mass of vacuum and cap	of each of the slurr the sample. Recor	ies reaches the targe d the mass.	ets calculated	above, remove th	PRB S/3/o nem from the
C6 EVAP A		C6 EVAP B		C6 EVAP C	
Total	g Total	a	Total		~
Tare	g Tare	5	Tare		g a
Sluppy	g Slurry	g	Slurry		g
/	5	~ 8 s	Siurry		g contribuse con
with caps or plus	gs. Record the mas	ss and volume of ma	natery sized paterial in each	of the graduated	ated eylinders / 7/08 cylinders. con LS Loylinders. con LS Loylinders. Loylind
Total 27.357	g Total	38.115 Nag	Total	-0 474	used to
Grad 19.7650		19.8639 g	Con Grad	19.9053	g +lis port
Slurry 7.592	g Slurry	8.311 g	Slurry		of tests
Volume 8.0		e 5.05 ml	Volume		ml PRB
72re = 19.765 79) Preweigh 3 teflor	0	9.8039			= 1.13/4 5/4/02
	Α	В		С	7
\ _	g	g	-	g	mess data 1
80) Preweigh 3 appro	opriately sized volu	metric flasks.	12 × 3		mess data 1 suspect. use
		В		0	step 85 PRB 5/11/
	4			С	SEP 85
_	g	g	***************************************	g	PRB 5/11/
81) Place one stir bar mass of the volum	in each of the volumetric flasks. Calc	umetric flasks and fulate the volume of	ill to the mar	k with DI water.	Record the
A	_	В		C	0~
Total	g Total	g	Total		SerAD
Flask ()g Flask	()g	Flask		g 5/31
Bar ()g Bar	()g	Bar		g
Water	g Water	g	Water	8	3
82) Place stir bar A is	n graduated cylind	er C6 A, stir bar B	C6 B, and	stir bar C in C6	c.
	*		0	RB	
	tr 1		e	RB 5/3/00	

12/6/99)						Page 36 of 60
	C6 EVAP A			C6 EVAP B		C6 EVAP C	36B
Date			Date	7	Date	1	
Mass	-		Mass		Mass		
Date			Date_		Date		
Mass			Mass		Mass		- PRB
							- PRB - 5/3/0
	en the mass o				rgets calculated	above, remove th	em from the
	C6 EVAP A					C(FYID C	
	COEVAPA			C6 EVAP B		C6 EVAP C	
Total	***************************************	g	Total		g Total	g	
Tare		g	Tare		g Tare		
Slurry		_g	Slurry		g Slurry		_
				~82			contritize Con
78) If the with	ne samples are h caps or plug	e in glass ja s. Record	ers, tran	sfer them to appr s and volume of	ropriately sized material in each	preweiged gradua of the graduated	ted cylinders PRS cylinders. \$13100
							Constitution
	C4-5 B	P=1.39		C6B (4.15B)	الدارانا الم	26C 2425B	e= 1.151/a /
Total	30.161	.7	Total	~- ~ . /	g Total	27.896	
Grad	19.9815	5 	Grad		g Grad		
Slurry	10.1795	5 g	Slurry		· ·	20.0465 g	1
Volume		s ml	Volume		g Slurry ml Volum		.)
tare			VOIGH		iii voiuiii		
	weigh 3 teflon	coated ma	agnetic s	19-5538 stir bars.		20.0465	1
		A		D			from the second
		Α		В		С	1-6×2 20
	_		g		_g	g	USE muss.
80) Pre	weigh 3 appro	priately siz	zed volu	metric flasks.			
							PRB 5/11/2 Descty red.
		Α \		В		С	N
			g/		_g	g	Deserty redo.
01\ D1			.)				5/23/0
81) Plac	e one stir bar	in each of	the volu	metric flasks an	d fill to the mar	k with DI water.	Record the
mas	s of the volun	netric flask	s. Calc	ulate the volume	of the stir bars	by the displaceme	nt of water.
	Α		-	R		С	
Total		σ	Total		g Total		
Flask	(g)g	Flask		 .	g	
Bar			Bar	@	- (()g	
Water)g	Water			()	
		5	W alti		g Water	g	
	e stir bar A in	oraduated	cylind	er C6 A stir har	B in C6 B and	stir bar C in C6 C	

attach + + 29953-077 /Kb Page ____ of_ 5/3//06

BNFL Melter Feel C-104 Malter Faced (No glass formers or 2st waste proberts)

	N2- H		Inition		
	<u> </u>	104	Metter	Fred	dessity rerva
				Ansint	, 50°C
	massg)	+++1 U/s-nph	50-16	volume (me)	volver (Me)
5 A	4.78	10.04	5.26	5.3	5.3
5 B	4.83	16.35	5.52	5.7	5.75.61RB 5/23/0-
15 A	4.75	10.27	5,52	5.3	5.4
15 B	4.81	10.00	5.19	4.9	4.9
25 A	4.81	11.21	5.8 6.4	5.8	5.9
25 B	4.83	11.01	6.18	5.4	5.5

Loaded into cones on 5/23/00 Read Ambient when cell temperes 34°C @ 2:00pm on 5/23/00

	and p (9/4)	1 50°C P (9/~1)
SA	0.993	50°C p (9/~1) 0.993
5B	0.986	0.986 7
15 A	1.04	1.02
15 B	1.06	1.06
25 A	1.10	1,08
25 B	1.14	1.12

Samples placed: 50°C water Bath at 2:30pm Musual volum of 50°C somples @ 4:00pm

83) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

C45A C6A	Time	Date 5/8/30
C 4 15A C6 B	Time	Date
C475AC6C	Time	Date

84) After turning off the stirrer, record the ambient temperature volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

C 4 5 A Ambient 30.0 °C

C6-A without glass formers at ambient temperature

	Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)	2015/1
_	≶ min	5/8/00	11:1520	8.0	7.8	 	PRB 45/8100
	15 min		11:1520	1			
	25 min		11:35		7.7	1	
	35 min		11:45		7.6		-
	45 min		11:55		7.6		-
	55 min		12:05		7.6	 	
Γ	1 hour		12:10		7.5	<u> </u>	
	1.5 hour		12:40		7.4		-hazy from 7.7 - 7.5
	2 hour		JE 1:10	ψħ. I.,	7.35		
	2.5 hour		1:40		7.35	 	
	3 hour		2:10		~7.3		-h.se
3	3.5 hour		2:40		7.1		Extrap 7.0-7.5 e Top of theze 7.5
Γ	4 hour		3:10		7.0	 	- To f H2 7.5
	4.5 hour	V	3:40		7.0		Lazety 75
Г	5 hour /	8			1.0	 	11.5
Г	5.5 hour						- (,,,
	6 hour						- υς·γ <i>ι</i>
-	6.5 hour						7~3)
-	7/hour						(12)
	24 hour	5/9/00	8:50		5.0		claude to 65
	28 hour	I	11:50		5.0		Sur The W
	32 hour	1	2:30		4.5	1	Cloudy to 6.5 Cloudy to 6.5 Cloudy to 5.0 Cloudy to 5.0 Control (6.7) Contro
-	48 hour	5/10/00	7:50		4.0		1044
:	52 hour	,	4:00	V	4.0		+ clocky to 5.0
:	56 hour				1.0		

1/8 = 50 x vol

83) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

CYSBCGA	Time	Date 5/8/00
C415BC6B	Time	Date
C425BC6C	Time	Date

84) After turning off the stirrer, record the ambient temperature volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient 30.0 °C

C6 A without glass formers at ambient temperature

١	Target	Date	time	Total	Calid		
	larget	Date	time	(ml)	(ml) st	Liquid	-1-1
10	8 min	5/8/00	11:4520	7.373	7.07.0	(ml)	116 5/8/00
	15 min	1	11:25	7.3	7.0		
İ	25 min		11:35	1	6.9		
	35 min		11:45		6.9		
	45 min		11:55		6.9		
	55 min		12:05		6.85		
	1 hour		12:10		6.85		
	1.5 hour		12:40		6.8		← h-ze from -6.9 to 6.8
Ī	2 hour		1:10		6.7		
	2.5 hour		1:40		6.7		
	3 hour		2:10		6.5		
	3.5 hour		2:40		6.5		+ from 6.5-69 h = -
	4 hour		3:10		6.5		etopoffice 6.9 haze
	4.5 hour	4	3:40		6.5		T+1: 6.8
1	hour						*p = 6.5
7	5.3 hour						7''
)[6 hour						7
([6.5 hour						
A	7 hour			-	t/		
	24 hour	5/9/00	8:50		5.04.8		closely to 6.5 at 6.3 at MA 5/8/00
	28 hour	7	11:50		4.8		
	32 hour	4	3:30		4.5		Felosty +6.0
	48 hour	5/10/00	7:55				
	52 hour	L'	4:00	U	4.0 3.5		
	56 hour						

PR Bredt 12/6/99

C425AC415A

Battelle Test Plan: BNFL-TP-29953-073

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solution is not

C6-B without glass formers at ambient to

Target	Date	ormers at an	Total	Solid	Liquid
1 801			A second		Liquid
5 min	-/-/		(ml)	(ml)	(ml)
	5/8/00	11:15	5.05	5.05	
15 min		11:25		5.0	
25 min		11:35		5.0	
35 min		11:45		4.9	
45 min		11:55		4.9	-
55 min		11:1005		4.9	
1 hour		12:10		4.9	+
1.5 hour		12:40		4.8	
2 hour		1:10		4.7	
2.5 hour		1340		4.7	
3 hour		2:10		4.6	
3.5 hour		2:40		4.5	
4 hour		3:10		4.5	
4.5 hour	1	3:40		4.4	
hour					
5.5 hour					
6 hour					
6.5 hour				 	
7 hour				1	
24 hour	5/9/00	8:50		3.6	
28 hour		11:50		3.	
32 hour	U	3:30		3 4	
48 hour	5/10/02	2:55		3.3 3.4 3.3 3.4	
52 hour	7	4:00	→	3 4	
56 hour			00.00	1	

3.7 = 67.3 v.1%

PR Bredt 12/6/99

Battelle Test Plan: BNFL-TP-29953-073

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C415 B

C6B without glass formers at ambient temperature

Target	Date			Solid	Liquid
			(ml)	(ml)	(ml)
5 min	5/8/00	11:15	4.95	4.95	
15 min		11:25	1	4.9	
25 min	-J= 30	11:35		4.8	
35 min		11:45		4.75	
45 min		11:55		4.75	
55 min		12:05		7.75	
l hour	1 4 1	12:10		4.7	
1.5 hour		12:40		4.6	
2 hour		#1:10		4.5	
2.5 hour		1:42		4.5	
3 hour		2:10		4.4	
3.5 hour		2:40		4.4	
4 hour		3:10		4.3	
4.5 hour	1	3:40		4.3	
§ hour					
5.5 hour					
6 hour					
6.5 hour					
7 hour					
24 hour	5/4/00	8:50		3.5	
28 hour		11:50			
32 hour	1	3:30		3,5	
48 hour	5/10/00	7:55		3.4	
52 hour	1	4:00	V	3.4	
56 hour					

solution is Not Hazy

3.4 = 68.7 °s

C425A

C6C without glass formers at ambient temperature

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min	5/8/00	11:15	7.6*	7.6	
15 min		11:25		76	
25 min		11:35		7.6 7.6	
35 min		11:45		76	
45 min		11.55		7.6	
55 min		12105		7.6 7.6 7.6	
1 hour		5/2:10		7.5	1
1.5 hour		12:40		7.5	
2 hour		11/0		7.5 7.5 7.5	1
2.5 hour		1140		75	
3 hour		2:10		7.5	
3.5 hour		2:40		73	1
4 hour		3:10		7.3	1
4.5 hour	1	3:40		7.2	
5 hour					+
5.5 hour					
6 hour					
6.5 hour					
7 hour		17.77			
24 hour	5/8/	8:50		7.1	
28 hour	1	11:50		7.1	
32 hour	1	3:30		7.1	
48 hour	5/10/00	7:55		7.0	
52 hour	1	4:00	1	7.0	
56 hour				1.0	

Battelle Test Plan: BNFL-TP-29953-073

only ~ 0.1 ~ of standing liquid before starting to setting study. This was after ~5 days of sattling.

PRB
5/8/00

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7.6 Let to tal with some material smeared on 5: de IRB 5/8/00

85) Place the graduated cylinders in an oven at 50° C ($\pm 5^{\circ}$ C)for 1 day. Remove the samples and record the mass and volume.

C6A C45A	C415A	C 4 25A	
Total 27.357 g Total Tare 19.7650 g Tare Slurry 7.592 g Volume 7.9 ml	e 19.8039 g	Total 28.457 g Tare 19.9053 g Slurry 8.5517 g Volume 7.8 ml	
P = 0.90 3/22)	0= 1.03 3/20	p- 1.00 g/2	رادر

138

5111/00 5111/00

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C425 B

Target	Date	time	Total (ml)	Solid (ml)	Liquid
5 min	5/8/00	11:15	6.9*		(ml)
15 min	1	11:25	19	6.9	-
25 min		11:35	6.9	L.9	
35 min		11:45	6.8	1 QX	
45 min		11:55	6.8	18	
55 min		12:05	6.8	6.8	1
l hour		12:10	68	6.75	-
1.5 hour		12:40	1	6.7	
2 hour		+2:1:10		6.7	
2.5 hour		1:40		6.7	
3 hour		2:10		6.6	
3.5 hour		2:40		6.6	
4 hour		3:/•		66	
4.5 hour	1	3:40		6.6	
5 hour /				.,,	
5.5 hour					
6 hour		750			
6.5 hour					
7 hour		William Co.			
24 hour	5/8/00	8:50		6.5	
28 hour		11:50		1.5	
32 hour	T	3:30		6.5	
48 hour	5/10/00	7:55		6.5	
52 hour	e'	4:00	-	6.4	
56 hour					

with some netrial small on sides

PRA

5/8/0

some string lifered Now

85) Place the graduated cylinders in an oven at 50°C (±5°C) for 1 day. Remove the samples and record the mass and volume

the mass and volu	me.			-
C45B	c 415	B	C425B	
C6A	C6B	(26C	
26.912	24.404		27.844	
Total 30.16/	_g Total 27.806	g Total	27.896 g	
Tare 19.9815	_g Tare /9.552		20.0465 g	-7076
Slurry 10.1795	g Slurry 8.253		7.8495 g 6	7.7975
Volume	ml \ Volume <u>4.75</u>	ml Volume_	6.6 ml	-0
(p= 0.96	-2/1 P= 1.02	e (P = 1	1.18 2/	
	000	2/m / 3	3/2	()
6.9305 g	1			` /
g .	(, , , ,			
	4.8512			/ .
	1			1.1
				19/10 mes

P	R	Bredt
1	2/	6/99

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86) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After \sim 2 minutes, turn off the stir plate and record the time and date for each of the three samples.

C45A CGA	Time 8:45	Date 5/11/00
C 415A C6 B	Time	Date
(475A C6C	Time	Date

87) Return the graduated cylinders to the oven at 50°C.

88) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

C45A

Target		ormers at 50		10111		_		
laigei	Date	time	Total	Solid	Liquid			
	1		(ml)	(ml)	(ml)			
30 min	5/11/00	9:15-9:3	7.9	7.9				
60 min		9:45	7.9	7.8				
90 min	1.00 m	10:15	7,9	17.8				
120 min		10:75	7,9	7.8				
150 min		11:15		7.8	-			
180 min		11:45		11.0				
210 hours		12:15						
240 hour.		12:45						< >1,0
270 hour		1:15	79	77		Time	total	3011
300 hour.		1:45	7.9	7.75		7:NE 2:45 3:45	79	7.75
24 hour						2:45	7, 1	- 0/
28 hour						3:45	11, 9	11,10
32 hour	5/12/00	4:30	7.8	0.5		= 11dy to 6.2		
48 hour	71-					, , ,		
52 hour	1711							
56 hour	5/15/00	9	0.6	0.6		- (/- /	-	
			7.6	1		- clody to	2.5~	

PR	Bredt
12/	6/99

Battelle Test Plan: BNFL-TP-29953-073
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86) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

C45BS6A	Time 8: 45	Date 5/11/00
c415B C6B	Time	Date
175BC6C	Time	Date

87) Return the graduated cylinders to the oven at 50°C.

88) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

C45 KB 1KB 5/3/00

					_		
Date	time	Total	Solid	Liquid			
	1	(ml)	(ml)	(ml)			
5/11/00	69:15	7.25	7.25		1		
	9:45	7,25					
	10:15	7,25	7.00				
	10:15	7,25	6.80				
	11:15						
	11:35				at a land		
					1		
						1. Ll	< D1.0
	1:15	7,25	6.65		1 ine	1071	
	1:45	7.25			7 2:45	7,25	6.65
			0.00			777	. /
					3:45	1,25	0,163
5/12/00	4:30	7.2	-0.9		- cland 1 = 6		
					3.5 on Lan		
5/15/00	9.~	0.55	0.55		€ c/a./		
	Date 5/11/00	Date time 5/11/00 89:15 9:45 10:15 11:15 11:45 1:45 5/12/00 4:30	(ml) 5/11/00 89:15 7.25 9:45 7.25 10:15 7.25 10:15 7.25 11:85 12:15 1:45 7.25 1:45 7.25 1:45 7.25	Date time Total (ml) (ml) 5/11/00 69:15 7.25 7.25 9:45 7.25 7.25 10:15 7.25 7.00 10:15 7.25 6.80 11:15 7.25 6.65 1:45 7.25 6.65 5/12/00 4:30 7.2 -0.9	Date time Total Solid (ml) (ml) 5/11/00 89:15 7.25 7.25 9:45 7.25 7.25 10:15 7.25 7.00 10:15 7.25 6.80 11:15 7.25 6.65 1:45 7.25 6.65 5/12/00 4:30 7.2 -0.9	Date time Total Solid Liquid (ml) (ml) (ml) 5/11/00 69:15 7.25 7.25 9:45 7.25 7.25 10:15 7.25 0.80 11:15 7.25 6.65 12:45 7.25 6.65 1:45 7.25 6.65 7:25 6.65 7:45 7.25 6.65 5/12/00 4:30 7.2 0.9	Date time Total Solid Liquid (ml) (ml) (ml) 5/11/00 69:15 7.25 7.25 9:45 7.25 7.25 10:15 7.25 7.25 10:15 7.25 6.86 11:45 7.25 6.65 1:45 7.25 6.65 7:45 7.25 6.65 3:45 7.25 5/12/00 4:30 7.2 -0.9

PR B 5/15/00

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C415A

C6B without glass formers at 50	°C
---------------------------------	----

=/./-		(1)		Liquid	
=/.//=		(ml)	(ml)	(ml)	
5/11/00	~9:15=9:	554.8	4,6		
7	9:15	4,8			
	10:15	4.8	4.5	 	
	17:45	4.8	44	 	
	10.45	4.8	4.3	 	
	70.1		113		
					total Solice
	115	4.8	4.1	114.60	time total solice 2:45 4.8 3.8 3:45 4.8 3.7
- A-1	1:15	61.4	40		1 2 3.8
	1.9	-//-	1,0		7 2.15
•					7 3:45 718 3.1
5/12/00	4.30	48	3 6		
	1.0	7.	2.5		-
5/15/0	6.	35	3.5		
		5/12/02 4:30	10:15 4.8 10:15 4.8 10:15 4.8 1:15 4.8 1:45 4.8 1:45 4.8 5/12/02 4:32 4.8	19:15 4.8 4.5 10:15 4.8 4.4 10:15 4.8 4.4 10:15 4.8 4.1 1:15 4.8 4.1 1:15 4.8 4.1 1:15 4.8 4.0	10.15 4.8 4.5 10.15 4.8 4.4 10.45 4.8 4.1 10.45 4.8 4.1 1.15 4.8 4.1 1.15 4.8 4.1 1.15 4.8 4.0

C6-C without glass formers at 50°C 4.7 KB5/15/15

Target	Date	time		Calid	
rarget	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
30 min	5/11/00	~9:15.93	7.8	7.8	
60 min	, ,	9:45	7.8	7.8	
90 min		10:15	7.8	7,75	-
120 min		10:45	7.8	775	
150 min		11:15	7.8	7.60	
180 min		/-/		-	
210 hour					
240 hour					
270 Hour		1:15	7.8	7.5	
300 hour		1:15	7.8	7.5	
24 hour				, ,	
28 hour					
32 hour	5/12/00	4:30	7.7	7.3	
48 hour				1.2	
52 hour					
56 hour	5/15/00	710	7.4	74	

time total 5.11d 2145 7.8 7.45 3:45 7.8 7.45

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C 4 15 B C6B without glass formers at 50°C

Target	Date	time	Total	Solid	Liquid
	,		(ml)	(ml)	(ml)
30 min	5/11/0	29:15-9:3	4.75	4.65	
60 min	7-7	9:45	4.75	4.60	
90 min		10:15	4.75	4,60	
120 min		10:45	4.75	4.50	
150 min		11:15	4.75	4.40	
180 min				, ,	
210 hour				*******	
240 harr					
270 høur		1:15	4,75	4,2	
300 Your		1:15	4.75	4,2	
24 hour					
28 hour			1		
32 hour	5/12/00	4:30	4.7	3.7	
48 hour					
52 hour	- 21				
56 hour	5/1500	9A~	4.6	3.8	

Time total Sol. d -> 2:45 4:75 4:1 3:45 4:75 369

C425B C6C without glass formers at 50°C

Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
30 min	5/1400	19:15-9:30	ما .ما	6.6	
60 min	177	9:45	11.6	6.6	
90 min		10:15	6,6	6.55	13 = 1
120 min		10.45	6.6	62.55	
150 min		14:45	0.0	6.50	
180 min				1	
210 hour					
240 hour		Algeren se			
270 hour		1:15	(0,6	6.50	
300 hour		1145	6.6	6.50	
24 hour				,	
28 hour					
32 hour	5/2/00	4:35	66	6.6	
48 hour		- 1	-		
52 hour					
56 hour	5/5/00	9	6.5	15	

72:45 6.6 6.45 3:45 6.6 6.45

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89) If not performed in the last 30 days, analyze one standard between 10 and 100 cP for shear stress as a function of shear rate at 25°C from 0 to 1000 s⁻¹. Print out a copy of the rheogram and attach to this test plan.

90) Remove the graduated cylinders from the oven and allow to cool overnight.

91) While stirring the samples on a magnetic stir plate remove subsamples from each of the graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s⁻¹ over 2 minutes and then returning from 300 to 0s⁻¹ over 2 minutes Print out a copy of the rheograms and attach to this test plan

Frint out a copy	of the rheograms and attac	ch to this test plan.	1 20.5	
C6 A	File name 650	Date analyzed 5/12/00	05/200 H	
C6 A Duplicate	File name _05/200B	Date analyzed	051200 I actually	
C6 B	File name 05/200C	Date analyzed	05/2005 A2-107 Siaples	
C6 B Duplicate	File name 61200 D	Date analyzed	05/200K 28	
C6 C	File name <u>65/2∞</u> €	Date analyzed	Insufficent 5/31/6	٥
C6 C Duplicate	File name 05/200 F	Date analyzed		

92) Return this material to the respective graduated cylinders.

material in Rhometer + comes returned to respective jers and supermetent decented to return samples to target weight.

See attachment

IRP

5/31/00

Page _____ of__

Prepared By: Paul Bredt

Date: 5/22/00

Subject:

Mass	.f Reco	world samples	Fillowiz Rh	الم الم
Sample	Tom Things with jor	++1 ~55	water + add	
C109 Sutis	2 36. 5815	203.11	33.47	236.61
156t%	202.3	182.00	20.30	202.54
2562%-1	202.2	197.28	4.92	202.20
AZ-102 5.62		166.26	48.15	214.46
	711.75	209.43	2.32	211-73
25utis-1	269.59	28641	-16.82	282.774
with Stran	et Arm		attachment + 29953-0	

Balance check 1000g = 1000.00g

PR Bredt 12/6/99 - 15 m. Callos Derivers

Battelle Test Plan: BNFL-TP-29953-073 Page 43 of 60

93) Add the BNFL prescribed quantity of intermediate waste products to each of the three graduated cylinders and stir for 1 hour. Use the space below to record the quantity of intermediate waste products added and the time and date stirring started and stopped.

C6 A Stir Start (time/date) 2:45 Stir Stop (time/date) 2:45

Source Chemical	Target wt%	Amount (g)	Actual Added (g)
Softer precipitate		1.614	5.484
STATU PROLIPITATE		0,6 ml	0.7370
			CANA TO THE PARTY OF THE PARTY

235.757; ofter signal SH/free 241.234; 241.234; 241.971 g after story 240.811 s 242.805 g Final

C6 B Stir Start (time/date) 3.55 Stir Stop (time/date) 3.30

Source Chemical	Target wt%	Amount (g)	Actual Added (g)
Sc/TEN precipitate		12,231 9	12.0620
Sc/Tes precipitate CS Fluint		lilml	12.0629
	-		

213.8329 213.8329 CS Elunt 215,2685 Afric Strict 215,2685 Afric Strict 215,2685 Afric Strict 216,5329 Final

In Short -Tight vi-S 21k, 038

Source Chemical	Target wt%	Amount (g)	Actual Added (g)	201.065
Sr/tru Cs Eluint			20.160	after adding solv
Cs Eluint	- Landa	1.9 mL	2.4519	221. 225
			5 24.2	98tor CS ELLIN
				223.676
				222,045 222,045
•			3 44	224. 758

	C6 A	C6 B		C6 C	
Total Tare	g	Total	g	Total	g
Slurry		Slurry	g g	Tare	g g
Volume	ml \	Volume	ml	Volume	ml

95) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

C6 A	Time	Date
C6 B	Time	Date
C6 C	Time	Date
		Test run in 15 ml cent for comes cent for affected sheet
		PRB

ENGINEERING WORKSHEET Date: 5/23/00 Project: BNFL HLW Melter Feed Bredt 1TRU Simulant ITRU was prepared by Rich Hallen waln TI-082 He Number I was used for this work removed 2 subsamples for drying test on 5/23/00

ing Balance 384-06-01-018 axf. 8/00

36-2-06-01-041 exp 2/01

Bottle 1

15-9443

16-5963 13.2983 14.0050 1RB5/24/20 3.6085 laced in oven at 1050c indicated on merery thermometer at 850 am in 5/23/00 mass @ 2:40pm on 5/23/00 14.00 64 2 14.2590 Mass @ 9:30 an on 5/24/00 1 14.0050 - 13.2983 = 0.7067 7 14.2559-13.2878 = 0.9681 $\frac{0.7067}{2.646} = 0.267 \text{ g s.l.ds} \qquad \frac{0.96815}{3.6085} = 0.268 \text{ g s.l.ds}$ x = 0.268 & 5, 11d 5/ g 51.dy 75 uta-: 5 4tc 15 Lt% 25 we% -1 slis and-l 1.648 5.456 5.472 20.358 solis audid 6.149 12.23/ helled by LKJagille U.S. GPO: 1997-592-715 Tint

5 uts Syringe 1 tare 11.1101 11.8059 what with 5,-16 6.138g 15046. Syring 2 tor. 11.6575 5-- Ple 9.8115 2 2.420 Stripe 3 tar- 11.6717g Sapl 2.4440 J +otal 12.256 25-1 at% 5x1:204 tare 11.6547 s. pl 10.3147 18.043) 5 rringe 5 tore 11.6828 5 - - pl 10.0012 & total 25-2 wt% Tom! 22.03537 5 71inge 6 tan 11.6086 5- ph 10.4267 T= 11.64

attachment to Test Plan 29953-073

•

Pacific Northwest Laboratories		ENGINEERING	WORKSHEET		Page	of
Prepared By: LK Jag	ods Date:	126/00 Project:	BNFL-		9953	-073
'Subject: (-/0.4)	\$ AZ -10)Z SeH		ic S		
w/soconder waste)	7 U/seco	alon waste s		ر،،		
				6055	1, pf	
	tares) Filled	3) Sample	10.700	6-9-0	0
AZ-5-A	4.506	12.832	8.326	12.822	12.8	16
AZ5-B	4,508	12.386	7,878	12.375	12.3	70
A Z-15-A	4,509	12.858	8, 349	N.+	12.8	40
A Z-15-B	4,512	12.744		Musel	12.72	6
AZ 5 Bother	Betser 225	,936 F	fter -	2 5 3451	Smple 16.	186.0
HZ 15BoHh	Before 244,	160 011+	-c <u>-c</u>	27.345	Lost. C	
	5.4				2031.	73 0 5
				6,052		
	Tare	Filled	Semple	100		6-9.00
C-5A	4,445	11.837	7.392	11.826		11.820
C-2B	4.820	12.523	7,703	12.517		12.509
C-15A	4,470	11.75%	7.286	-7.286 , 11.746	AB 5/30/03	11.739
C-15B	4,784	12,128	7.344	12.062-	2dj - andelf20	12.066
C-25A	4.389	11.902	7.513	Not me		11.855
C-25B	4,792	11,580	6.788	ast m	esend	11.556
Circus Bottle S	Start 242,	697g Af	4,227:	573 g Sa	mpli 15. St 0.08	0955
C-104-15 Bottle	Start 216.	365g Af	ter 201e	429 Sa	mpk 1	4.63 5
C-104-25 Bottle	Start 234	. 707 S Af	ter_209,1	183 Sam	iple 14.	30/ 9
100		1				

) / 24 W & U.S. GPO: 1997 - 592-715

54-1007-114 (1/83)

Prepared By: Paul Brust Date: Project:

Subject:

Subject: Study C-104 w/secondary waste + A2-102 w/6/ss forms

- Reference to Step 94 of test plan
- Glass formers / secondary wastes were added 5/26/00, so Souples
have sothed in comes for n 4 days.
- A2-102 15 wt/2 samples have shown very 1: the sattly, and
C-104 25 wt/2 samples have shown none

Meas	und vo	lumes @ 9:15 a	- 07 5/26/0	0	e 214
		Total (me)	solids (wl)	mass (3) A.	100 Lais 621)
C104	5 A 5 B	7. Z 7. 5	4,6 1.7 1.8	7.39 Z 7.703	1.63
	15A 15B	6.4 stir. 6.8	5.3 5.64 643655	7.286 7.344	1.14
	15 A 15 B	6.9	6.9 6.7	7.5/3 6.788	1.09
A2402	5A 5B	7.77.65 7.2	4.64.45	8.326 7.878	1.09
	15A 15B	6.6	6.35	8.349 8. 232	1.26 1.23

- · No meniscus on \$2-102, but -0.2 ml of miscus on C-104 supls
 - . C-104 redon Botton of maniscus
 - .Gas bubbles seen in C-104 15B, No bubbles in A
 - · C-104 rishts are sygesty of tropped gas

Project: Attachment to TP 29953- 073

settling study C-104 w/ securlary weste + 42-102 w/class formers

· Samples C-104 = A+B did at settle over 4dys, so no indirectly in this study

· Samples A 2-102 15 A+B did not settle, so not included in this study

C-104

[Anbient study] steps 96 2 step 45

C-104 Shakan @ 10:250

'te	Time	5A		45B		15 A		150	
_		To+4	501.75	total	501.13	Total	50lid5	+41	Solids
130	10:35 10:45 11:00 11:10	7.5 7.85 7.5 7.5	7.3 43 7.1 ching 4.3 3.4	7.7	7.24	6.5	7.16.6 6.3 6.2	6.7 6.7 6.7	6.7 6.3 6.2
	11: 20 11: 30 12 12: 30 1 1: 30 2 2: 30	7.5 2 7.2 7.7 7.7 7.7 7.7 7.7 7.7 7.7 7.7 7	2.7 1 2.2 2.0 1.9 1.21.9 1.75 1.75	7.7 7.5 7.5 7.5 7.6 7.6	2.91 2.4 2.2 2.0 2.0 1.9 1.9	66666555	6.1 6.0 5.8 5.7 5.6 5.6	6.5 6.5 6.5 6.5	6.2 6.1 6.0 5.7 5.7
	3 3:30 4	7. 2 7. 2 7. 2	1.75	7.6	1.8	6.5	5.55 5.5 5.5	6.5	5.6 5.6 5.4
31/00	7:30 m 2100p	7.3 7.3	1.6	7.5	1:7	6.5	5.2 5.1	6.5	5.3 5.2
//	B:00a_	7.3	1.5	7.5	1.55	6.5	5.1	6.5	5,2
12	4:00am	7.3	1.45	7.5	1.5	6.5	5.0	6.5	5./

used plastic antifux coms

Prepared By: Pal Bre Date: 5/30/00 Project: Aftachant + TP 29953-073

Subject: Settling: 5tudy

8/10/03

AZ-102 - Andient (De glass firmins)
sh-kane 10:32 an

Date	Time	AZ-10251	a 1	5B	2 12:33 12:3 24
	1120	10-13 C 3 /	5.1.25	10 to to 1	501:45
5/30/00 5/30/00	10.3/0 /6:35 /0:45 //:00 //:00 //:00 //:00 //:30 //:30 //:30 2 7:30 3 3:30 4	7.7.6.66555555555	7.7.7.6.6.6.5.30 9.85.55	7.3 7.7 7.7 7.7 7.7 7.7 7.7 7.7 7.7 7.7	7.753085520876544
5 31 00	7:30 km 2:00 pm	7.5 7.5	4.2	7.1	4.2
6/1100	G:00an	7.5	3.8	7.1	3.9
6/2/00	8	7.5	3.7	7./	3.8

used plater contry

3.5cm - 0.583 m 3.5cm from 4+10al 6/2/00

AZ-102 with Glass formers and C-104 with Secondary Waste Products AZ-102	• •	50°C Settling Study	ling Stuc	dy	-						Attachi	nent to Te	Attachment to Test Plan 29953-073	53-073	
Solids Total Total Solids Total To	1/00	AZ-102 w	rith Glass	s formers	s and C-1	104 with S	Seconda	ry Waste	Product	s					
Total Solids Total Total Solids Total	一大			AZ	-102					ن	104				
Total Solids Total A.V. A.	(V) 19-1		5	A	5	B	5	V	5	В	15	5A	15	3B .	,
7,6 7,8 7,9 7,9 7,9 7,0 7,6 7,0 6,5 54.16 (2.6. 7,6.8) 7,6 7,3 7,3 6,9 7,5 7,0 7,6 7,0 6,5 54.16 (2.6. 7,) (1 1	Total	Solids	Total	Solids	Total	Solids	Total	Solids	Total	Solids	Total	Solids	
7.6 7.3 7.3 6.9 7.5 7.0 7.6 7.0 6.5 54.16 6.6 7.6 6.8 7.6 6.5 54.16 6.6 7.6 6.8 7.6 6.5 54.16 6.6 7.6 6.8 7.6 6.5 54.16 6.6 7.6 6.8 7.6 7.6 6.5 7.6 7.6 7.6 7.6 7.6 7.6 7.6 7.6 7.6 7.6		- 1	م./ب	7.0	2.50	7.6	4,6~		ったっ		れんいろ	ì	819~		
10:50 71.6 6.18 71.3 6.15 6.24 6.15 6.14 6.15 6.15 6.15 6.15 6.15 6.15 6.15 6.15		10:25	2,6	7,3	7,3		7,5	01/	م'ر	20	26,5	54.216		-jarys	
2:35, 7.6 4.57 7.6 7.6 7.7 1.6 7.7 1.8 6.8 5.5 6.5 5. 3.35, 7.5 7.8 7.8 7.2 7.6 7.8 7.8 6.5 5. 6.5 5. 3.35, 7.6 7.6 7.6 7.6 7.8 6.5 5. 6.5 5. 3.35, 7.6 7.6 7.6 7.6 7.6 7.7 1.8 6.8 5.7 6.5 5. 3.35, 7.6 7.6 7.6 7.6 7.7 1.9 1.9 6.8 5.7 6.5 5. 3.35, 7.6 7.6 7.7 7.6 7.7 7.6 7.7 7.7 7.7 7.8 6.8 5.7 6.5 5. 3.35, 7.6 7.8 7.7 7.9 7.7 7.7		05/01		6.8		5'9	12.07	817		(0,4	5,0	4.4			
1.30, 7.6 5.85 ~ 7.5 7.3 7.2 7.6 2.35 ~ 6.5 6.5 6.5 5.1 1.30, 7.6 7.6 7.7 7.6 6.5 5.2 5.2 7.45 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.6 7.7 7.7		S.		29.50	- Daller	2,5	6. Am	12.5	が託さ	2.5		7.7			
2.136, 76 5.0 7.6 4.7 7.6 3.0 7.8 1.90 6.8 5.85 6.5 5. 2.135, 7.6 4.65 7.6 4.6 7.8 1.9 1.9 6.8 5.7 6.5 5. 2.35, 7.6 4.65 7.6 4.50 7.7 1.9 6.8 5.7 6.5 5. 3.35, 7.6 4.65 7.9 4.90 7.5 1.75 7.1 1.9 6.8 5.7 6.5 5.9 3.30 7.65 4.5 7.3 4.9 7.9 1.7 7.6 1.7 6.8 5.3 6.9 5.9 3.30 7.65 4.5 7.3 4.9 7.9 1.7 7.6 1.7 6.8 5.3 6.9 5.1	الم	16:40	17.6	5.85	27.5	5.5	7.5	2,2	7,6		12:31	6,2	~6.5	6,2	
3:35, 7.6 4.7 7.6 4.6 7.6 1.9 7.7 1.8 6.4 5.8 6.5 5.3 3:35, 7.6 4.65 7.6 4.50 7.6 1.85 7.7 1.4 6.8 5.7 6.5 5.8 3:35, 7.6 4.65 7.0 4.40 7.5 1.75 7.7 1.7 6.8 5.35 6.5 5.9 3:32, 7.65 4.5 7.3 4.4 7.4 1.75 7.7 1.7 6.8 5.30 5.9 8:30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.30 5.1 8:30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1	4.70	1.40	17	5,0	7.6	4.7	2,6	20	214	1.90	6.8	5.85	6.5	5.9	
3:35, 76 4,65 76 4,50 76 1.85 7.7 1.4 6.8 5.7 6.5 5.9 8.30. 765 4,59 7.7 4.40 7.5 1.75 7.7 1.7 6.8 5.35 6.5 5.9 8.30. 765 4,57 7.7 4.40 7.5 1.75 7.7 1.7 6.8 5.35 6.5 5.1 8.30. 765 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1 8.30. 765 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1		2. 15m	5	4.7	17.6	4.6	3/2	1.9	67	811	50	S S	10.51	15'5	
8.38cm 7.65 41.60 71.7 4.40 71.5 7.7 1.7 6.8 51.35 11.5 51.9 8.38cm 7.65 41.55 7.7 4.40 7.5 1.75 7.7 1.7 6.8 51.35 6.5 51.9 8.38cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 51.9 8.38cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 51.9 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 51.9 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.6 1.7 6.8 51.30 8.39cm 7.65 41.5 7.3 44.9 7.9 1.75 7.7 1.7 1.7 1.7 1.7 1.7 1.7 1.7 1.7 1.7		-	9"L"	4.65	2,0	05/4	3.0	1.85	12	1,9	6.8	2:5	(0, 5	Sis	
3.32 765 4.54 7.7 4.40 7.5 1.75 7.7 1.7 6.8 5.35 6.5 5.1 8.30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1 8.30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1	4/00	_	597	4,60		4,40	7,5	1.75	<i>ل. ب</i>	1.7	6.8	5:35	6.5	5,45	41
3.32 765 45 7.3 44 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1 8:30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4 5.1	_	থ	1	4.50	7.7	4.40	7.5	1.75	7,7	1,7	10.8	5.35	6.5	5.15	
9:30 7.65 4.5 7.3 4.4 7.4 1.75 7.6 1.7 6.8 5.3 6.4		3.30		45		4.40		1.75		1.7	9	5,30		5,13	
	00/6	8:30		4.5	7.3		7.4	1.75		1.7		5.3	7.9	1.5	
								Y I							
															T.
											3				
	•.													Š	
						i.									

Density of AZ-102 with Class formers C-1024 with 2nd waste products

cones were proposed on 5/26/00 and settling studies were conducted at ambient +50°C. Howevery gas bubbles in sludge made density measurements un relieble.

Samples will be contributed @ ~ 1000 xg for 5min to remove bubbles and then the volume will be mensured @ ambient 33°C (on read out 2215 exp 10/11/00)

and @ 50°C (in an over at 50° on readout 2013 eyp 8/01)
for I hour

P1653	(5)	Total Volum (ml)	after the
AZ-102 5 A	12.816	7.7 p=	7.8
5 B	12.370	7.2	7.3
15A	12.840	6.8	6.8
15B	12.726	6.75	6.8
C-104 \$5A	11.820	7.3 p=1.62	7.3
5 B	12.509	7.6 p=1.653/4	7.6
15A	11.739	6.5 f= 1.81 3/21	6.5
15B.	17.066	6.6 P= 193 3/d	6.6
25A	11.855	6.2 7=1.91312	6.2
25B	11.556	5.65.8 P= 1.99 J= 1 PAB 6/9/00	5.8
		ignore	

Part Bru-6/9/00

Manual Brand

6/9/00

Deasity of settled samples at ombient

A2-102 5A 17.816-4.506 = 1.08 31-8

@ 500 8.31/7.8= 1.069/2

5B

(12.370 - 4.508) / 7.2 = 1.09 grad

15 A

(12.840-4.509)/6.8= 1.23g/ml

15 B

(12.726-4.512)/6.75 = 1.22 g/al

Some as andert

7.862/7.3= 108g/al

C-104

5 A 1.01ghd (11.820 - 4.445)/7.3 =

5B

(12.509-4.820) 17.6 = 1.01 g/ml

(11.739-4.470)/6.5 = 1.12,/ml

15 B (12.066 - 4.784) 16.6 - 1.10 g/al

25 A (11.855-4.389)/6.2 = 1.20 g/~

(11.556-4.792)15.8 = 1.17,12

4:

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96) After turning off the stirrer, record the ambient temperature, volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)		
5 min	\						
15 min							
25 min							
35 min							
45 min	1		,				
55 min							
1 hour							
1.5 hour			-				
2 hour							
2.5 hour		ļ ,					
3 hour							
3.5 hour							
4 hour							
4.5 hour							
hour							
5.5 hour							
6 hour							
6.5 hour							
7 hour				1			
24 hour							
28 hour							
32 hour						ser atte	,
48 hour						ď.	L,
52 hour					1	~ H2	
56 hour						sec 1	PO

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Target	Date	time	Total		Liquid
5 min			(ml)	(ml)	(ml)
					Late 1911
15 min					
25 min					
35 min					
45 min					
55 min	-/			Mark Control	
l hour					
1.5 hour	1				
2 hour					
2.5 hour					
3 hour					
3.5 hour	•				
4 hour					
4.5 hour					
5 hour			1		
5.5 hour					
6 hour					
6.5 hour				1.	
7 hour			1		
24 hour				1	
28 hour				1	
32 hour				1	
48 hour				1	
52 hour					
56 hour				1	

140/31/0°

Target	Date	·time	Total (ml)	Solid (ml)	Liquid (ml)
5 min					1, ,
15 min					
25 min					
35 min					
45 min				1	
55 min					
1 hour					
1.5 hour					1
2 hour				/	
2.5 hour					
3 hour			/		
3.5 hour					
4 hour			/		
4.5 hour					
5 hour			1-1-1-1-1-1		
5.5 hour					
6 hour		1			
6.5 hour					
7 hour					
24 hour					
28 hour					
32 hour					1.00
48 hour					
82 hour					
56 hour					

97) Rlace the graduated cylinders in an oven at 50°C (±5°C) for 1 day. Remove the samples and record the mass and volume.

	C6 A	C6 B		C6 C	
Total _	g	Total	g	Total	g
Tare	g	Tare	g	Tare	g
Slurry _		Slurry	g	Slurry	g
Volume	ml	Volume	ml	Volume	ml

98) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

C6 A	Time	Date
C6 B	Time	_ Date
C6 C	Time	Date

See attachant 8/10/02

99) Return the graduated cylinders to the oven at 50°C.

100) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

C6 A with intermediate waste products at 50°C.

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min					<u> </u>
60 min					
90 min					
120 min					-
150 min					
180 min	1				
210 hour					-
240 hour					
270 hour					1
300 hour		1			
24 hour			X		
28 hour					
32 hour	-				
48 hour					
52 hour			1	1	
56 hour					

C6 B with intermediate waste products at 50°C

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min					
60 min		100			
90 min					
120 min				7	1
150 min			1		1
180 min					<u> </u>
210 hour					
240 hour					
270 hour					
300 hour			7		
24 hour			-	- 3	
28 hour					
32 hour		0.11		al cureau con	1 a 10 K
48 hour		una et	1 10 1 10	and the same of	6 (),0
52 hour					
56 hour					

See aft a Hackment 8/10/00

Battelle Test Plan: BNFL-TP-29953-073 Page 49 of 60

Target	Date	time	Total	Solid	Liquid	See attacher 8/10/02
			(ml)	(ml)	(ml)	8/10/0=
30 min			1	1,		
60 min		- 100 (1)				
90 min						
120 min						
150 min				4		
180 min						
210 hour		/				
240 hour						
270 hour		/				
300 hour						
24 hour						
28 hour		* 7		1		
32 hour		1,		1	1	
48 hour					 	
52 hour						
56 hour						

rheogram and attach to this test plan.

Viscometer M 5	Location A cell 500	Geometry	MUI
Viscosity 95.5 cP	Lot_////99	Manufacturer	Brook Field
File name	Date analyzed 6/1/0	0	

Remove the graduated cylinders from the oven and allow to cool overnight. 102)

While stirring the samples on a magnetic stir plate remove subsamples from each of the 103) graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s⁻¹ in 2 minutes and then returning from 300 to 0s⁻¹ in 2 minutes. Print out a copy of the rheograms and attach to this test plan

mates. Trint ou	25°C	s and attach to this	25°C \ 50°C \
C6 A	File name	_ Date analyzed	5 46 060100D 5 48/ 060200 F
C6 A Duplicate	File name	Date analyzed	15 wt 6 060100 F H
C6 B	File name	Date analyzed	254+ 6060100 H (J
C6 B Duplicate	File name	Date analyzed	T 75626 060200 K
Céc	File name	Date analyzed	K / K
)

PR Bredt 12/6/99				telle Test Plan: Bl		
C6 C Duplie	File nar	me D	ate analyzed	6/10/00 /a	>	
104) Retu	rn this material to t					
105) Add stir for 1	the BNFL prescrib hour. Use the space	ed quantity of glasses below to record	s formers to each	of the three gradua ss formers added a	ited cylinders and	d
date stirr	ing started and stop	oped.			V	
C6A Stir S	Start (time/date)_ 9 :	Stir Stop (time/date) /o:	50 6/19/	V:41 6	doled
073667	•	Glass Formers:		- 4	7.9530	PRB.
Source Chemical	Manufacturer	Lot#	Target wt%	Amount (g)	Actual Added	1-1-60
•						
			+ + +			
			ex bu	0 B 1 11	100	-
			/	1201		
			+			
						-
			A STATE			
		.		1		-
weight	out Gls	s formers		lure lynet		
	suto	15	vt2 / 2	5-1/251 1	25-21	2
Toil	24.4464	24.31	32 24	1254 24.1354 24.	1967 2	4.5155
	14.0981	28.0	235 27.	5406/19.1443 27	.5024 19	1.2739
Total	38.5445	51.33	67 51.96	60 43.27 51.	6991 4.	3.7894
		•	ı		1	
0-1	la <i>al</i>	7.1-1	1.		-1. C.	
brior a	air beek	dition, som	735.5.0	Il edd remaining	15 x + 4.	<i>-</i>
,	to show and air back 5 with	1 15 4	t'5 1 3	25-16to	in the later to p	veret or
	42.805	216.5	and the second	24.758		
lmss 2	34.930	217.57	701.40	11		
- 1 mas > 2			Clisto	11,520	•	

	Glass fe	rmulatio	ons in th	nis rep	ort f	or A	W-1	01 a	and AN-107 are considered to be
	Glass I	5		propr	ietar	y b	y VS	L/D	Duratek V
	`\ .	7/3					4	×	\ \frac{1}{2}
`~	-5_	5.65)		1	\	11	1	W / W
	1001, 2 1864	68.2 25 wt%-2	5.472	1.9	12.361	0.751	1.051	0.000 46.788	Jago de
	68.1	68 25 wt%-1 25	5.456	9.1	12.325 \	0.749	1.048	0.000	1 K J
	,25673	s 68.1 15 wt% 25 v	3.278	77-	7.406.7	. ,	1	0.000	7 1/1
ع	102.69 = ,25673	Actual mass 102.69 5 wt% 15 v	1.648 /	5.7 0.6	3.7237	0.226	7.463	0.000	
Additive		5 wt%	32.092		72.500	4.406	6.162	00000	
Ä	51	Based on 400 g of slurry 5 wt% 15 wt% 29	19.256	6.6	43.500 27.600	2.644	3.698	0.000	
1255	molati	Based on 40 5 wt% 1	6.418	2.2	14.500	0.881	1.232	0.000	
5		20 wt% (25.674	8.8	58.000 36.800	3.525	116.280 4.930	0.000	
C-104 (Additive Sr/TRU Precipitate	(dry solids basis) Cs Eluant	7 solution)	/ Na2B4O7@10H2O LiOH@H2O	Na2CO3	ZnO (KADOX-920)	Sugar (Granular) Total Glass Formers	

C104glass.xls 5/24/00 PR Bredt

G a S S A A A C L C A S C A S C C A S C C C A S C C C C C C C C C	20 wt% 5 w 25.674 25.674 25.674 116.280 3.525 116.280 0.000		Additive Sr/TRU Precipitate (dry solids basis) Cs Eluant (27 g total solids/ml solution) in ml Na2B40710H20 LIOHH20 Na2CO3 SiO2 (Sil-co-Sil 75) Zn0 (KADOX-920) Sugar (Granular) Total Glass Formers Na2B40710H20 LIOHH20 Na2CO3 SiO2 (Sil-co-Sil 75) Zn0 (KADOX-920) Sugar (Granular) Total Glass Formers
---	--	--	---

Batch D/

C104glass.xls 5/24/00 PR Bredt

PR Bredt
12/6/99

C6 B Stir Start (time/date) /0:55 Stir Stop (time/date) /1:55

Glass Formers:

Source Chemical

Manufacturer Lot#

Target wt%

Amount (g)

Actual Added (g)

 				
 \				
		1 . 8	~ y	
		- Sec	60	
P - D -		200	50 PRB 6119/00	
	 	\	11.0	
 		\	6/19/00	
		+		
				7
		 	+	

C6 C

Stir Start (time/date) /:0 0

Stir Stop (time/date) 1:50

Glass Formers:

Source Chemical	Manufacturer	Lot#	Target wt%	Amount (g)	Actual Added (g)
			per 5	-0	
		Ser	6 BB		
			6/19	100	

To 25-1 before mixing 6/19/00 PRB

106) Cap the graduated cylinders and record the mass and volume.

			C6 A	C	6 B	Land W.	C6 C	
7	Total Tare Slurry Volume		g g g ml	Total Tare Slurry Volume	g g m	Total Tare Slurry ! Volume	g g g ml	
	107) min	utes, tur	n oii the sti	rial in each of t	he graduated cy rd the time and	linders using a date for each o	magnetic stir plate. A	after ~2
		C6 A	Time		Date		See attach	ment 100 /RB
	****	C6 S	Time		Date			
/	\	5 6		ided in		t- 10 d	plastic contrib	fage cones
		C 5	5. •	c 5 C	S	c	15 A	
		15.4		13.19	152		4.816 2	
	re.			4.50		_4	.445	
	7	<i>C</i> 1.	0	8.64			2.371	21
To	te 1	-		16.3	5A 89		(.027 s	8 8
+	12	4.5	14	4.44	5 5		1.465	455
SI	dz	1132	1	11.94	7 1		1.562 5	
205	F. Chur	4/4	4/		t chak	14.27	8/3 wt check	18/30
-51	1 - 13 3 - 1	3,14	8 V		A-13.43 B-13.11	303	-54 - 13.410.	1
015	A - 1 B - 1	4181	7 /		5 A - 14.7 5 B - 1 5 .5	01	5B - 13.0919 15A - 14.7619	142/
7/1	11/00 -	cent	of ale	11 6 6-1	5000	77	15B - 15.544g 15A - 16.242 258 - 15.88)	1 100
	c 5	This	13 10 Aug	volumes	(251	\$ c	30 m ((() ())	3 1 4 8 8
	< 5	B 8.	1	11.07	C 25 B	<u>8.3</u>	1.41 -\ 1.41	
• • 6		5 A 8.		mx 1.30				8/3/0

A lent Settling Study

C-104 with Secondary Waste Products and Glass Formers

							כ	-101-O					
		2.2	5A	7.85	5B	8 , 1 15A	5A	9,0 15B	5B	2	25A	2	25B ·
Date	Time	Total	Solids	Total	Solids	Total	Solids	Total	Solids	Tatal	Solids	Total	Solids
6/21/00	6/21/00 9/25cm	8.2	216	1,8	6,5	8:1	1.8	12	1.1	_			
1.2/0	281P	5.5	6,1	7.8	5.3	1,8	178	7"5	911	_			
12/01	54.6	7.7	6.4	1.70	4.0	8,1	1'8	911	1,1				
12/9	25.0		25		5.3	181	8.11	1.6	611				
12/21	10.00 S		3.5		3.0				`				
12/01	10115		3.4		2.9						_		
15/21	US: 30		3.3		۶.						_		
1.80 6/21	10,50		3.0		4.7						_		
12/01	08/II		61%		5,56	-1%	3,0	116	9,0				
12/21	1.5		3.8	ŀ	53	_	الما "و	4,1	9,0				
44	13:3C		5.8		A.50		-						
2.5 6/21	55.55		7,7		7:4								
	13,30		7.7		25							_	
	9575.		3.6		3.3							_	
	14:20		3.6		3.3							_	
	14:50		573		٣,٢		-						
	15:30		3.5		3.3				1				
	15:30		ج أح:		7,3		`		⋗				
	Q: 131		2.5		4.3		7.8		8.9				
	05:91		2.5		7.3				je Ve				_
21/15	4.00		5		3.3		スン		رخ ئ				
			7,4		7 7	4	7.0		٧.				

Settle Sattle 125 8/10/03

Ambient Settling Study

C-104 with Secondary Waste Products and Glass Formers

							ל	C-104				
			5A	5	5B	15	15A	1	15B	\25A		25B ·
	Time	Total	Solids	Total	Solids	Total	Solids	Total	Solids	Total Solid	Total	Solids
			3,3		7.1		6.9		7.6	/		
						1.0		ı				
12/20	11.40cm 8.	58,5	12	87	1,9	2,0	9	2-8.8	7.2			
+											_	
1												
	Ŀ											
			+									
-												-
7												+
												+
												1
-												
_												

coold not so the ms

50-C Settling Study

C-104 with Secondary Waste Products and Glass Formers

_	T	1	Т	T	Т	T	T		_	T	_	_	1	Т	Т	_		-1	1	_		 	1
	25B .	Solide	Spilos																				
	2	Total															_	_	-	-			
	A	Solids							_	-	-	-			la.r								
	1 25A	Total																					
	8	lids	1	8.65	2	10 10		8.45	8.70	35.37	× ×	200	8.25	F. 25-	8,20	2.20	8.00	7.95					
04	90 151	Total So	2. 8.						3 0-		1	K	0 00	30	30	1	0-	1					
C-104		spi		8,0	-	7.7		7,7	7.7	0	7.5-	7.5	7,5	7.50	7.45	. Y.Y.	7.25	7.30					
	8.1 15A	Total	S. C.	S.													7	7					
		Solids	かの	3,/	87,8	がい		4.7	3,6	2.55	2.55	2,55	2,55	2.55	2,55	2.57	3.50	2.45					
	次 0 5B		1:00	118					7	••	. 0	10	1,2	.0	16	11		3 .					
		Solids	40	3,3	3,1	2.9	Œ.	3.8	3.8	7,8	2,75	2,75	2,70	2.70	J.A.	2	3.70	02.					
	8.3 5A	Total 5	8.5	8,5	()			1.9	.0	Œ	1.8	16	1.8	(8	60	12	3	~					
	3	Time	:40	10:12	04:01	(1): (C)		13:10	12:40	0/:	04:	0/;	06'	0/:	3:40	4:10	8:0G	4:00		v			
	9:10	Date T	5	10:121	355	1 08/9	- rx/d	2	127	1 12/2	1/27 1	6/213.	6/27 2:40	6/113:	0/21 3	10/27 4.							
@	Single of		3000 0140	100	40 6/34	2) (2)	4st	10081	272	2 40	270	300	17/2	_		1485	3260	60201 6/28			•.		

5.4 8/10/25

Battelle Test Plan: BNFL-TP-29953-073

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After turning off the stirrer, record the ambient temperature, volume of settled solids layers and liquids after 5 minutes, then every 10 minutes for the first hour, and then every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day. Collect video during the first 3 days of settling.

Ambient °C

C6 A with class formers at ambient temperature

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
5 min				1 , ,	1
15 min					
25 min					
35 min		1			+
45 min			1		1
55 min			1		
1 hour					
1.5 hour					
2 hour				-	
2.5 hour					1
3 hour			1		+
3.5 hour			1		1777
4 hour				1	
4.5 hour					1
5 hour				1	
5.5 hour					-
6 hour					T TING
6.5 hour					THEFT
7 hour					1
24 hour					
28 hour					
32 hour					
48 hour					1
52 hour					+ +
56 hour					

See attachment

Battelle Test Plan: BNFL-TP-29953-073

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Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 min					
15 min					
25 min \				1	
35 min	\				
45 min					
55 min					
1 hour					
1.5 hour					
2 hour					
2.5 hour					
3 hour					
3.5 hour	•				
4 hour					
4.5 hour					
5 hour					
5.5 hour				1	
6 hour					
6.5 hour					
7 hour				1	
24 hour					
28 hour					
32 hour					
48 hour					
52 hour					
56 hour					

See attachment

56 hour

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Target	Date	time	Total	Solid	Liquid
			(ml)	(ml)	(ml)
5 mily					
15 min					
25 min					
35 min					
45 min					
55 min					
1 hour					
1.5 hour					
2 hour					
2.5 hour		1			
3 hour					
3.5 hour	•				
4 hour					
4.5 hour					
5 hour					
5.5 hour					
6 hour					
6.5 hour					
7 hour					
24 hour					
28 hour	***				1
32 hour			1		
48 hour					
52 hour					
				1	

109) Place the graduated cylinders in an oven at 50°C for 1 day. Remove the samples and record the mass and volume.

C6 A		C6 B	/	C6 C		
Total Tare Slurry Volume	g g n	Total Tare Slurry Volume	g g ml	Total Tare Slurry Volume	g g g ml	hme-t

1 10) Mobilize the material in each of the graduated cylinders using a magnetic stir plate. After ~2 minutes, turn off the stir plate and record the time and date for each of the three samples.

 C6 A
 Time
 Date

 C6 B
 Time
 Date

 C6 C
 Time
 Date

111) Return the graduated cylinders to the oven at 50°C.

112) After turning off the stirrer, record the volume of settled solids layers and liquids every half hour until the end of the work day. As well, record these volumes every 4 hours during the second and third day.

C6 A with glass formers at \$0°C

Target	Date	time		Total	Solid	Liquid
			/	(ml)	(ml)	(ml)
30 min				1		1 /
60 min						
90 min						
120 min						
150 min						
180 min				/		
210 hour						
240 hour						
270 hour					1	
300 hour						
24 hour						1
28 hour						
32 hour				-	1	
48 hour						1
52 hour					1	1
56 hour					1	+

See attachment

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&6 B with glass formers at 50°C

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 mm					+
60 min					
90 min					
120 min					1
150 min					
180 min	1				
210 hour					
240 hour					
270 hour					
300 hour	1				
24 hour	200				
28 hour					
32 hour					
48 hour					
52 hour		1			
56 hour					

Target	Date	time	Total (ml)	Solid (ml)	Liquid (ml)
30 min			1	()	()
60 min					1
90 min			 		
120 min			1		
150 min				1	
180 min				1	
210 hour					
240 hour				1	
270 hour				1	
300 hour					
24 hour				1	
28 hour					4
32 hour			1-2		\land
48 hour					+
52 hour					+
56 hour					\

see attachment

Battelle Test Plan: BNFL-TP-29953-073 Page 58 of 60

If not performed in the last 30 days, analyze one standard between 10 and 100 cP for shear stress as a function of shear rate at 25°C from 0 to approximately 1000 s-1. Print out a copy of the rheogram and attach to this test plan.

Viscometer_ A 5	Location ACEll	Geometry MVI
Viscosity 95.5 cP	Lot	Manufacturer Brookfield
File name 060100 A	Date analyzed 6/1,	100

- Remove the graduated cylinders from the oven and allow to cool overnight. 114)
- While stirring the samples on a magnetic stir plate remove subsamples from each of the graduated cylinders and analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C and 50°C from 0 to 300 s-1 in 2 minutes and then returning from 300 to 0s-1 in 2 minutes. Print out a copy of the rheograms and attach to this test plan.

	25%
C6 A	File name Oblives B Date analyzed
C6 A Duplicate	File name Obitos B Date analyzed 062300 C
C6 B	File name 06 2200 Date analyzed 15 Lt's 06 2300D
C6 B Duplicate	File name $\frac{0622000}{0627306}$ Date analyzed $\frac{0623000}{0623006}$ Date analyzed $\frac{0623000}{0622006}$ Date analyzed $\frac{0623000}{0622006}$ Date analyzed $\frac{0623000}{0622006}$ Date analyzed $\frac{1}{1}$ Good naterial to the respective graduated cylinders.
C6 C	File name 062200F Date analyzed 25 4 2% 0623006 45
C6 C Duplicate	File name 06 2700 11 Date analyzed
116) Return this m	naterial to the respective graduated cylinders.

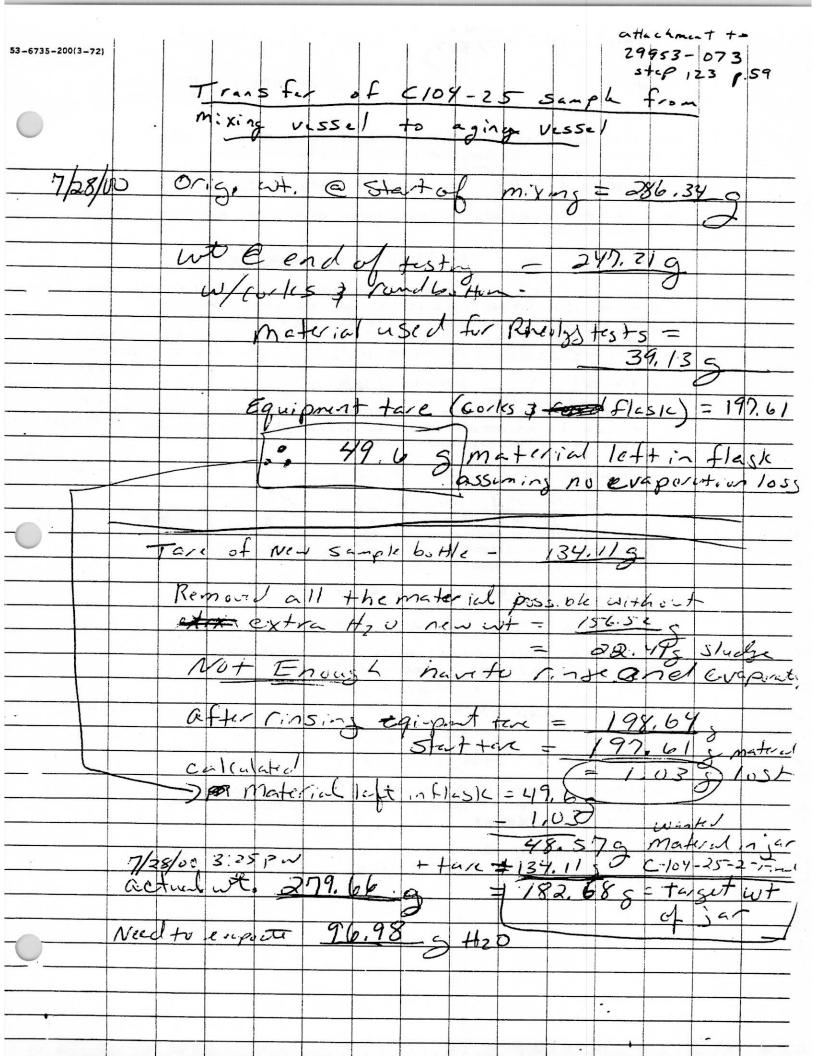
not enough material in H +I Assemble a mixing vessel using the following parts or equivalent. Attach impeller to a stirring 117) motor capable of maintaining a constant rotational rate from 100-1400 rpm.

Part	Vendor	Catalog number
500 ml O-ring Sealed Kettle, 3.75 inch OD, 5 3/8 inch flange	Labglass	LG-8071-100
Clamp	Labglass	LG-7316-106
O-ring	Labglass	LG-1022-476
Kettle top with three 24/40 necks		LG-8072-100
2 3/8 diameter 4 blade impeller	Fisher Scientific	14-505-20G

LG-1022-476	LG-8072-100			
2 3/8 diameter 4 blade impeller	Fisher Scientific	14-505-20G		
2 neck round	bottom 2 50 ml - torn	16 8.78 g		
Stopper	A - 14.44g	Can to hold round	Bottom	67.76
B - 14.3 9 g	Can to hold round	Bottom	67.76	
Total	197.61g			

Test Ylan 29953-073 Target for 51-rry mass in round Bottom = 68.2 g from P-2 B-ck of page 58 P-2- 34 Stop 72 mass of round Bottom 168.78g Mass of stoppers @ 14.44 & ©14.39 g target -> 265.812 (m-55 @ 8Am on 7/20/00 271.37g -> 5.58g too high smill . momt it > 266.689 > 0.97 to high Start 7 1.8.2 6 8:12 after 57/10 -> 284.549 net addian = 17.86g or. grid materal = 20,48 a 0.87 10st = 2,6283g H20 -= target Holoadd = 1.75. New taget = 286.293 after Hzvaddin = 286.34a 1:35 Start glass fund addition -Iwiss black Had to bump power / material is not mixing and goods formers are floation on top 1:43 - Second bottle of G.F. added - (viodes on)
Bunped powed to mix 1:52 stat Ihr Stirtime ~ 400 rpm.

Alf



A MIXIN SALI COAL	L		S. U
- massion 7/11/00 = 197	7207	The state of the s	3,5,4
	.30/9		
PR Bredt 12/6/99		Battelle Test Plan: BN	FL-TP-29953-073 Page 59 of 60
وخراب والسخوالا	t. + L.		
118) Transfer the sample specified Record which sample was transfer	red as well as the day a	nd time transferred below	
Sample transferred 7/18/00	Date	Time A ~	1000
119) Turn on the stirrer and adjust to date and speed below.	the rotational speed to the	hat specified by BNFL. R	decord the time,
Speed ~ 400/pm rpm	Date 7/20/00	Time 1152 p.	1
120) After 1 hour of stirring, remove shear stress as a function of shear Print out a copy of the rheograms 35 725 C. Run 1 File name 072000 B	rate in dunlicate Cond	uct the analysis at 25°C fi	rom 0 to 300 s ⁻¹
Run 1 File name 072000 B	Date analyzed 7/20	1/40 ~3: 25 p.	E: L 0720004
Run 2 File name 072000C 072000 121) After 1 day of stirring, remove shear stress as a function of shear Print out a copy of the rheograms	Date analyzed 7/20 7/20 re a sample through the rate in duplicate. Cond and attach to this test p	sampling port and immediate the analysis at 25°C flan.	Sample liftle over the
Run 1 File name 0721001	Date analyzed 7/2	1/00 ~ 3!20	
Run 2 File name 072100B	Date analyzed 7/2	2/50~3:30	
122) After 1 week of stirring, remo for shear stress as a function of sh 1. Print out a copy of the rheogra	ove a sample through the near rate in duplicate. C	e sampling port and imme conduct the analysis at 25°	ediately analyze
Run 1 File name 072700A	Date analyzed 7/27	1/00 A	
Run 2 File name 072700B	Date analyzed 7/a	7/00~	
	ole ID, volume and mass C -104-25-2 - F	s of material.	.119
Total 182.68 g Total Tare 134.11 g Solice	l ml	- Could no	t rend accoratly

ml

Focus a video camera on the solids-liquid interface of the sample and collect video for one

After the sample has remained undisturbed for 1 week, remove the standing liquid using a glass

No 6.5663 5.00 releasing or trapped of slacks

week taking care not to disturb the sample. Report any observed gas retention and/or release

Slurry

124)

behavior to the cognizant scientist.

Liquids

Tare C104-25-2 Wash 129.07

PR Bredt 12/6/99

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pipette:

126) Gently collect a subsample of the settled solids and immediately analyze for shear stress as a function of shear rate in duplicate. Conduct the analysis at 25°C from 0 to 300 s⁻¹. Print out a copy of the rheograms and attach to this test plan.

Run 1 File name 08/000A Date analyzed 8/10/00

Run 2 File name <u>081000 B</u> Date analyzed <u>8/10/00</u>

8/10/00

PNNL Test Plan Addendum 1

Document No.: BNFL-TP-29953-073 Add 1

Rev. No.: 0

Document Control: Only the original signed copy

is controlled

Work Location: Radiochemical Processing Laboratory	Page 1 of 4
Author: Paul Bredt	Effective Date: Upon Final Approval Supersedes Date: New
Use Category Identification: Reference	
Identified Hazards: Radiological Hazardous Materials Physical Hazards Hazardous Environment Other:	Required Reviewers: X Technical Reviewer Building Manager Radiological Control ES&H Quality Engineer
Arc One-Time Modifications Allowed to this Pro NOTE: If Yes, then modifications are not anticipated to see SBMS or the controlling Project QA Plan as appropri	cedure? X Yes No impact safety. For documentation requirements of a modification ate.
n-The Job Training Required? Yes orX	_No
Approval Signature	Date

PR Bredt 05/12/00 Test Plan: BNFL-TP-29953-073 Addendum 1 Page 2 of 4

High Activity Melter Feed Rheological and Physical Properties Measurements

Instructions

Under Test Plan BNFL-29953-073, "High Activity Melter Feed Rheological and Physical Properties Measurements", samples of the C-104 and AZ-102 melter feeds were adjusted to 5, 15, and 25 wt% solids. Duratek has provided BNFL with specifications for secondary waste product and glass former addition to the initial feeds (20 wt% for C-104 and 9.54 wt% for AZ-102). This addendum to the test plan defines specifications for secondary waste product and glass formers additions to the adjusted concentrations.

Secondary waste products to be added to the C-104 waste include Cs eluant and Sr/TRU precipitate. Given the limited quantity of actual secondary waste products currently available, simulated secondary waste products will be used for C-104 testing. Secondary waste products to be added to AZ-102 include Cs eluant, Tc eluant, and Sr/TRU precipitate. Actual secondary waste products will be used for AZ-102 testing.

The Cs eluant simulant will be prepared using the Concentrated Cs Eluant data provided on page 25 of the SRTC report "Estimation of Physical Properties of Tank 241-AN-107 Cesium and Technetium Eluate Concentrate Blend" by Alexander S. Choi. This Cs eluant is approximately 0.14 g of oxide/ml of simulant and 27 wt% dry solids.

The Sr/TRU simulant will be prepared from an AN-107 simulant. The Sr/TRU simulant will be adjusted to 25 wt% solids prior to addition. Both the Sr/TRU precipitate and Cs eluant will be analyzed by ICP prior to addition to the actual waste.

Table 1 provides the specifications for a 400 g sample of C-104 at 20 wt% solids. This is the basis used in Test Instruction 29953-079 Rev.1 that reflects the Duratek specification. Table 1 also provides ratios required for addition to the adjusted samples. The 400 g basis will be adjusted to the actual sample masses at the time of additions.

Table 2 provides the specifications for a 436.27 g sample of AZ-102 at 9.535 wt% solids. This is the basis used in Test Instruction 29953-079 Rev. 1 Addendum 5 that reflects the Duratek specification. Since the AZ-102 sample masses are known, Table 2 defines exactly how much of each material is to be added to each of the samples.

Table 3 lists the AZ-102 samples received for this testing. At the conclusion of the AZ-102 testing, all AZ-102 material will be composited into a single jar labeled "AZ-102 Melt 2 COMP" for transfer to the vitrification task.

The quantity of Cs eluant and Tc eluant required for the AZ-102 process baseline is very small. The Cs and Tc eluants are to be added at 27 and 25 wt% solids respectively, and they are currently less than approximately 0.2 and 0.02 wt% solids respectively. Therefore, following evaporation to the correct water content, these small additions will not effect the rheological properties of the test materials.

Glass formulations in this report for AW-101 and AN-107 are considered to be proprietary by VSL/Duratek

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Addendum 1 Page 3 of 4

For example, the largest addition would be less than 0.32g of Cs eluant addition to the 136.56 g sample Rheol-25-1:

(137.83 g eluant/436.69g waste) x (0.002 g solids/g eluant) x (1 g concentrated eluant /0.27 g solids) x (136.56 g waste) = 0.319 g concentrated eluant

Given the small amounts of concentrated eluants required, the Cs and Tc eluants will not be added for rheological testing. The diluted eluants (137.83 and 76.67 g respectively) will be added directly to the final sample "AZ-102 Melter 2 COMP" prior vitrification task.

Table 1. Secondary waste products and glass formers to be added to C-104 melter feed.

Additive		Target (g) per	400g of Slurry	
Additive	20 wt%	5 wt%	15 wt%	25 wt%
Sr/TRU Precipitate (dry solids basis)	25.674	6.418	19.256	32.092
Cs Eluant				
(27 g total solids/ml solution)	8.8 ml	2.2 ml	6.6 ml	11 ml
Na ₂ B ₄ O ₇ +10H ₂ O	58.000	14.500	43.500	72.500
LiOH+H ₂ O	36.800	9.200	27.600	46.000
Na ₂ CO ₃	3.525	0.88125	2.64375	4.406
SiO ₂ (Sil-co-Sil 75)	116.280	29.070	87.210	145.350
ZnO (KADOX-920)	4.93	1.232	3.698	6.162
Sugar (Granular)	0	. 0	- 0	0

Glass formulations in this report for AW-101 and AN-107 are considered to be proprietary by VSL/Duratek

PR Bredt 05/12/00

Test Plan: BNFL-TP-29953-073

Addendum 1 Page 4 of 4

Table 2. Secondary waste products and glass formers to be added to AZ-102 Melt-2 melter feed in grams. The AZ-102 Slurry Basis is 9.535 wt% solids.

Sample	Slurry Basis	Rheol-5	Rheol- 15	Rheol- 25-1	Rheol- 25-2
Slurry Mass (g)	436.69	41.84	122.00	136.53	136.32
Sr/TRU Precipitate (25 wt% solids basis)	10.38g x (46.26 wt%/25 wt%) = 19.21	1.841	5.367	6.006	5.997
Actual Cs Eluant (Diluted Basis)	137.83	13.206	38.506	43.092	43.026
Actual Tc Eluant (Diluted Basis)	76.67	7.346	21.420	23.971	23.934
Na ₂ B ₄ O ₇ +10H ₂ O	10.76	1.031	3.006	3.364	3.359
LiOH+H ₂ O	15.51	1.486	4.333	4.849	4.842
Na ₂ SiO ₃ +5H ₂ O	32.09	3.075	8.965	10.033	10.017
SiO ₂ (Sil-co-Sil 75)	39.73	3.807	11.100	12.421	12.402
Sugar (Granular)	1.34	0.128	0.374	0.419	0.418

Table 3. Samples of AZ-102 slurry received for testing. Samples are 9.535 wt% solids.

Sample	Mass (g)
AZ-102 Washed Sludge:Rheol-5	41.84
AZ-102 Washed Sludge:Rheol-15	122.00
AZ-102 Washed Sludge:Rheol-25-1	136.53
AZ-102 Washed-Sludge:Rheol-25-2	136.32

PNNL Test Instruction To Supplement TP-29953-073

Document No.: BNFL-TP-29953-073

Rev. No.: 0

Document Control: Only the original signed copy

is controlled

Work Location: Radiochemical Processing Laboratory	Page 1 of 3
Author: Paul Bredt	Effective Date: Upon Final Approval
Use Category Identification: Reference	Supersedes Date: New
Identified Hazards: Radiological Hazardous Materials Physical Hazards Hazardous Environment Other:	Required Reviewers: X Technical Reviewer Project Manager Building Manager RPL Manager Radiological Control SFO Manager ES&H Quality Engineer
Are One-Time Modifications Allowed to this NOTE: If Yes, then modifications are not anticipat SBMS or the controlling Project QA Plan as appropriate the controlling P	ed to impact safety. For documentation requirements of a modification see riate.
FOR REVISIONS: s retraining to this procedure required?Yes	
FOR REVISIONS: s retraining to this procedure required?Yes Does the OJT package associated with this procedure YesNoN/A	X_No require revision to reflect procedure changes?
FOR REVISIONS: s retraining to this procedure required?Yes Does the OJT package associated with this procedure YesNoXN/A	XNo require revision to reflect procedure changes?
FOR REVISIONS: s retraining to this procedure required?Yes Does the OJT package associated with this procedure YesNoN/A	XNo require revision to reflect procedure changes?
OOR REVISIONS: s retraining to this procedure required?Yes Ooes the OJT package associated with this procedure YesNoX_N/A pproval Signat	

Test Plan: BNFL-TP-29953-073 Addendum 1 Page 2 of 3

High Activity Melter Feed Rheological and Physical Properties Measurements

Scope

This test instruction provide specific details regarding the implementation of Test Plan BNFL-29953-073 Addendum 1, "High Activity Melter Feed Rheological and Physical Properties Measurements". Addendum 1 to this Test Plan, provides the ratio of glass formers, and secondary waste products to be added to each of the AZ-102 melter feed samples. However, due to changes in client needs, not all of the steps in the Test Plan were implemented. As a result, the samples do not contain all ingredient required for the sample transfer to the Vitrification Task as specified in Test Plan 29953-073 Addendum 1. This test Instruction provides the details required to prepare the feed for the Vitrification Task.

Work Instructions

Weigh a clean 500 ml glass jar labeled AZ-102 Melter 2 COMP. 18.+er PRB 6/14/00

AZ-102 Melter 2 COMP

Transfer the material in A7-102 Phones & A7-10

Transfer the material in AZ-102 Rheol-5, AZ-102 Rheol-15, and AZ-102 Rheol-25-1 to AZ-102 Melter 2 COMP. Use deionized water as needed to transfer the material.

Weigh 25.116g of AZ-102 Glass formers from the jar labeled AZ-102 Glass to a clean 40 ml 3) vial or similar container. Weigh the material in the vial.

> Clean Vial Total 49.6894 g
> Tare 24.5595 g
> Solids 25.1299 g

Transfer the glass formers collected in the previous step to AZ-102 Melter 2 COMP

Weigh 2.33g of material from the jar labeled AN-107 DF SOLIDS to a clean 20 ml vial or similar container. Weigh the material in the vial.

Clean Vial used + platic boot

Total
Tare

Solids

1.367 eAG V 115/60

Clean Vial

Used + platic boot

Total

For rest of Test Instruction.

TRO 4/14/08

Transfer the AN-107 DF SOLIDS collected in the previous step to AZ-102 Melter 2 COMP.

Test Plan: BNFL-TP-29953-073 Addendum 1

Page 3 of 3

Weigh 86.5g of Cs eluant into a clean 125 ml jar or similar container. Weigh the material in the jar. Record the label on the original Cs eluant bottle.

Cs Eluant Bottle C5 10f2 composite 3/00" mass on 6/14/00 = 733.33, before renoving material 203.477 Clean Jar Total <u>203,477</u> g Tare 116.98 g

- Transfer the Cs eluant collected in the previous step to AZ-102 Melter 2 COMP.
- 9) Weigh 48.133g of Tc eluant into a clean 125 ml jar or similar container. Weigh the material in the jar. Record the label on the original Cs eluant bottle.

To Eluant Bottle "A2-102 Te Me 1+ #2" mass on 6/14/00 = 240.485 g

Clean Jar

Total 164.500 g

Tare 44.99 g

Solids 48.192 g

- 10) Transfer the Tc eluant collected in the previous step to AZ-102 Melter 2 COMP.
- 11) Mix the material in AZ-102 Melter 2 COMP and describe the mixing technique and observations below.

below.

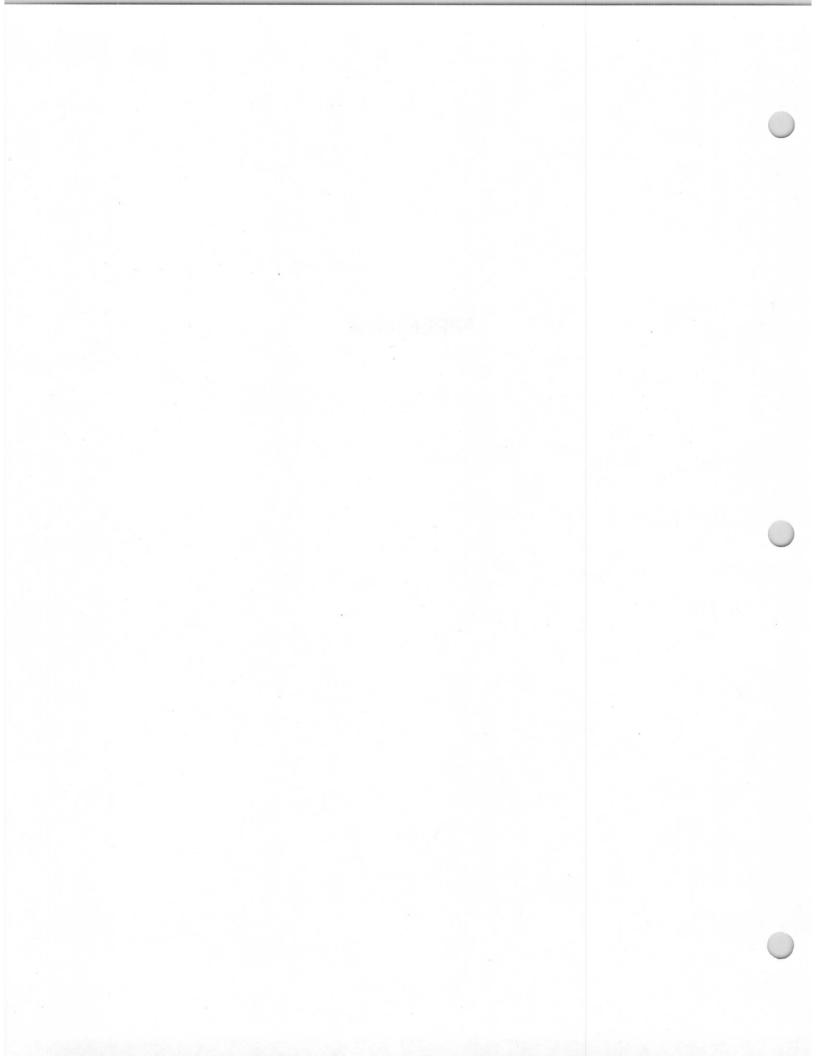
Sample mixed using a Braun hand blender modified for hot cell operation for -/min.

6/15/00

PRB

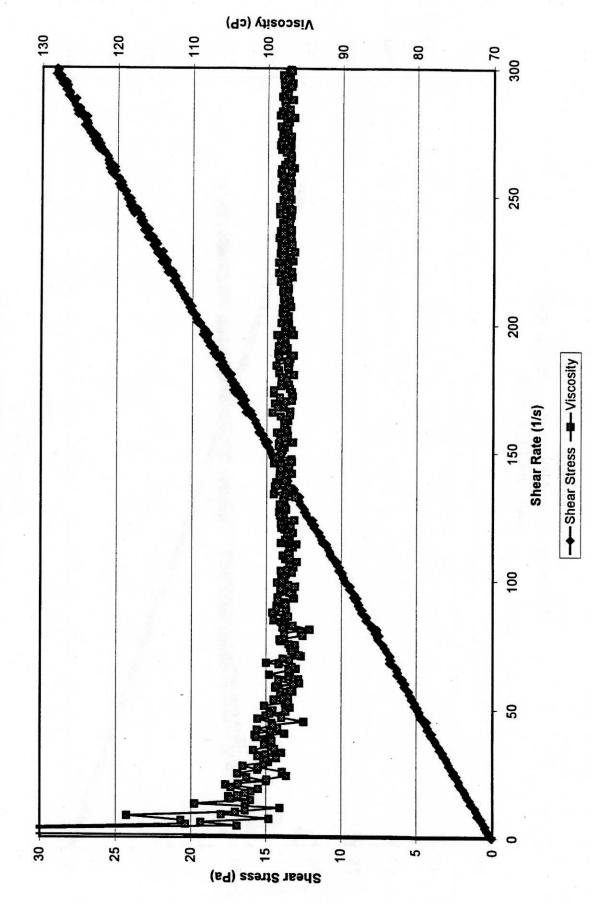
@ 9:15 am

APPENDIX B

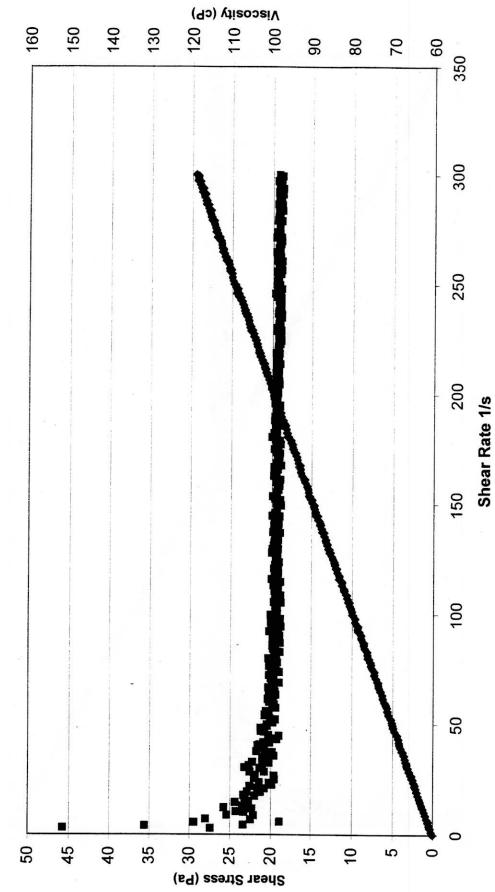


Appendix B: Rheograms

95.5 cP Brookfield Standard: 25°C on 5/2/00

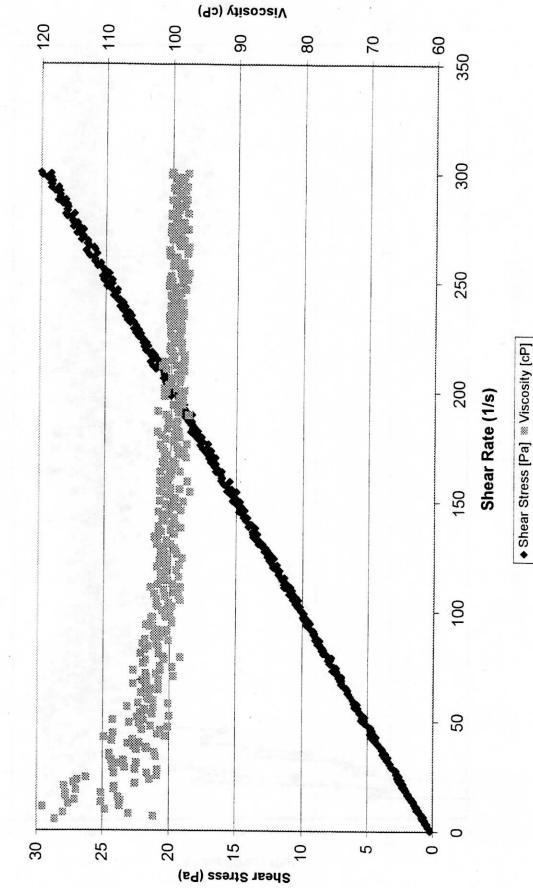


95.5 cP Standard Lot #111199 Shear Stress and Viscosity vs. Shear Rate Analysis #1 (06/01/00)



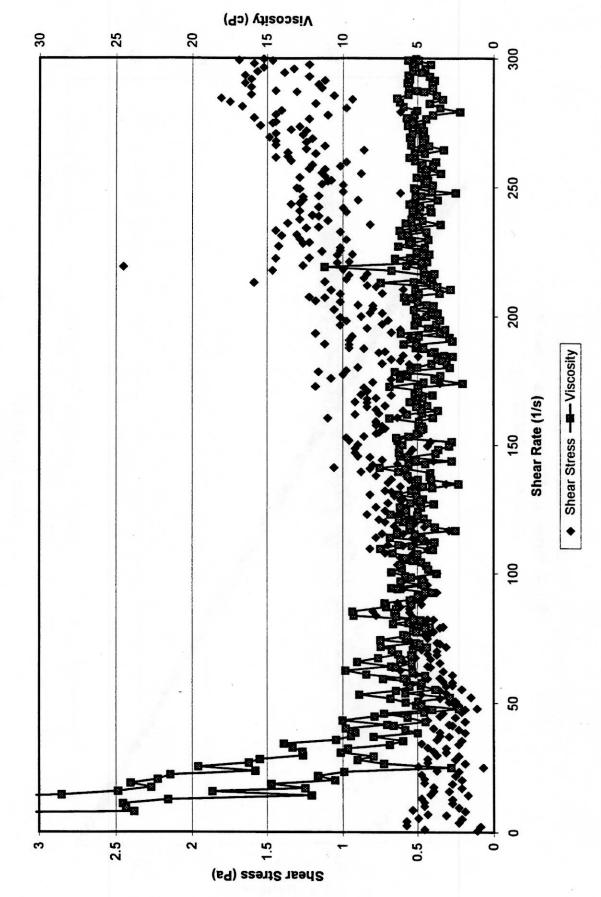
◆ Shear Stress [Pa] ■ Viscosity [cP]

95.5 cP Standard Lot #111199 Shear Stress and Viscosity vs. Shear Rate Analysis #1 (07/20/00)



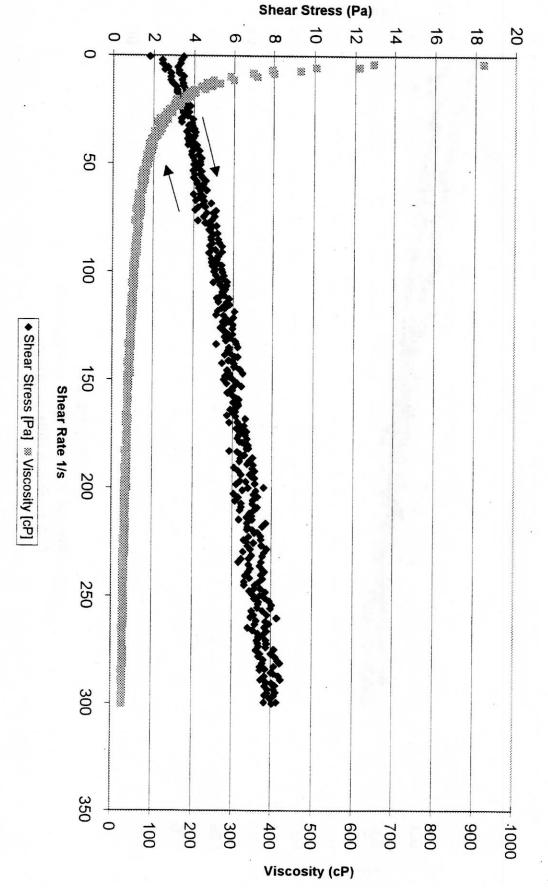
Measurement performed with a Haake M5 and MV I sensor

AZ-102 Melter Feed 5wt% Solids: 25°C, Analysis 1

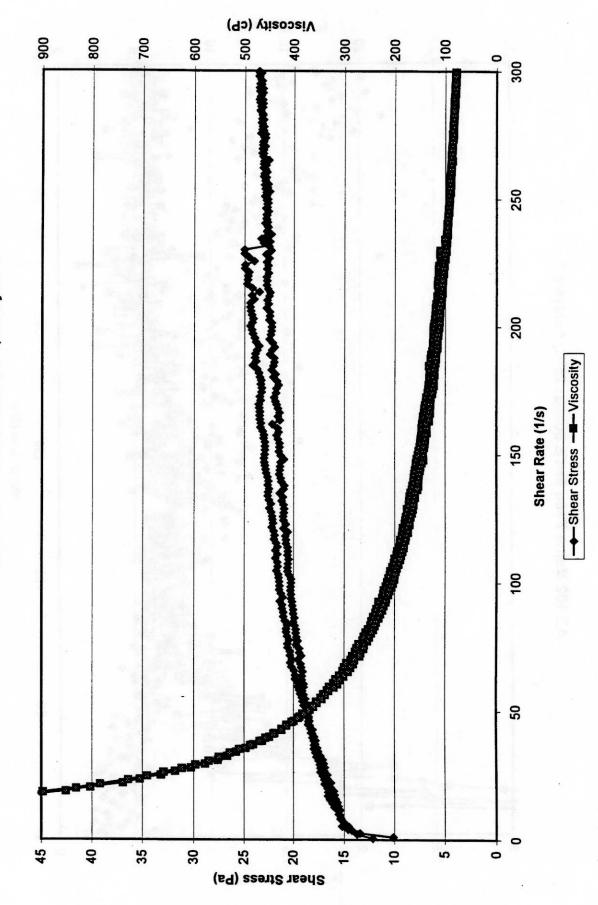


Haake M5 Viscometer with SV1 Geometry

AZ-102 Mixing Study - 1 Day Shear Stress and Viscosity vs. Shear Rate Analysis #2

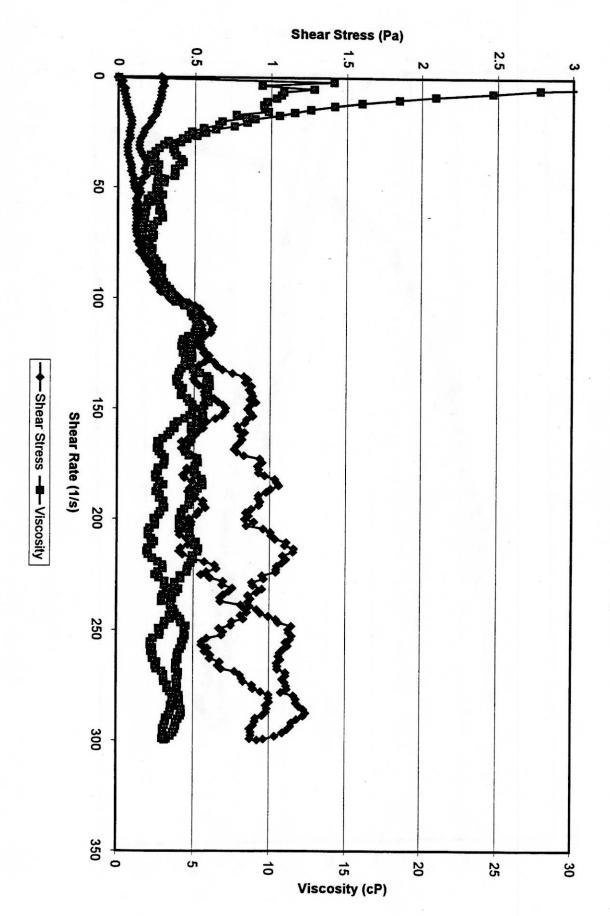


AZ-102 Melter Feed 15wt% Solids: 25°C, Analysis 1



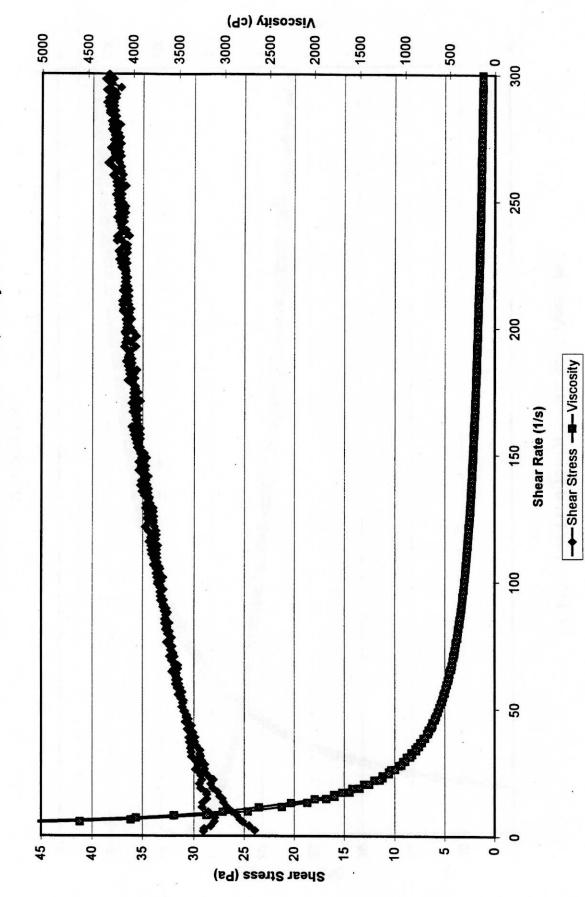
Haake M5 Viscometer with SV1 Geometry

C-104 Melter Feed 5wt% Solids: 50°C, Analysis 1



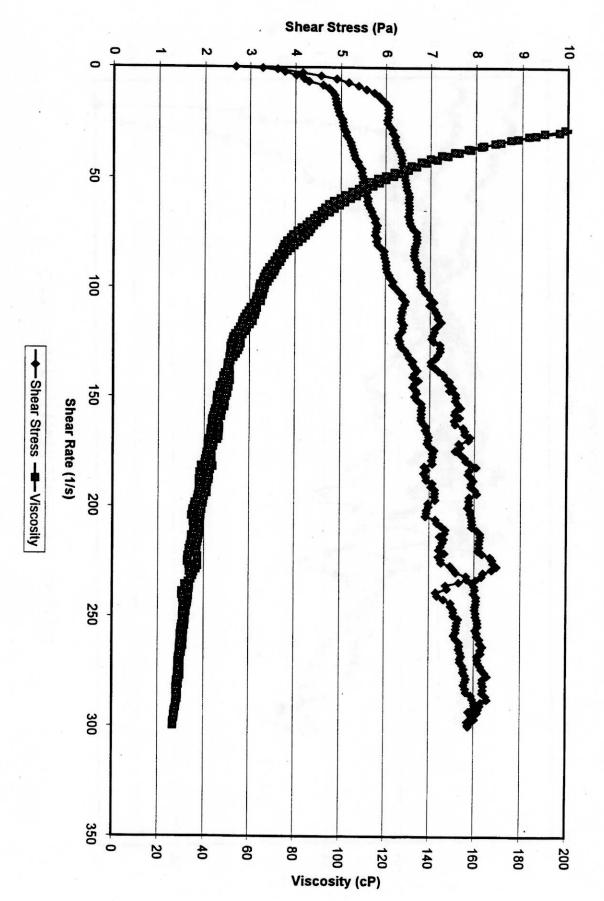
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

AZ-102 Melter Feed 20 wt% Solids: 25°C, Analysis 1

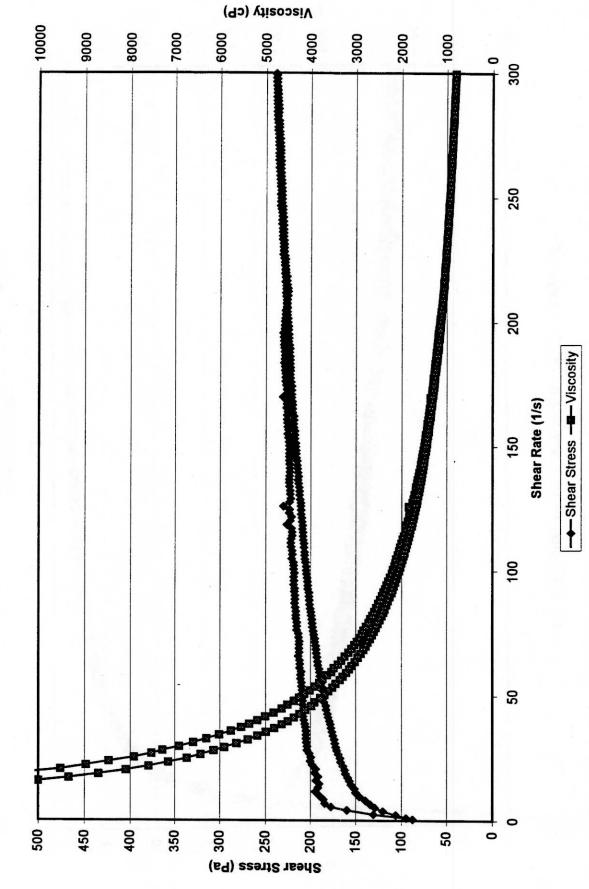


Haake M5 Viscometer with SV1 Geometry

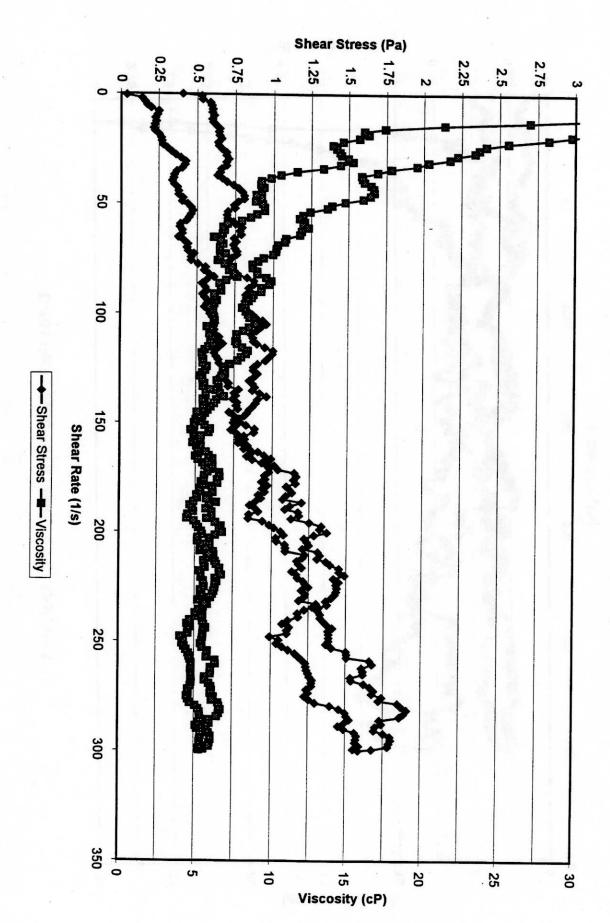
C-104 Melter Feed 25wt% Solids: 25°C, Analysis 1



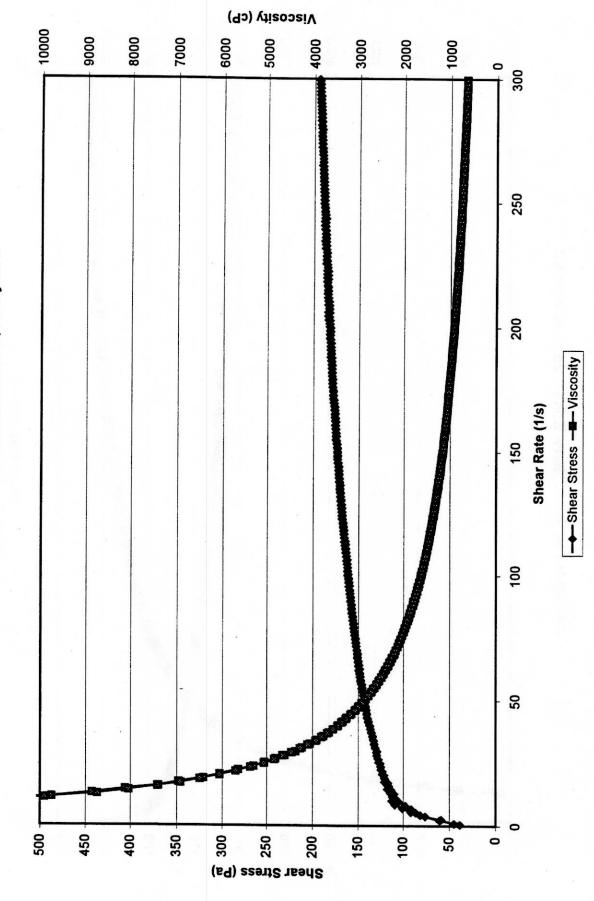
AZ-102 Melter Feed 25wt% Solids: 25°C, Analysis 1



C-104 Melter Feed 15wt% Solids: 25°C, Analysis 1

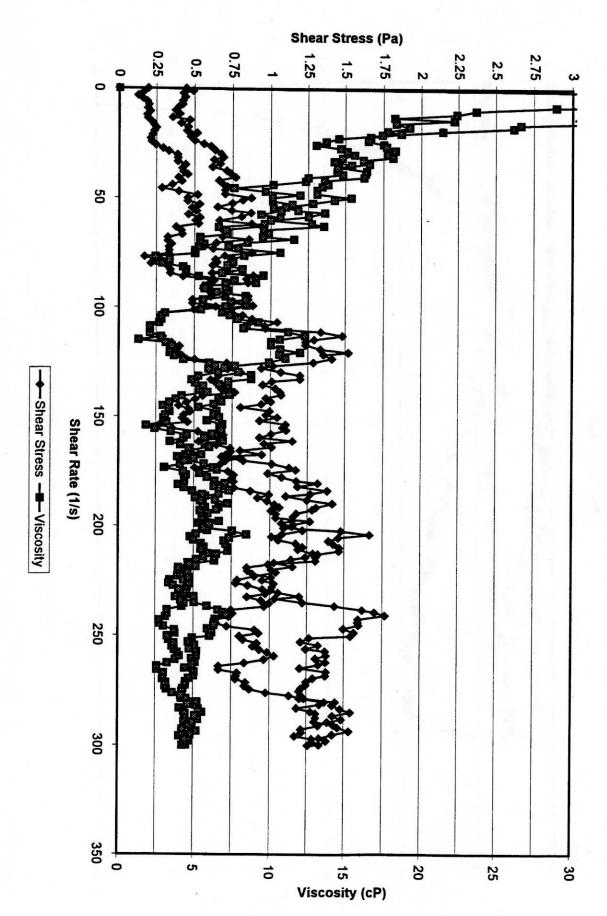


AZ-102 Melter Feed 25wt% Solids: 25°C, Analysis 3

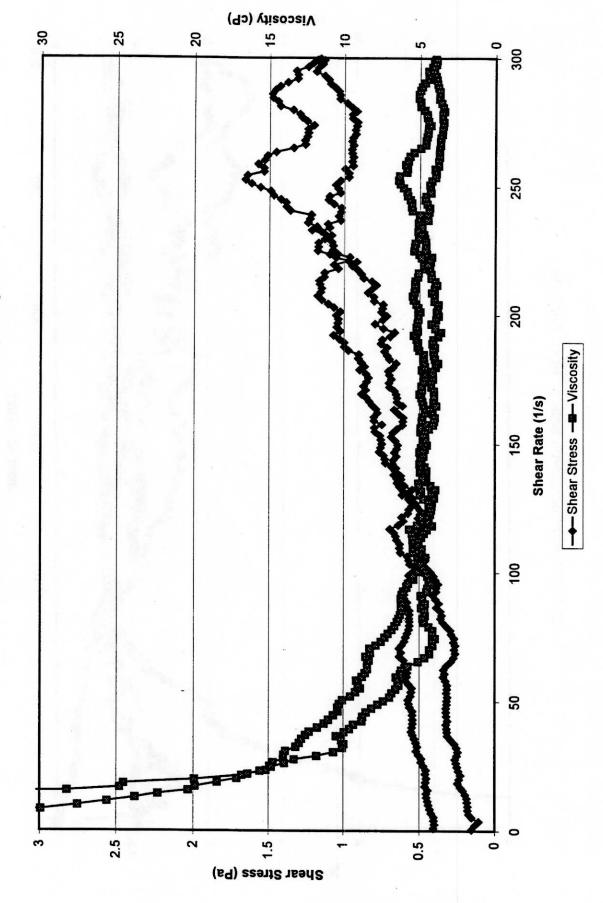


Haake M5 Viscometer with SV1 Geometry

C-104 Melter Feed 5wt% Solids: 25°C, Analysis 2

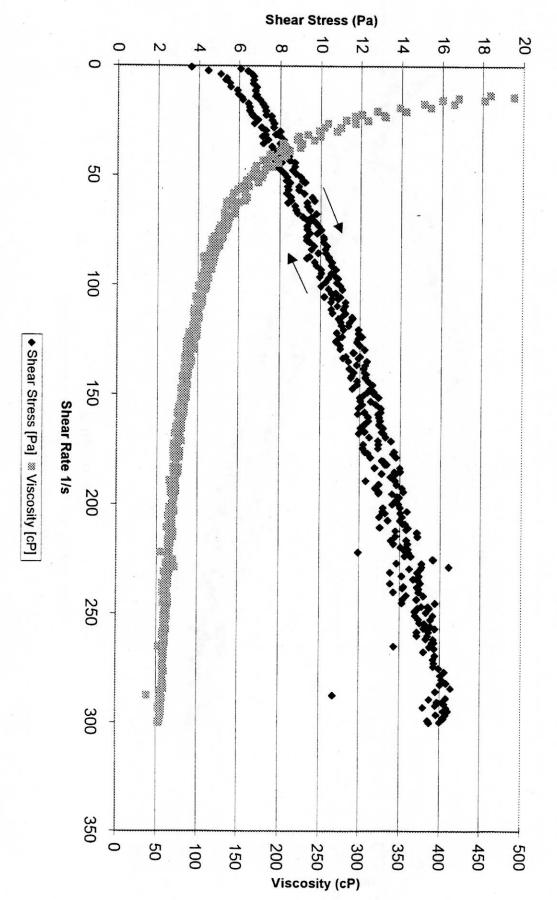


AZ-102 Melter Feed 5wt% Solids: 50°C, Analysis 2

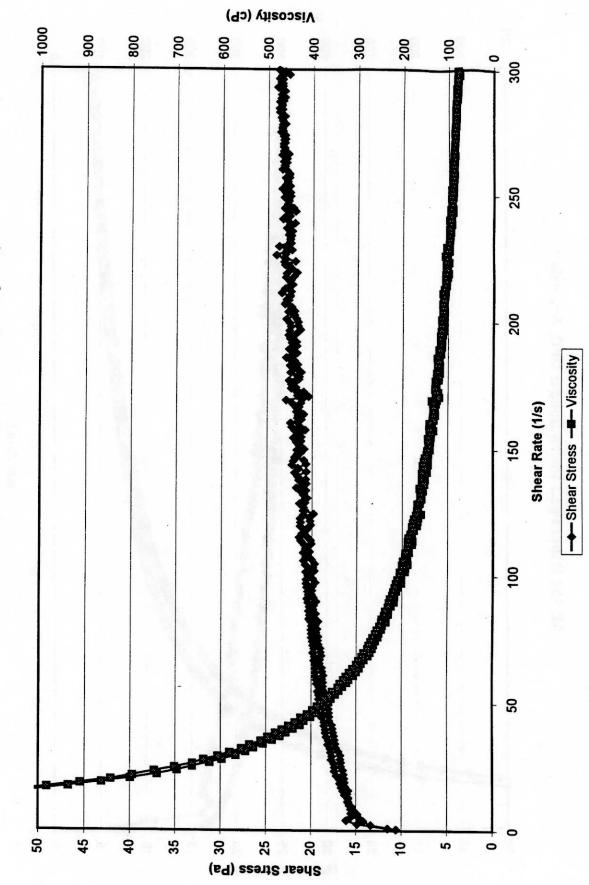


Haake M5 Viscometer with SV1 Geometry

AZ-102 Aging Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #2

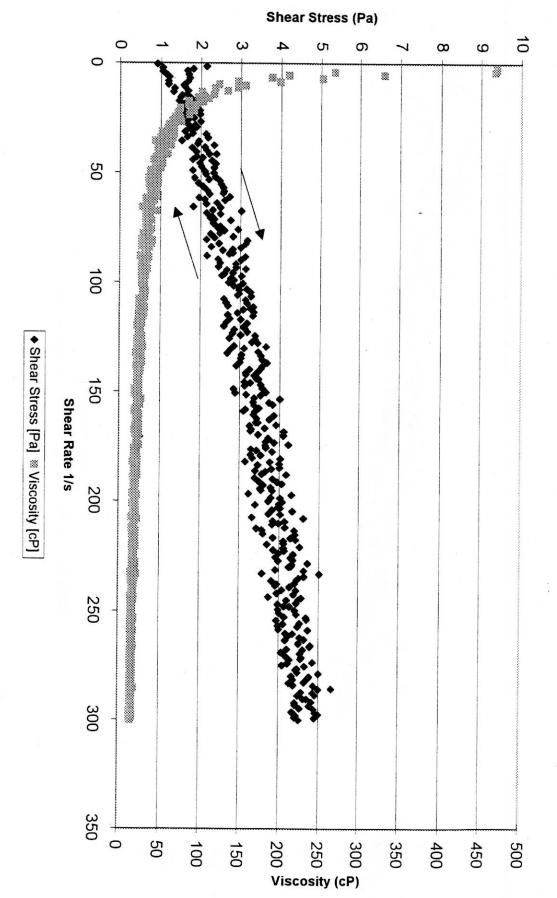


AZ-102 Melter Feed 15wt% Solids: 50°C, Analysis 2

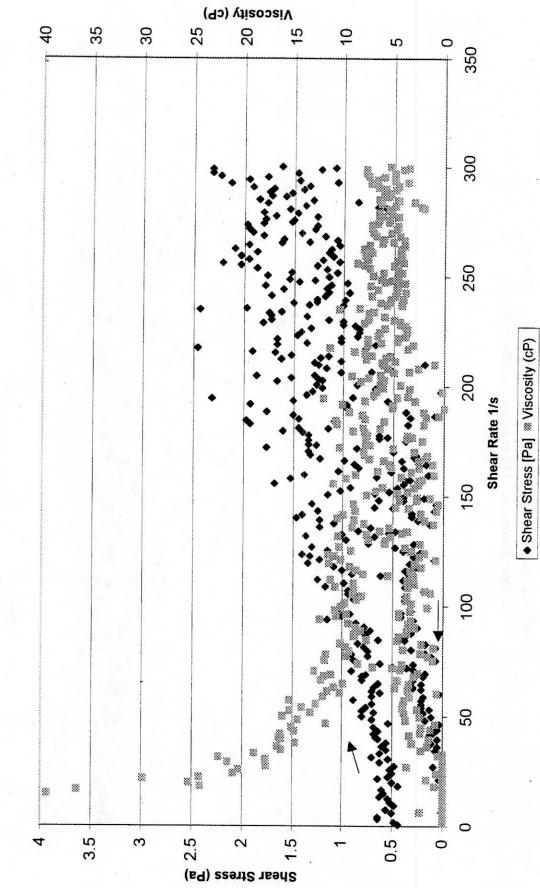


Haake M5 Viscometer with SV1 Geometry

AZ-102 Mixing Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #2

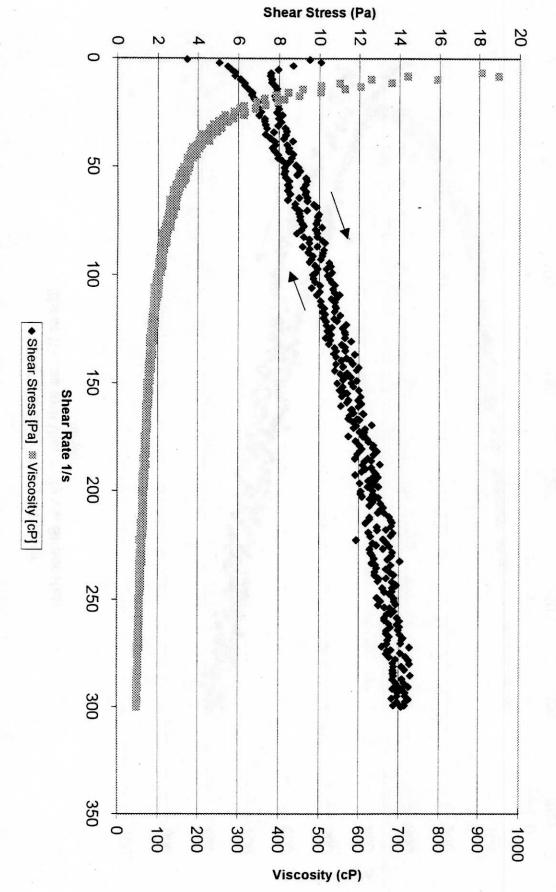


AZ-102 w/secondary waste & glass formers - 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2

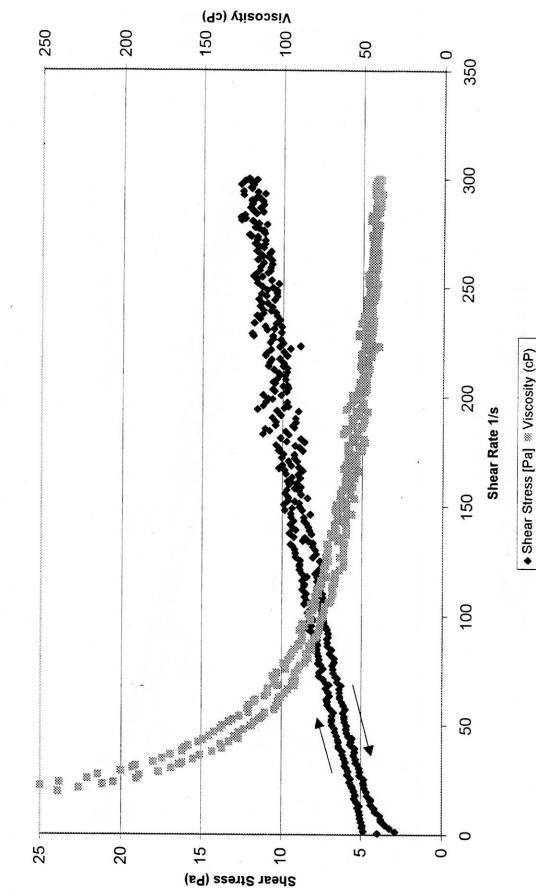


Measurement performed with a Haake M5 and SV I sensor

AZ-102 Mixing Study - 1 Hour Shear Stress and Viscosity vs. Shear Rate Analysis #2

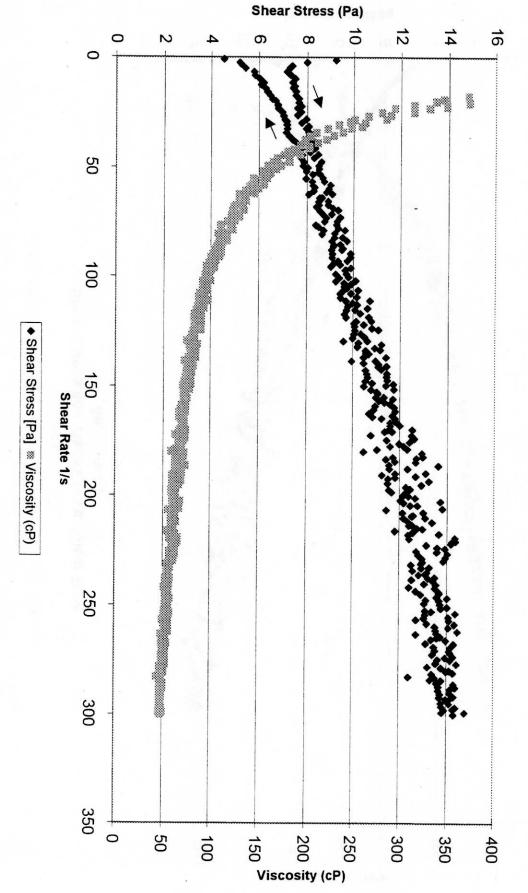


AZ-102 w/secondary waste & glass formers - 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2

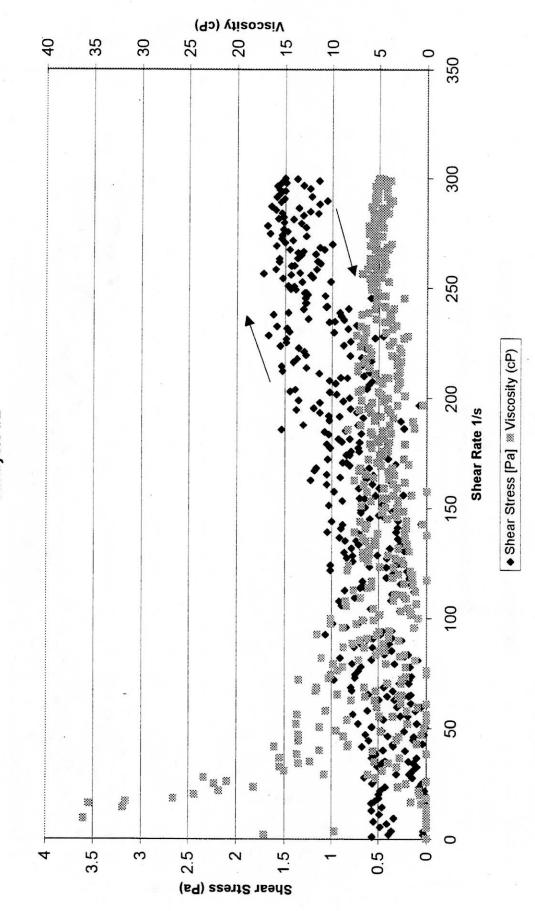


Measurement performed with a Haake M5 and SV I sensor

AZ-102 w/secondary waste & glass formers - 15wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #2

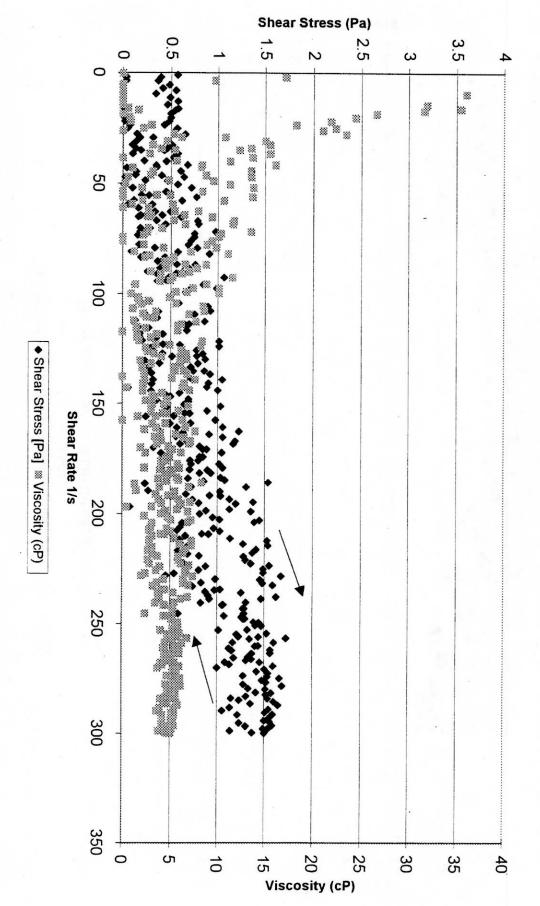


AZ-102 w/secondary waste & glass formers - 5wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #2

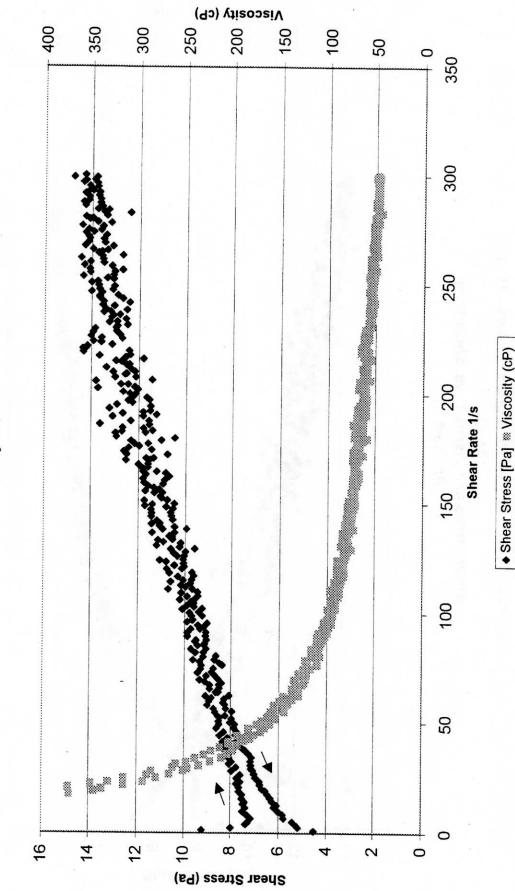


Measurement performed with a Haake M5 and SV I sensor

AZ-102 w/secondary waste & glass formers - 5wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #2

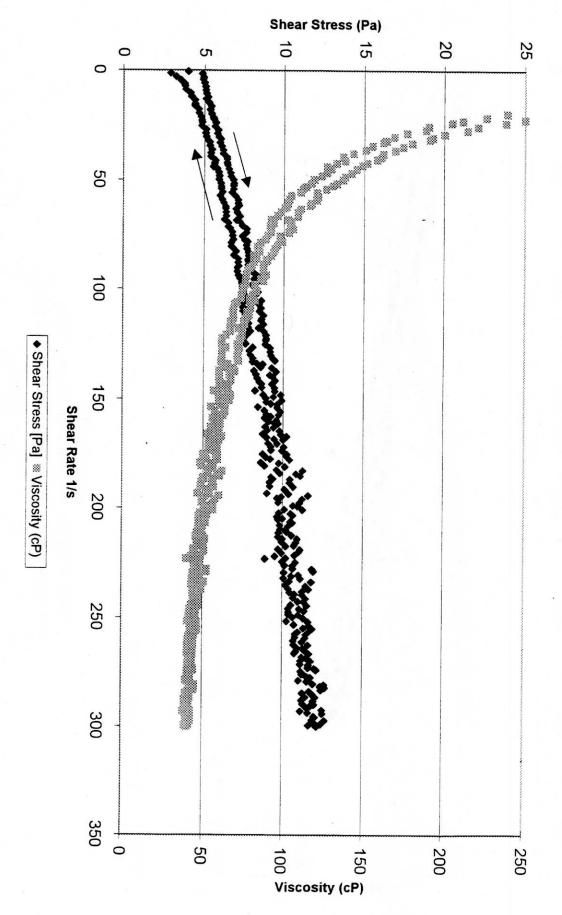


AZ-102 w/secondary waste & glass formers - 15wt% @ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #2

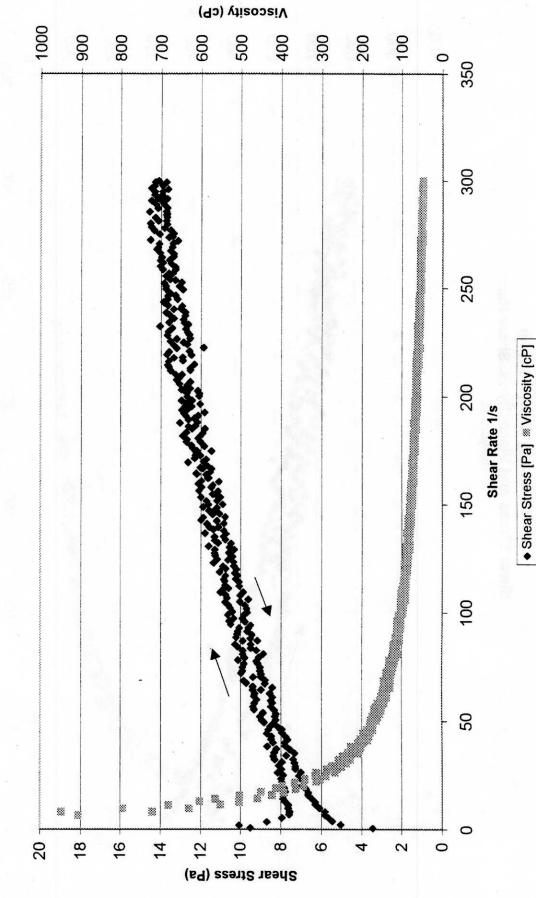


Measurement performed with a Haake M5 and SV I sensor

AZ-102 w/secondary waste & glass formers - 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2

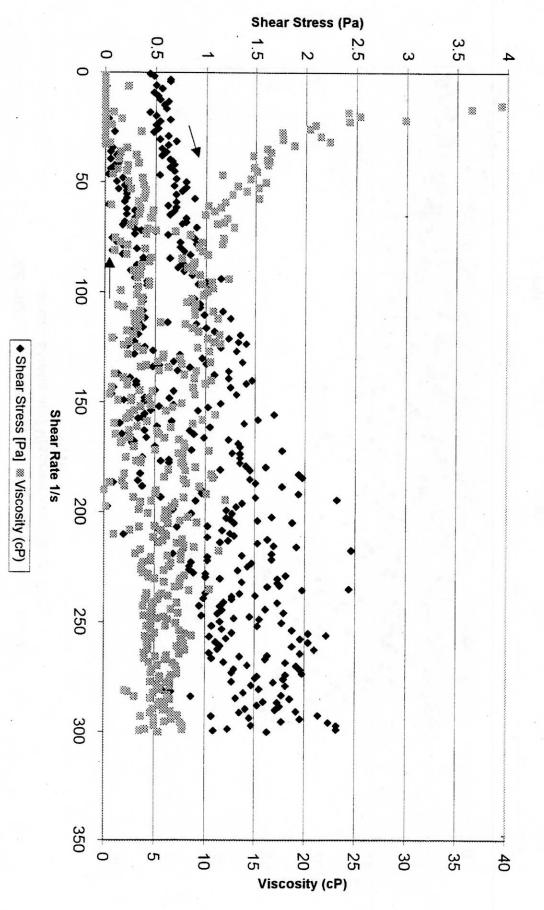


AZ-102 Mixing Study - 1 Hour Shear Stress and Viscosity vs. Shear Rate Analysis #2

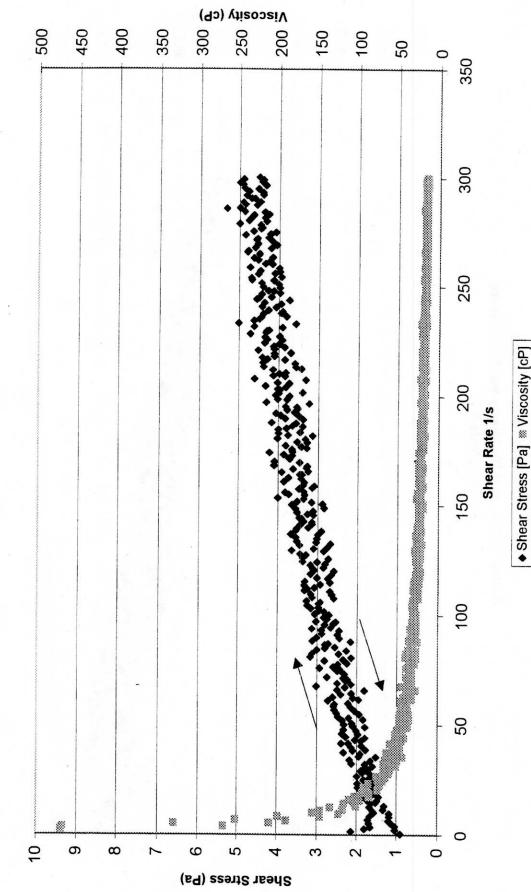


Measurement performed with a Haake M5 and SV I sensor

AZ-102 w/secondary waste & glass formers - 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2

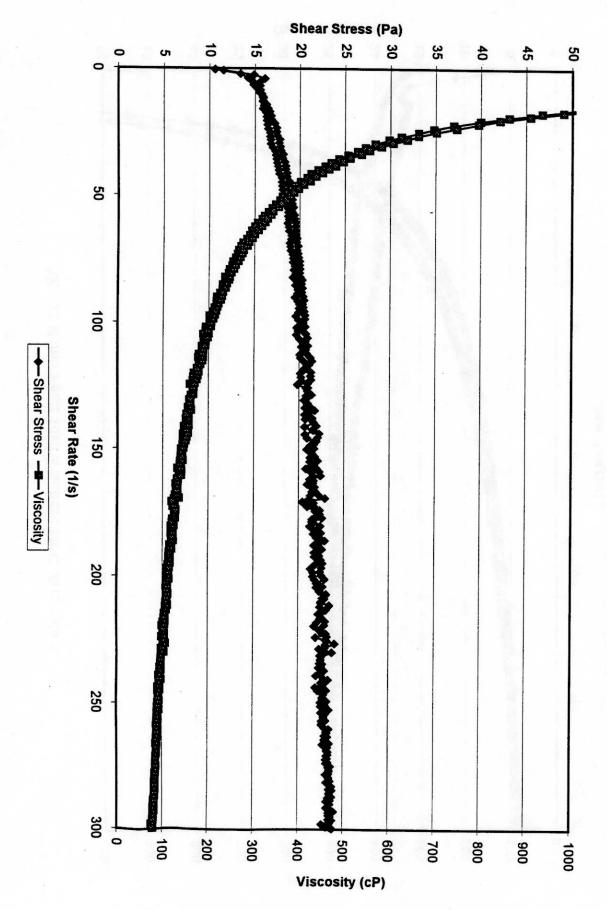


AZ-102 Mixing Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #2



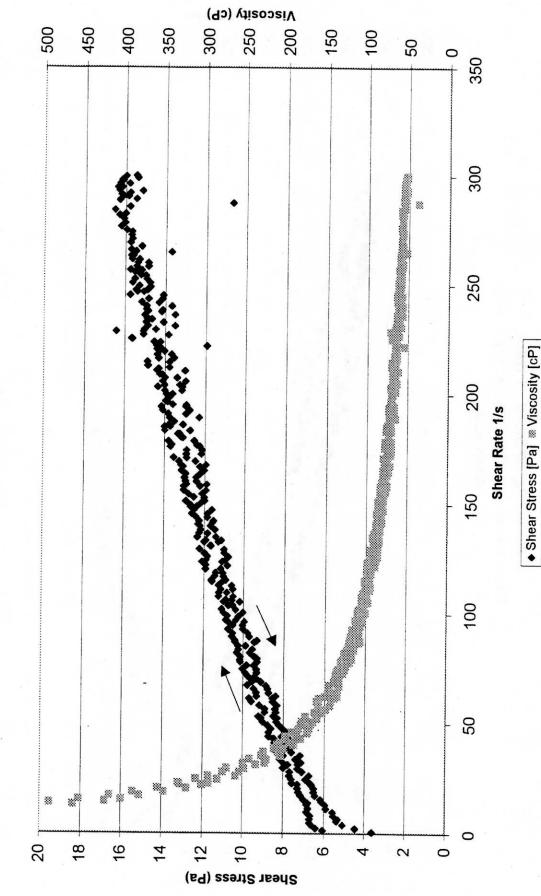
Measurement performed with a Haake M5 and SV I sensor

AZ-102 Melter Feed 15wt% Solids: 50°C, Analysis 2



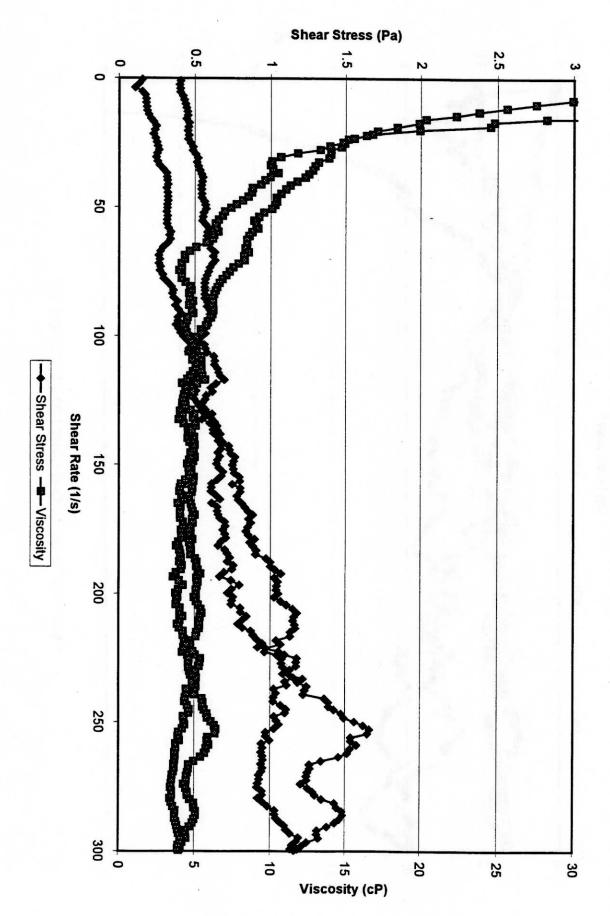
Haake M5 Viscometer with SV1 Geometry

AZ-102 Aging Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #2

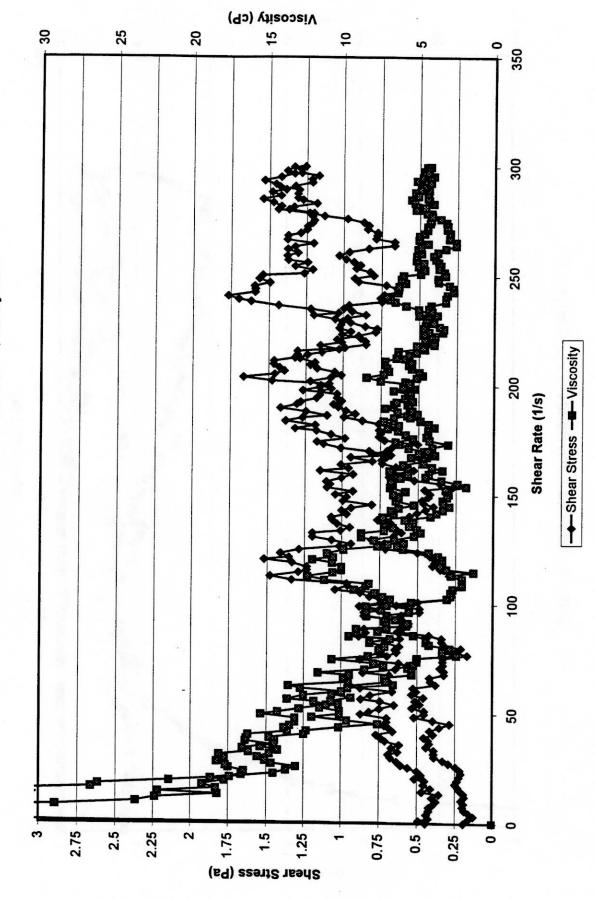


Measurement performed with a Haake M5 and SV I sensor

AZ-102 Melter Feed 5wt% Solids: 50°C, Analysis 2

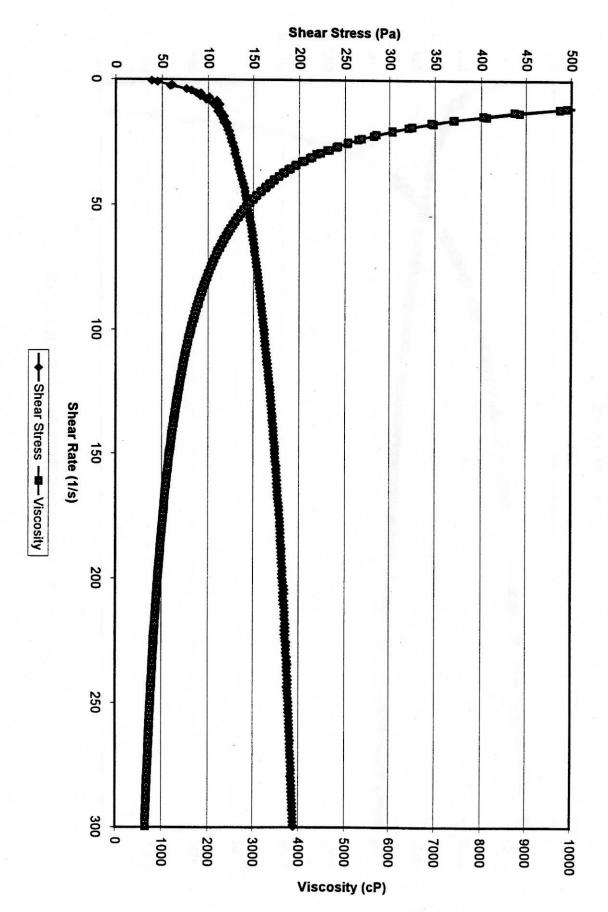


C-104 Melter Feed 5wt% Solids: 25°C, Analysis 2

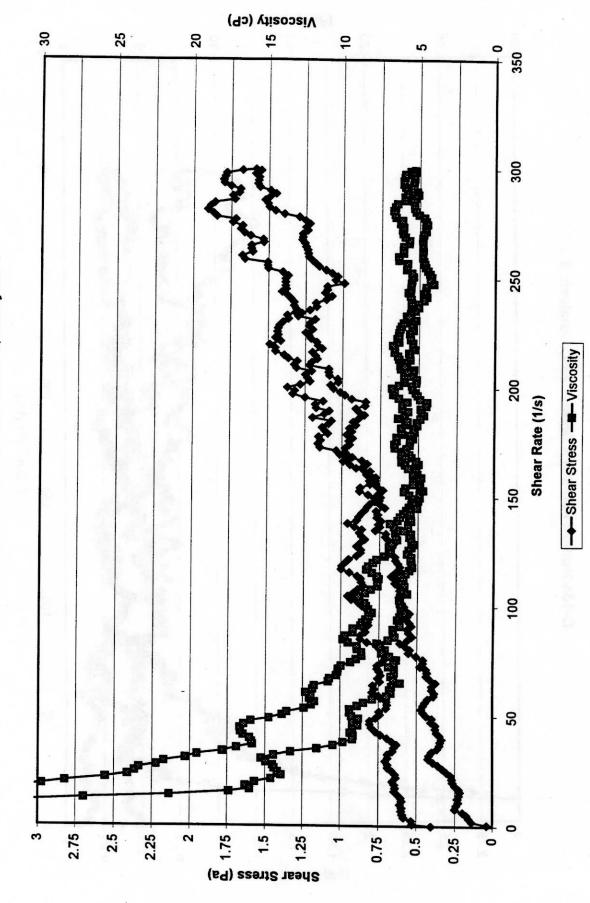


Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

AZ-102 Melter Feed 25wt% Solids: 25°C, Analysis 3

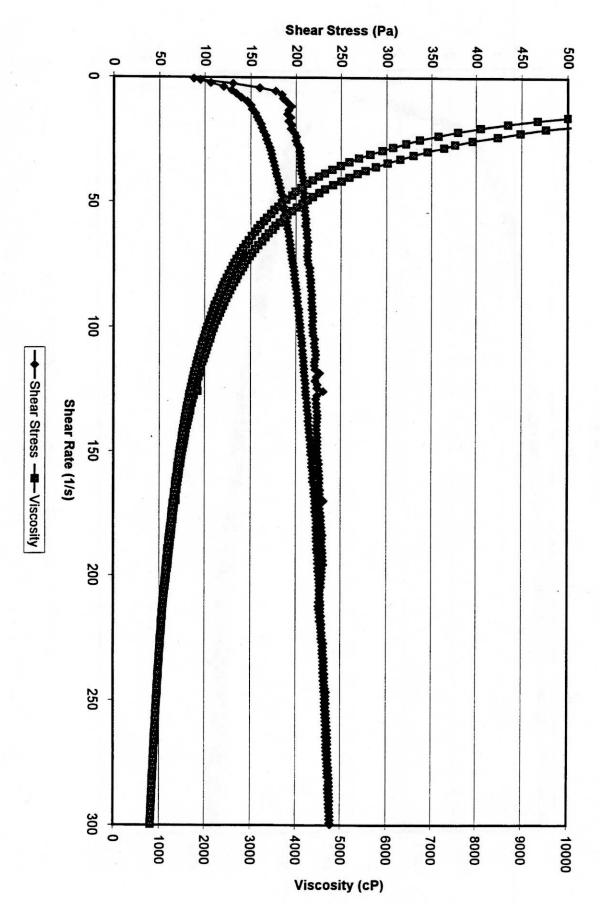


C-104 Melter Feed 15wt% Solids: 25°C, Analysis 1

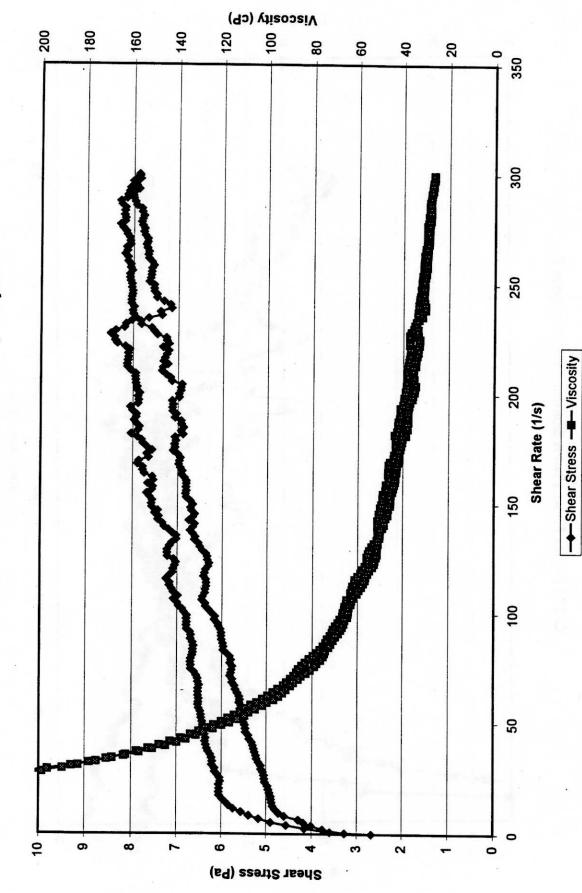


Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

AZ-102 Melter Feed 25wt% Solids: 25°C, Analysis 1

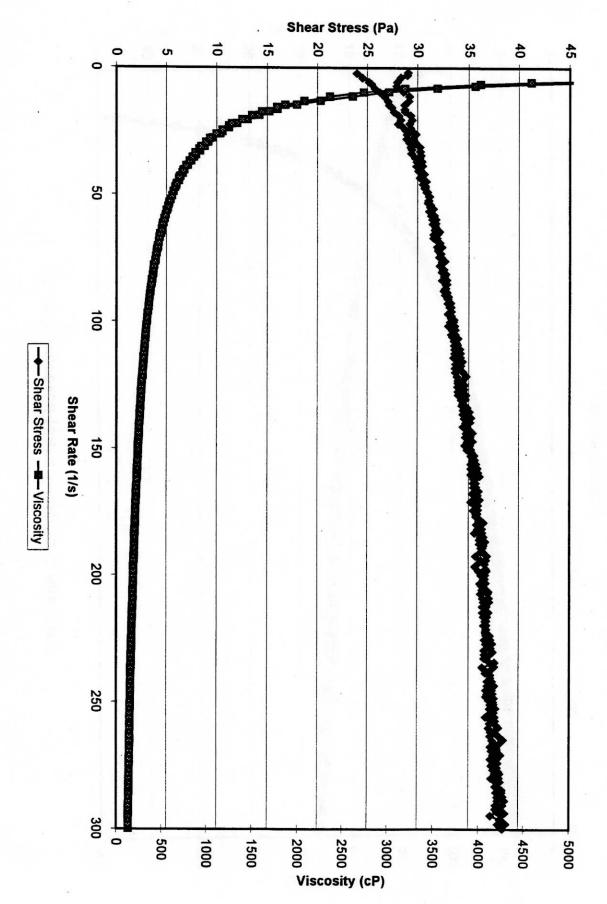


C-104 Melter Feed 25wt% Solids: 25°C, Analysis 1

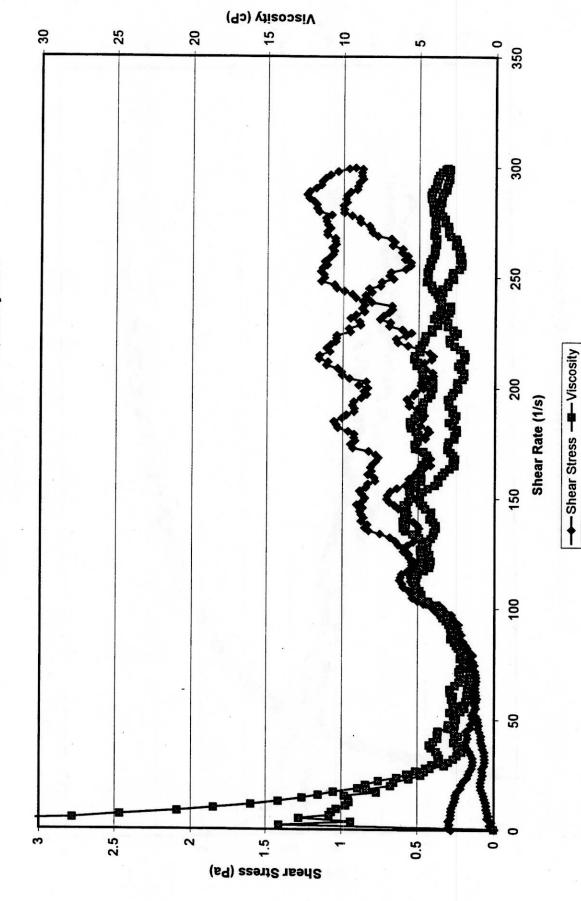


Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

AZ-102 Melter Feed 20 wt% Solids: 25°C, Analysis 1

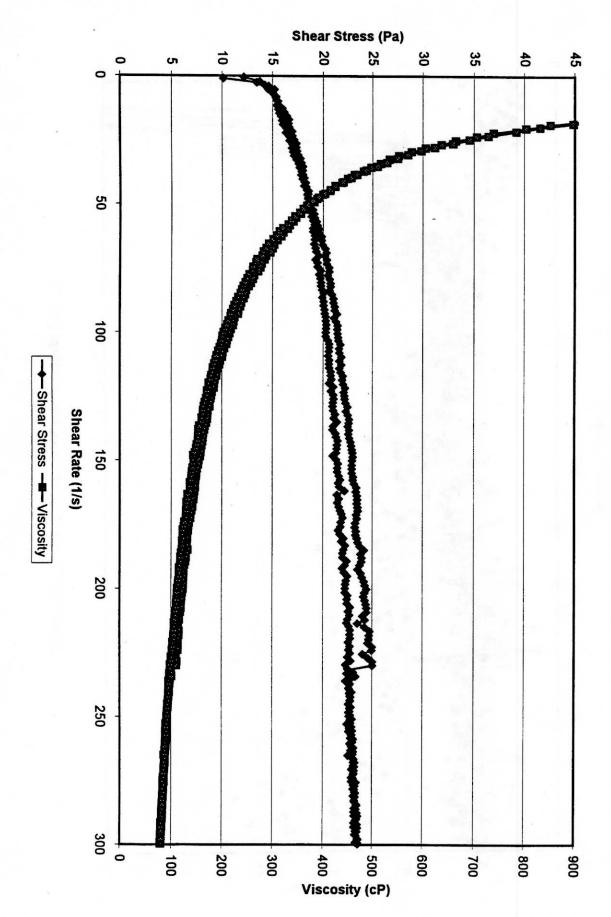


C-104 Melter Feed 5wt% Solids: 50°C, Analysis 1

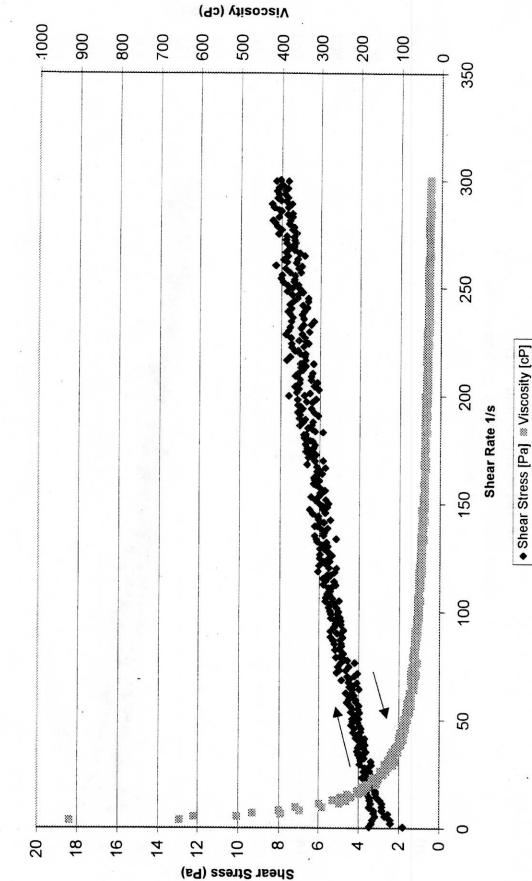


Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

AZ-102 Melter Feed 15wt% Solids: 25°C, Analysis 1

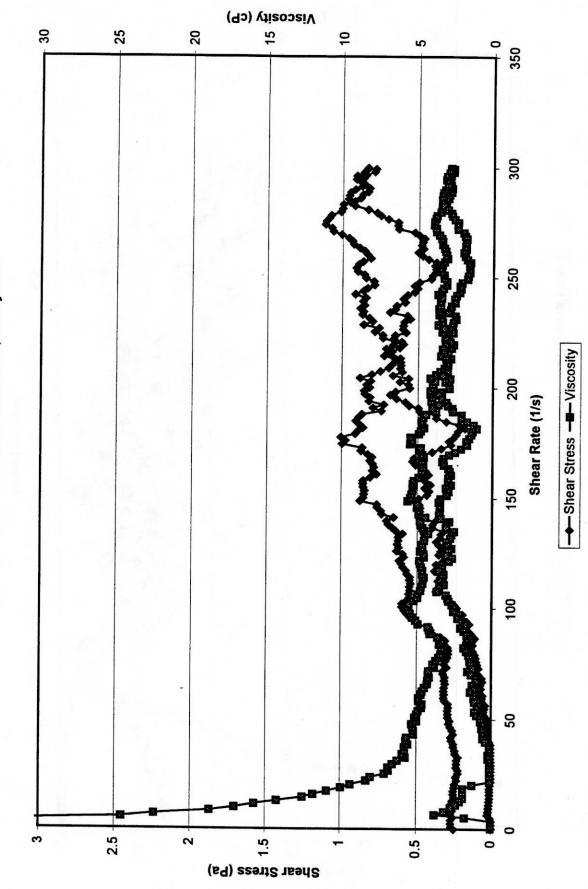


AZ-102 Mixing Study - 1 Day Shear Stress and Viscosity vs. Shear Rate Analysis #2



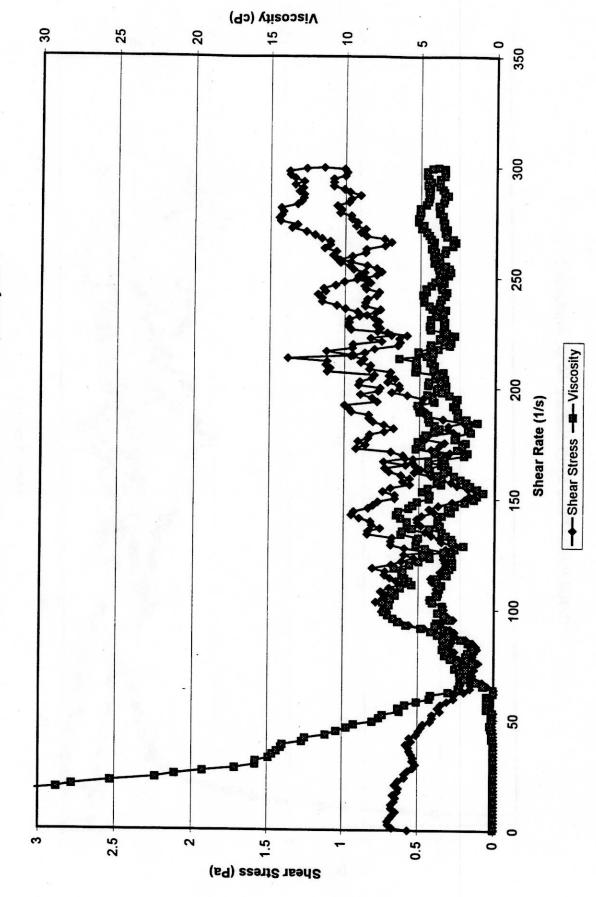
Measurement performed with a Haake M5 and SV I sensor

C-104 Melter Feed 5wt% Solids: 50°C, Analysis 2



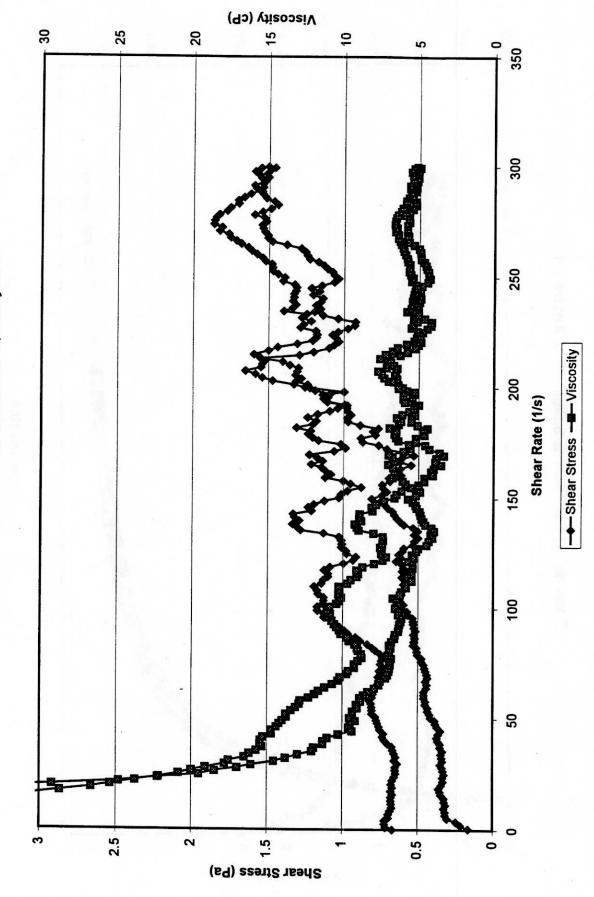
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

C-104 Melter Feed 15wt% Solids: 50°C, Analysis 1



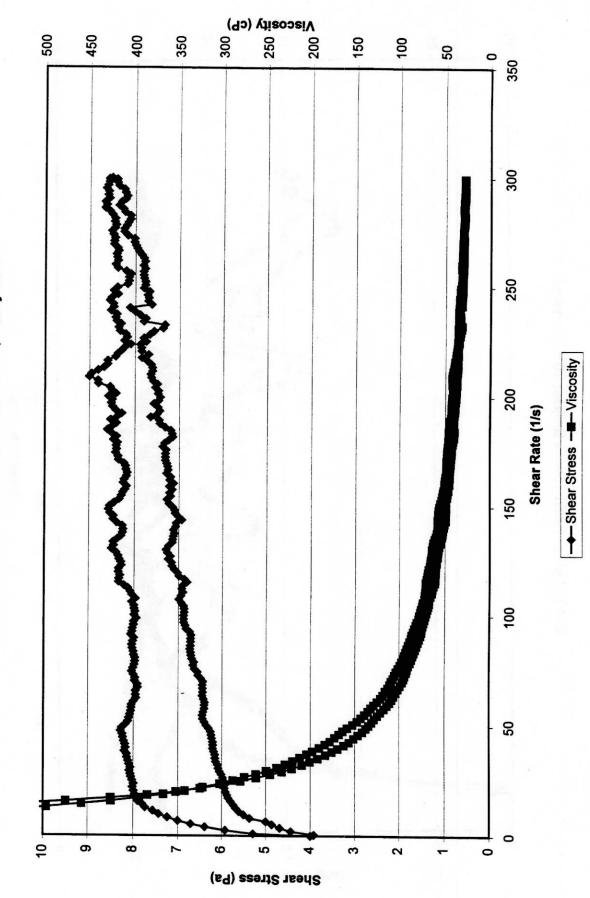
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

C-104 Melter Feed 15wt% Solids: 50°C, Analysis 2



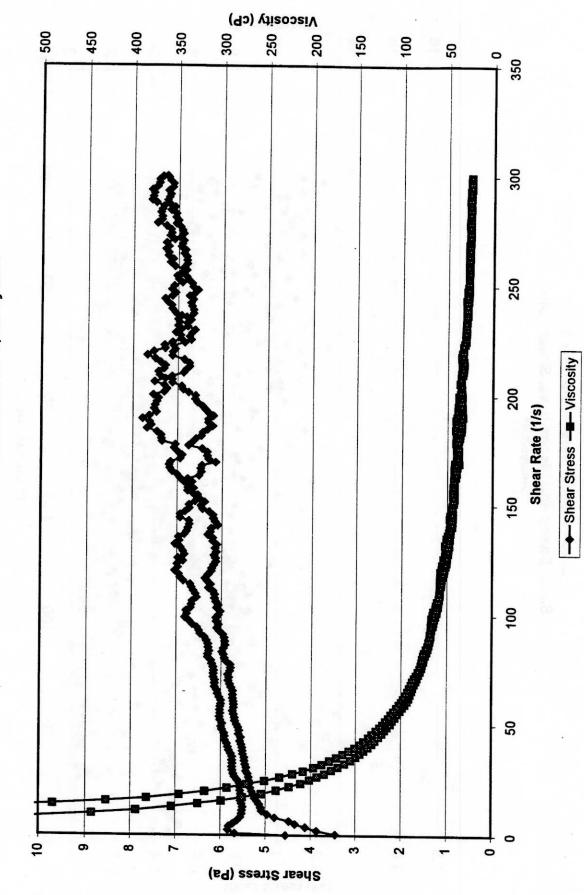
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

C-104 Melter Feed 25wt% Solids: 50°C, Analysis 1



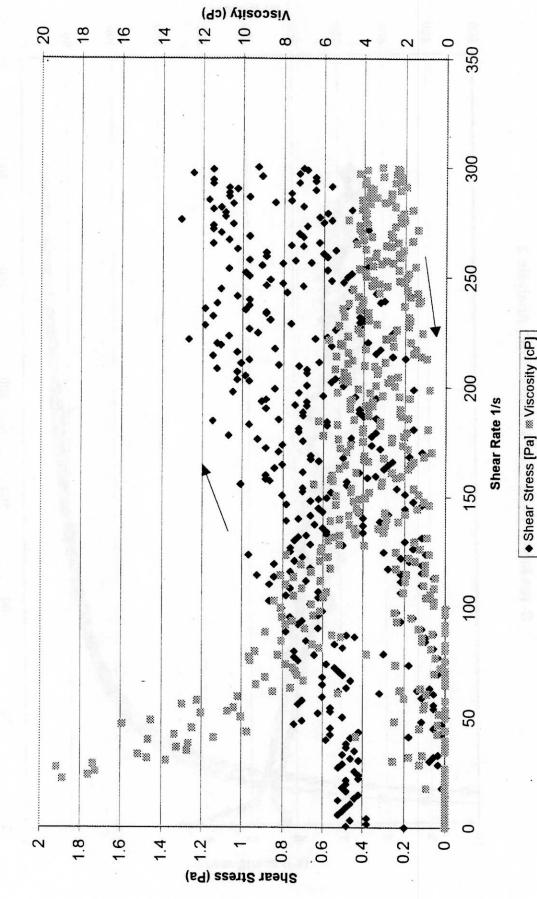
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

C-104 Melter Feed 25wt% Solids: 50°C, Analysis 2



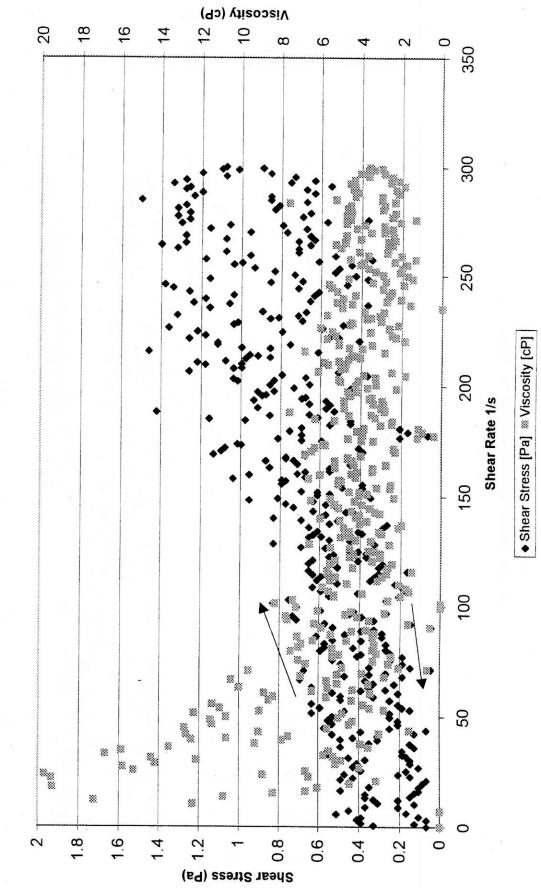
Analysis using M5 viscometer modified for hot cell operations: SV1 measuring geometry

C-104 w/secondary waste- 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



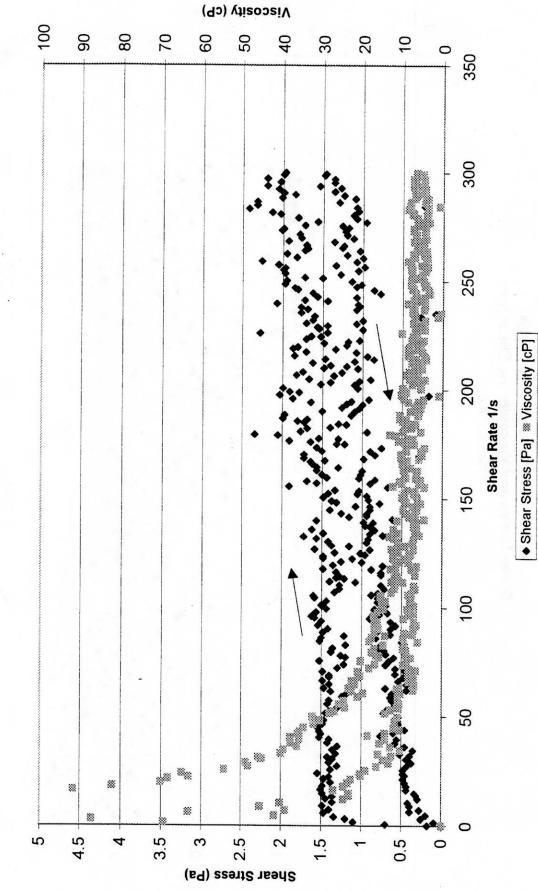
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



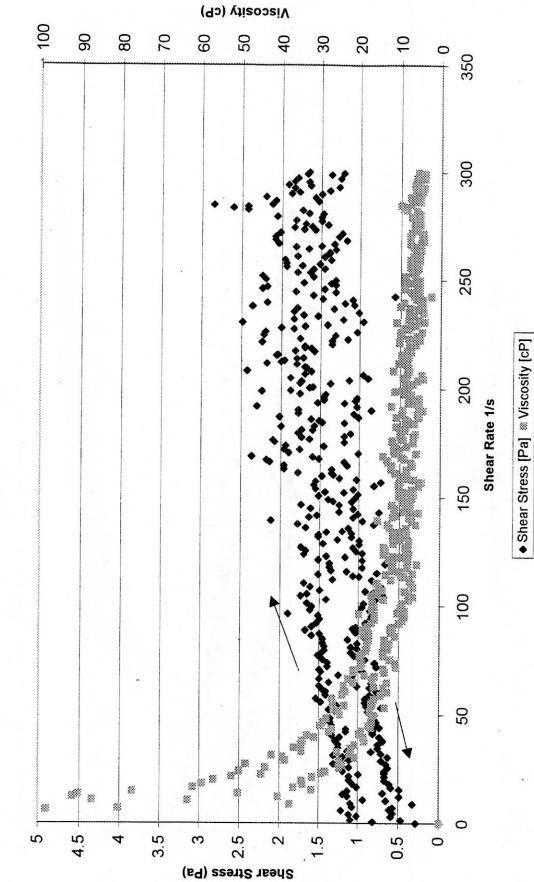
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



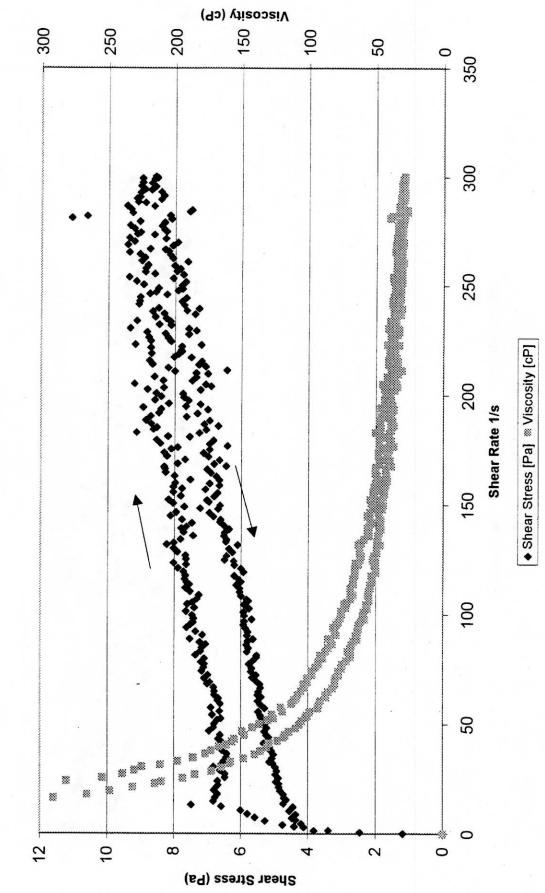
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



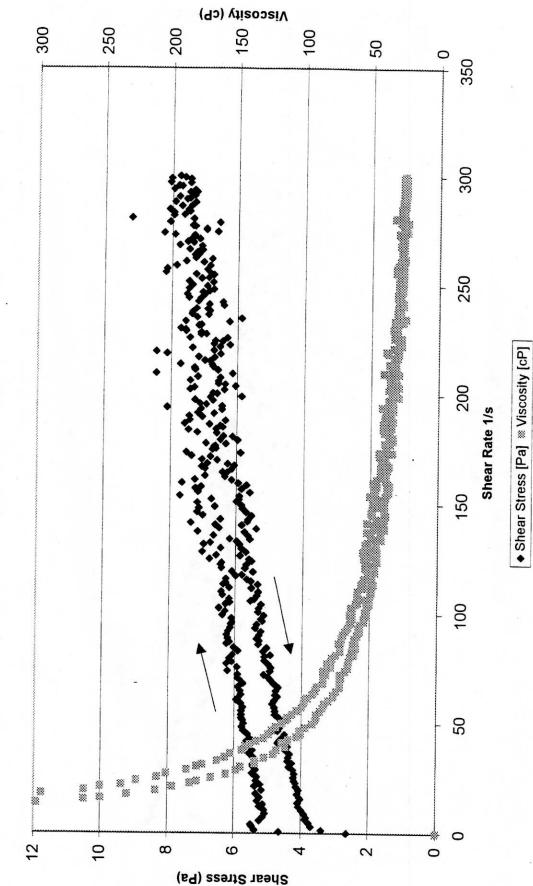
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



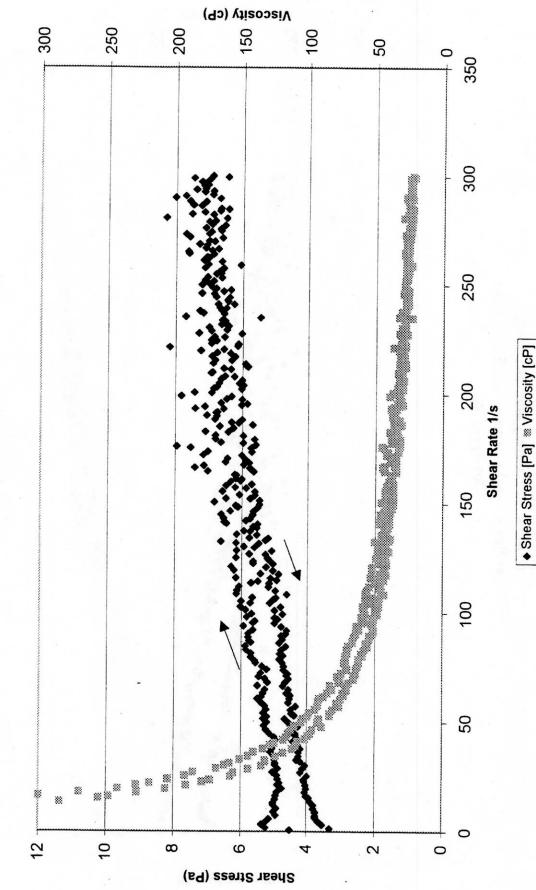
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



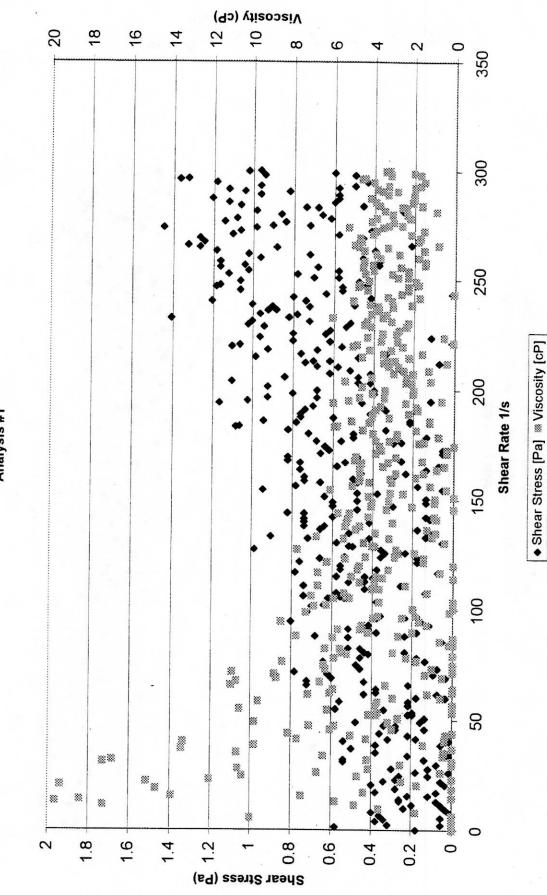
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #3



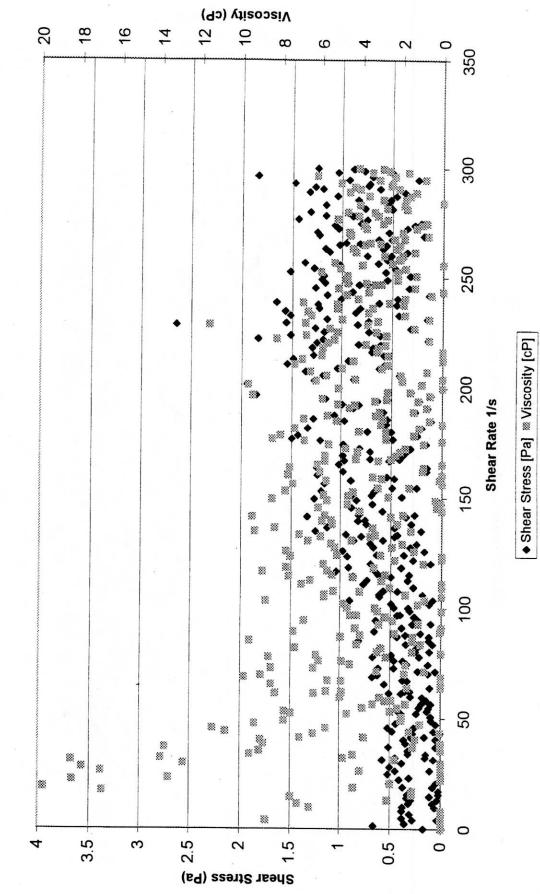
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 5wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #1



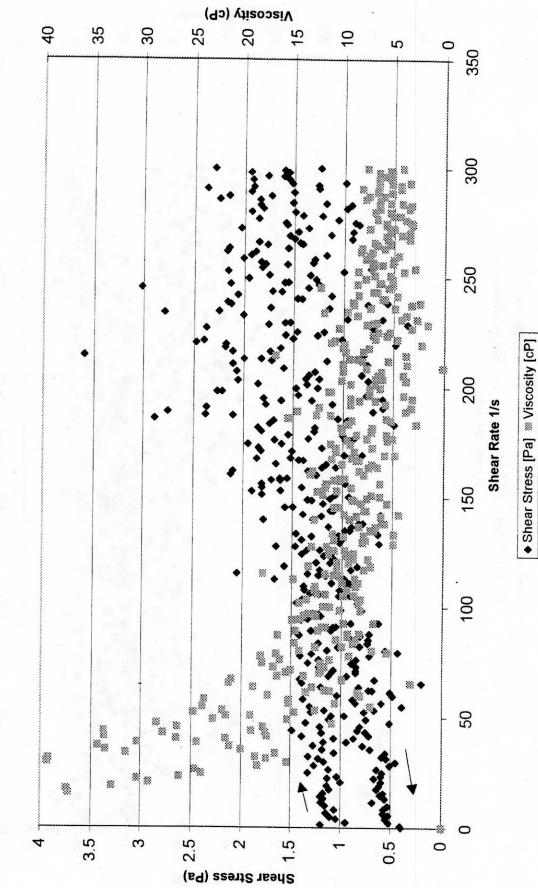
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 5wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #2



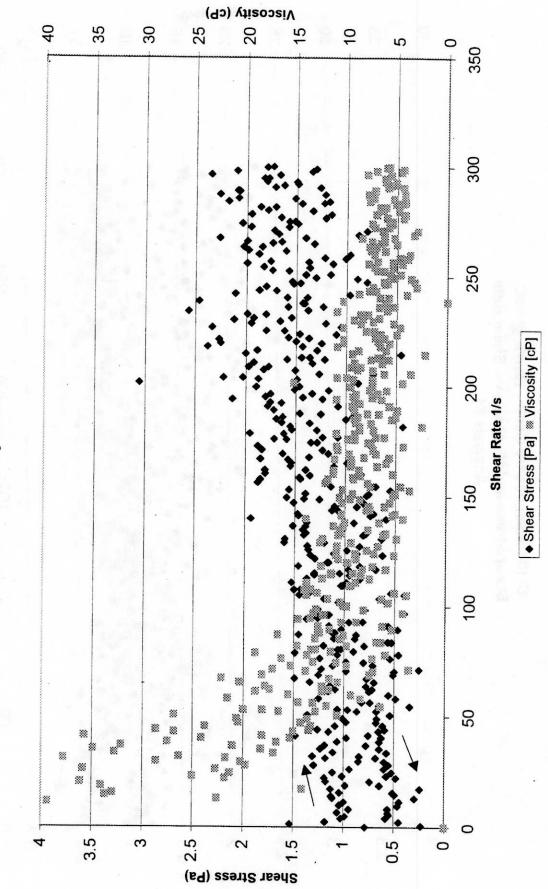
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 15wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #1

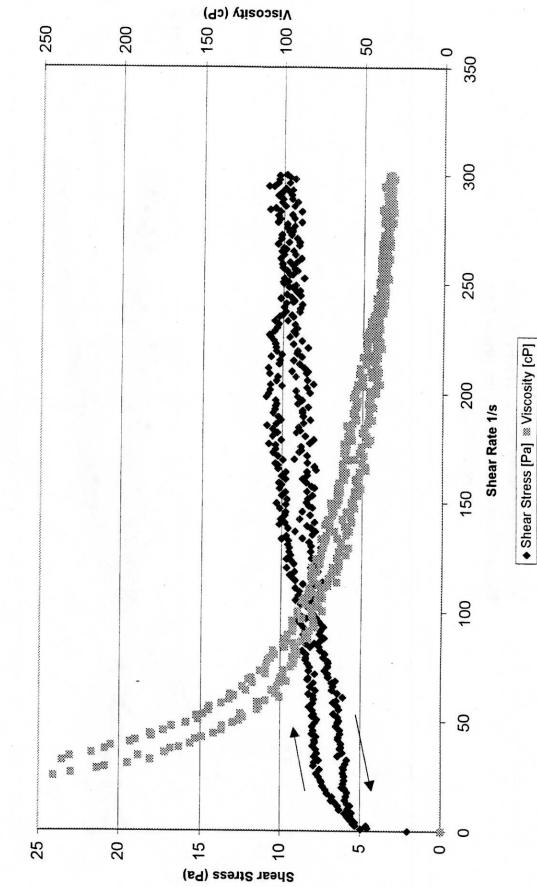


Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 15wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #2

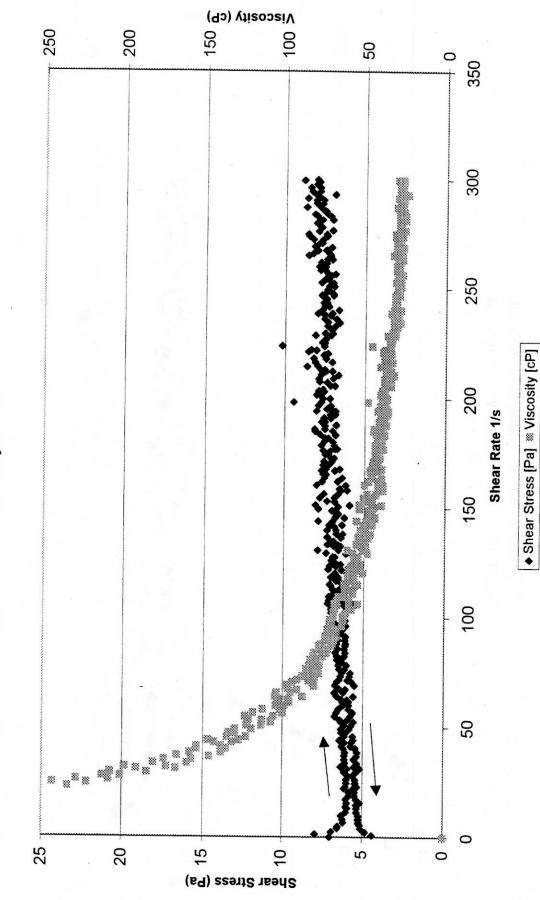


C-104 w/secondary waste- 25wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #1



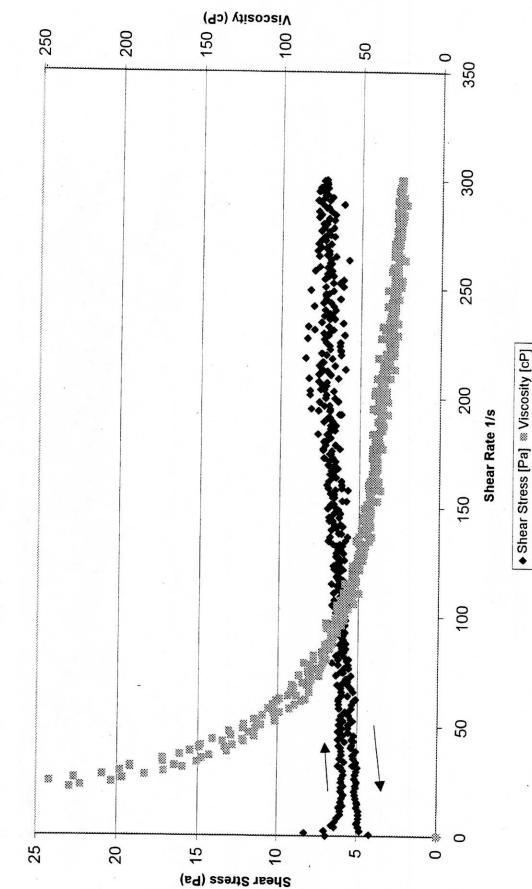
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 25wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #2



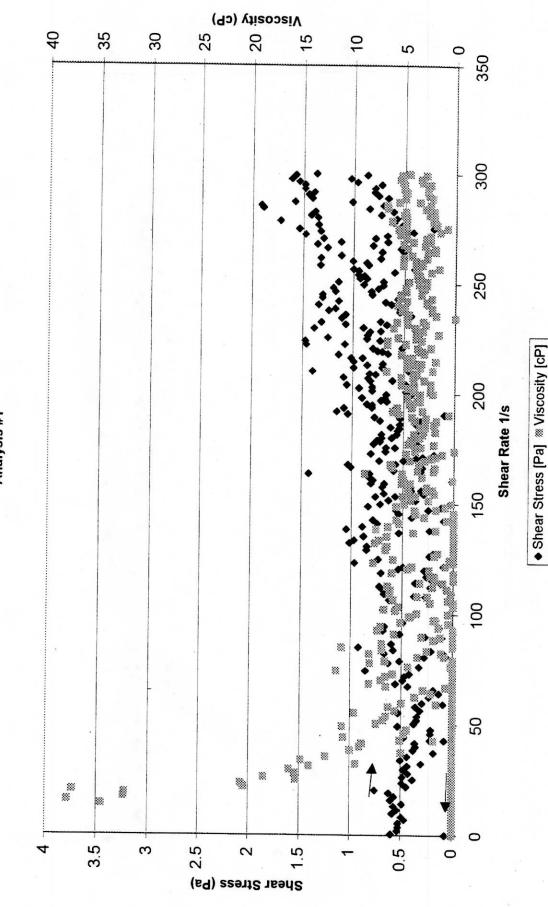
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste- 25wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #3



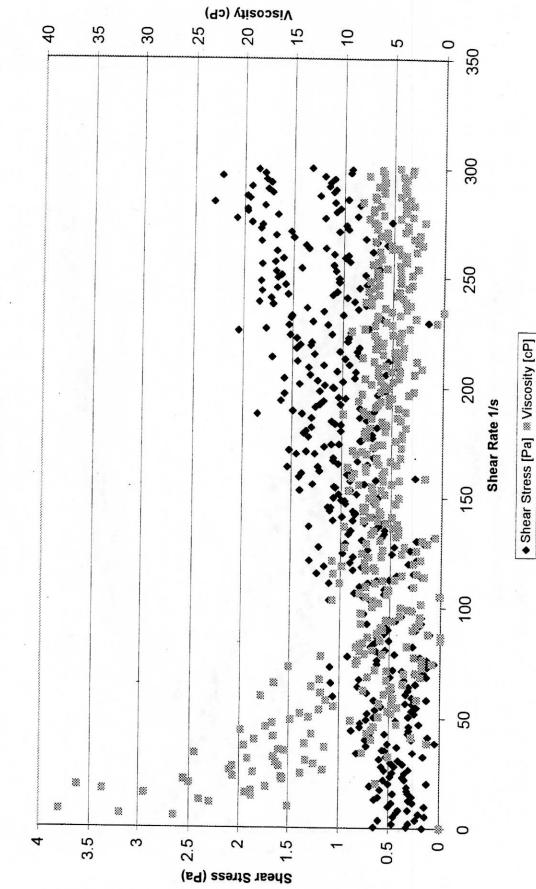
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



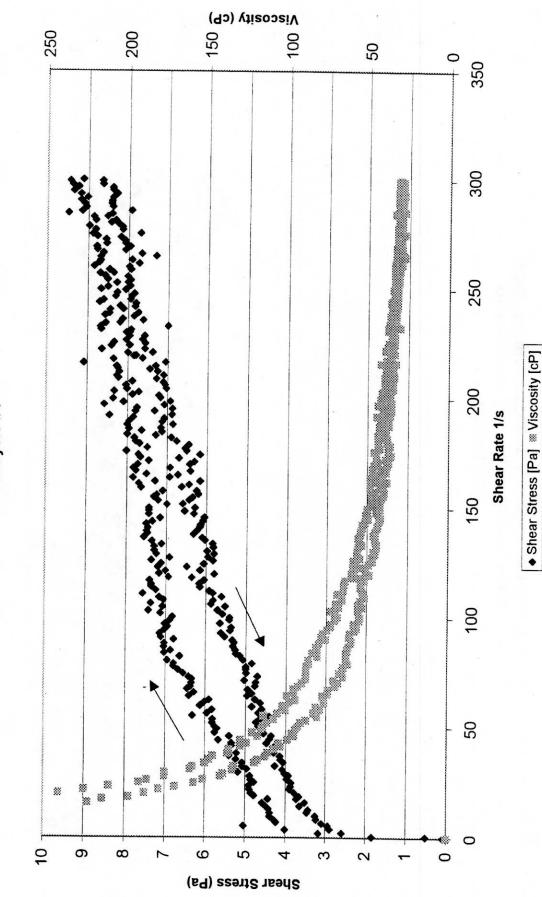
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 5wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



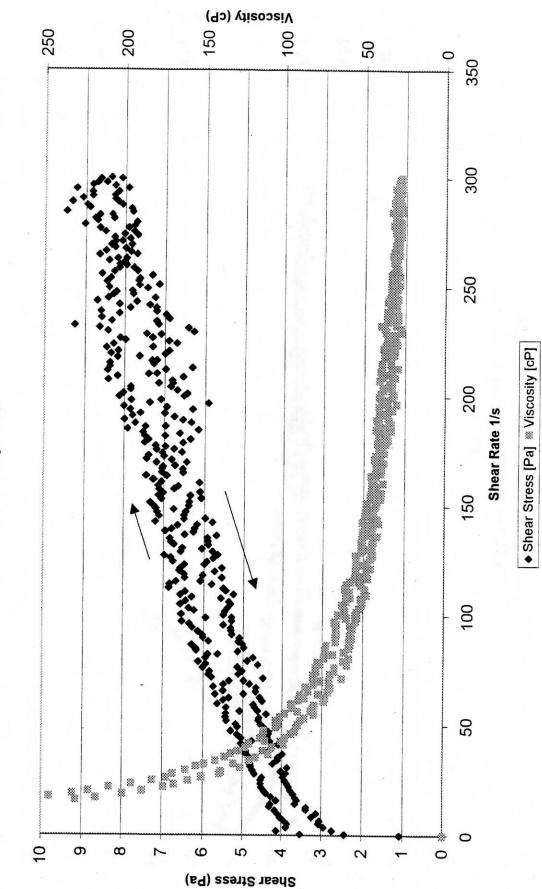
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



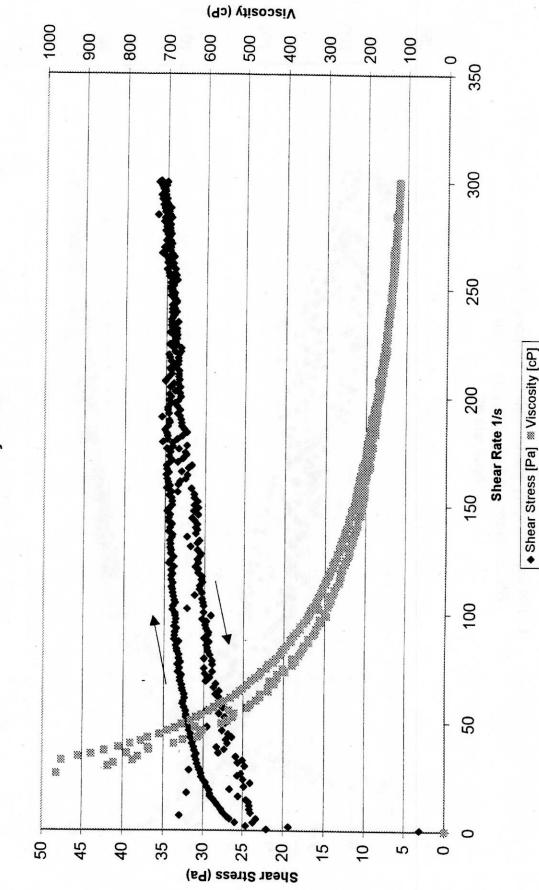
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 15wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



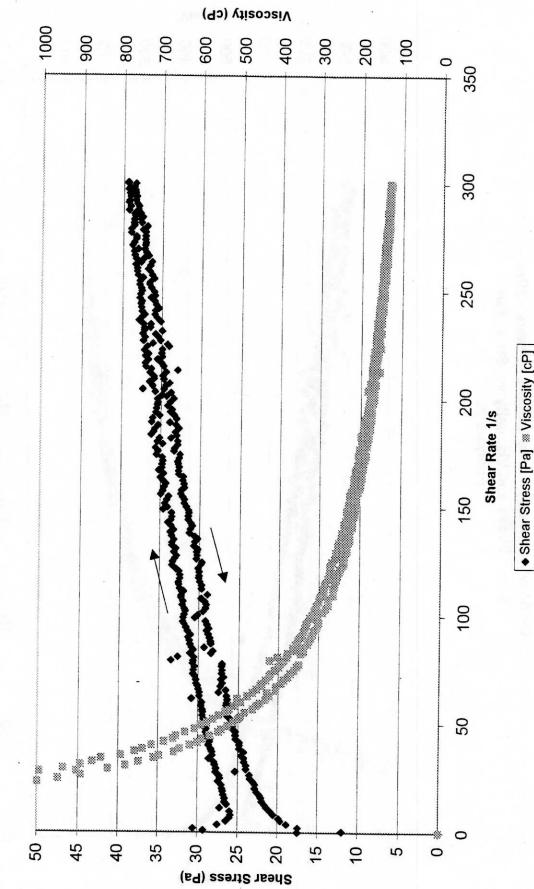
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #1



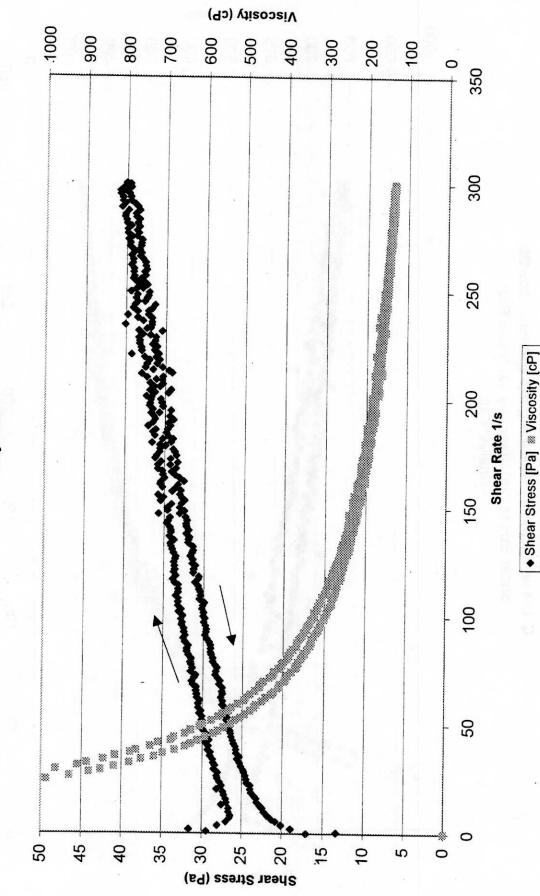
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #2



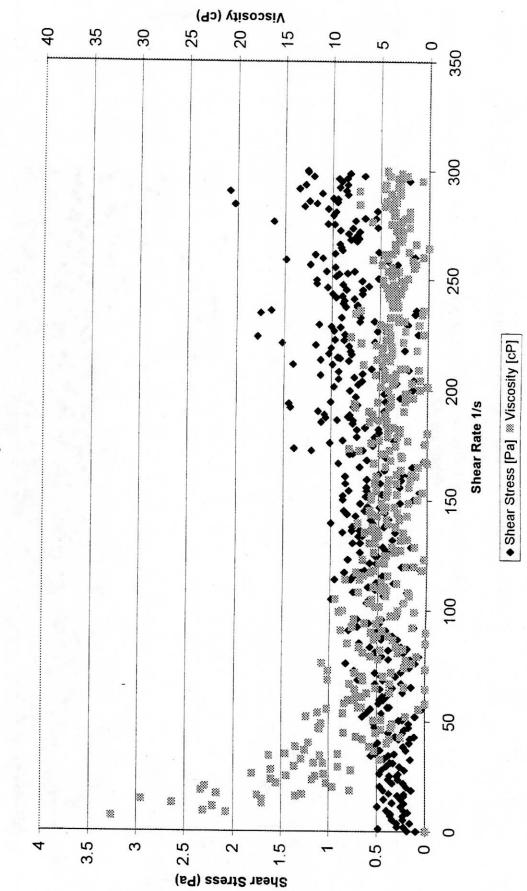
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 25wt% Shear Stress and Viscosity vs. Shear Rate Analysis #3



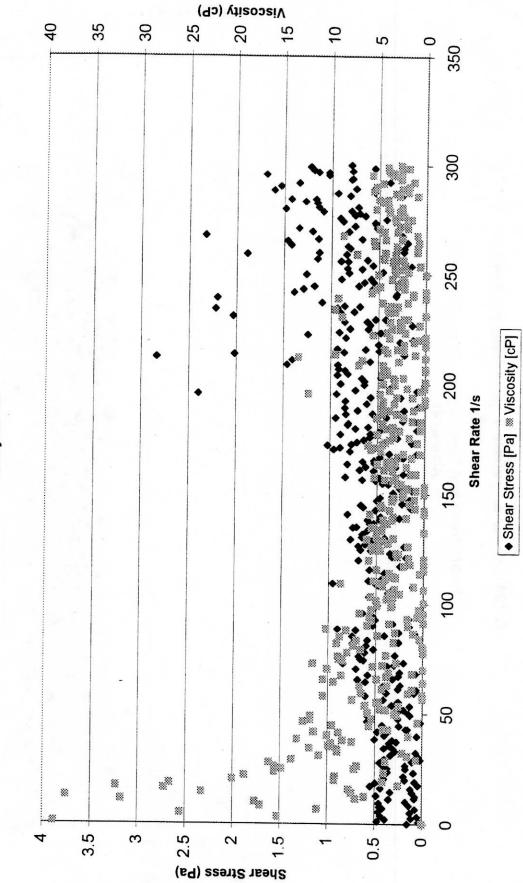
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 5wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #1



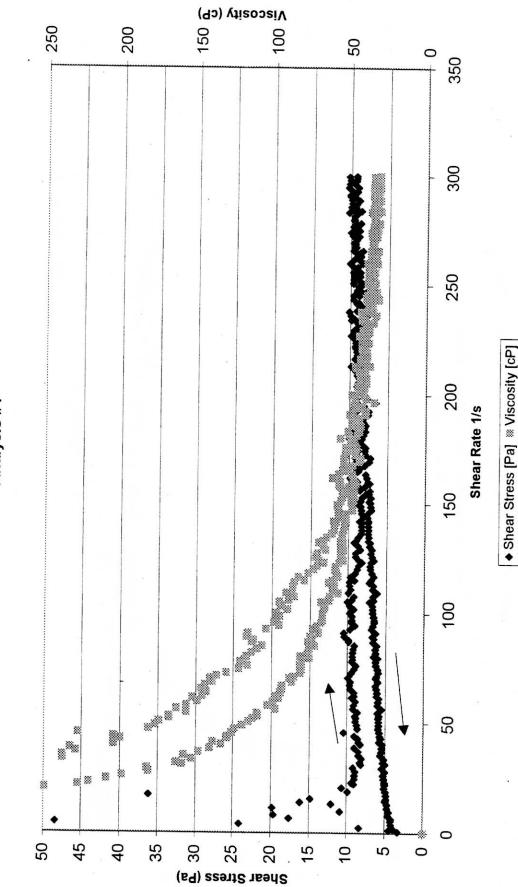
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 5wt% @ 50C Shear Stress and Viscosity vs. Shear Rate Analysis #2



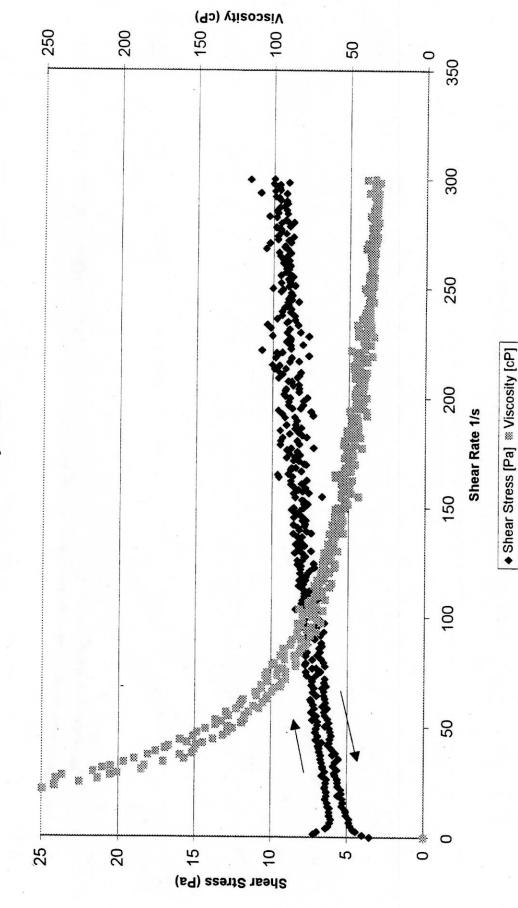
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 15wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #1



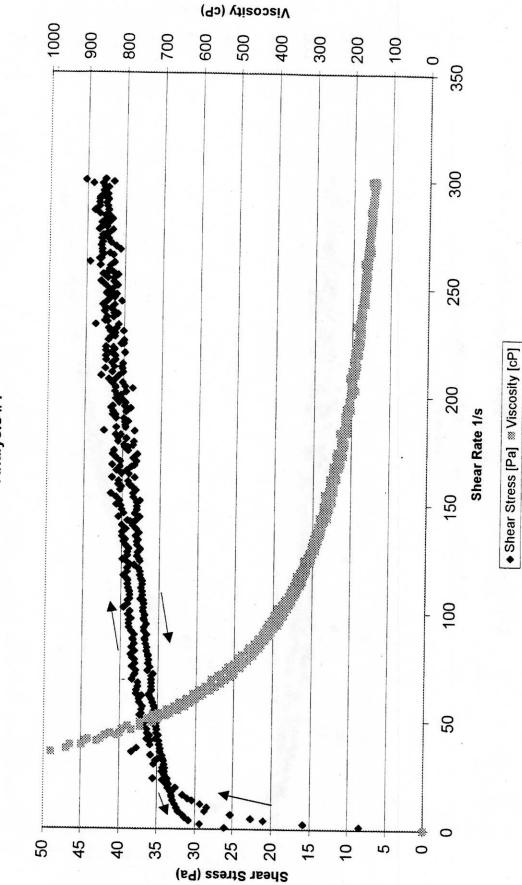
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 15wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #2



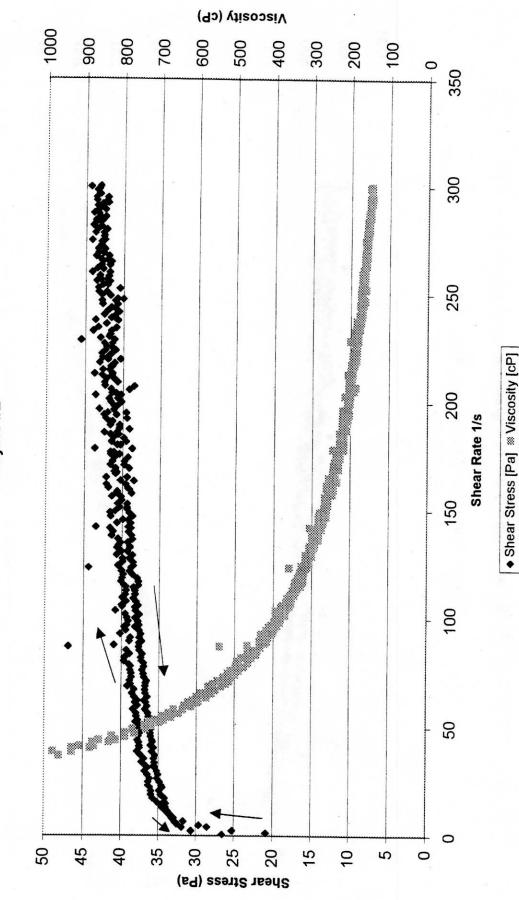
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 25wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #1



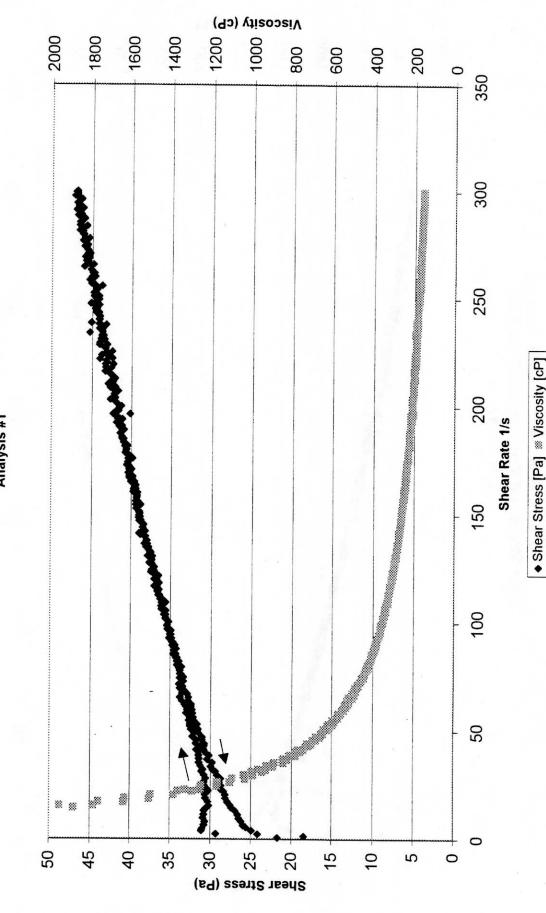
Measurement performed with a Haake M5 and SV I sensor

C-104 w/secondary waste & glass formers - 25wt%
@ 50C
Shear Stress and Viscosity vs. Shear Rate
Analysis #2



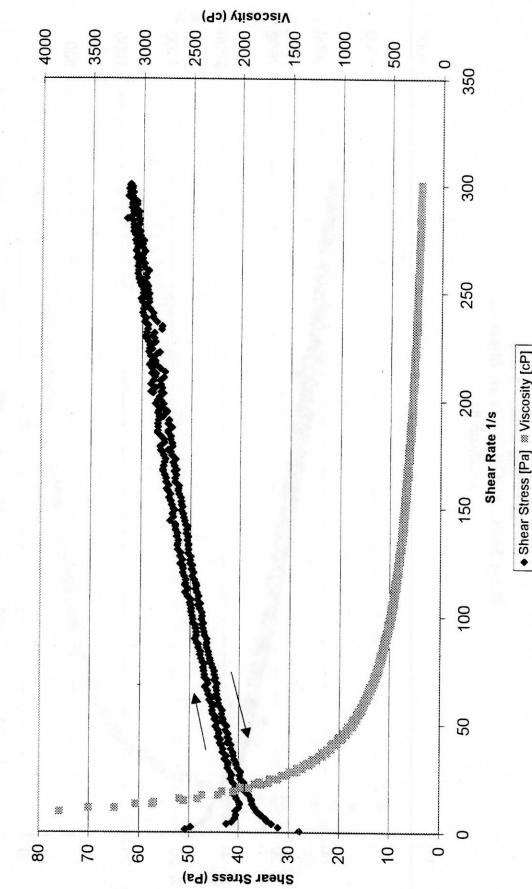
Measurement performed with a Haake M5 and SV I sensor

C-104 Mixing Study - 1 Hour Shear Stress and Viscosity vs. Shear Rate Analysis #1



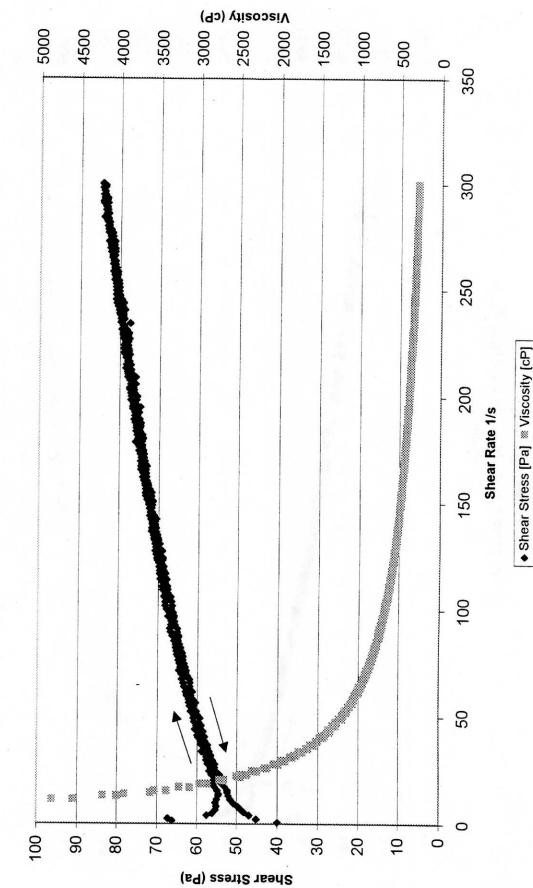
Measurement performed with a Haake M5 and SV I sensor

C-104 Mixing Study - 1 Day Shear Stress and Viscosity vs. Shear Rate Analysis #1



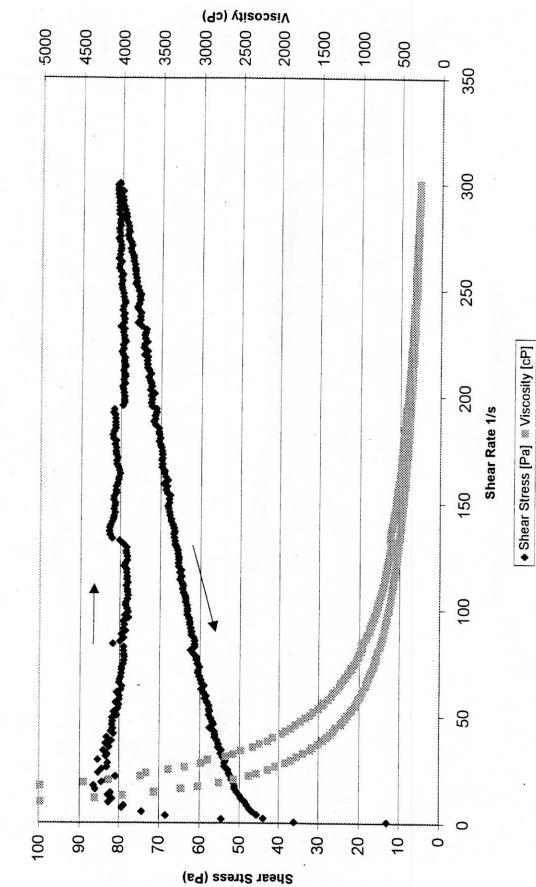
Measurement performed with a Haake M5 and SV I sensor

C-104 Mixing Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #1



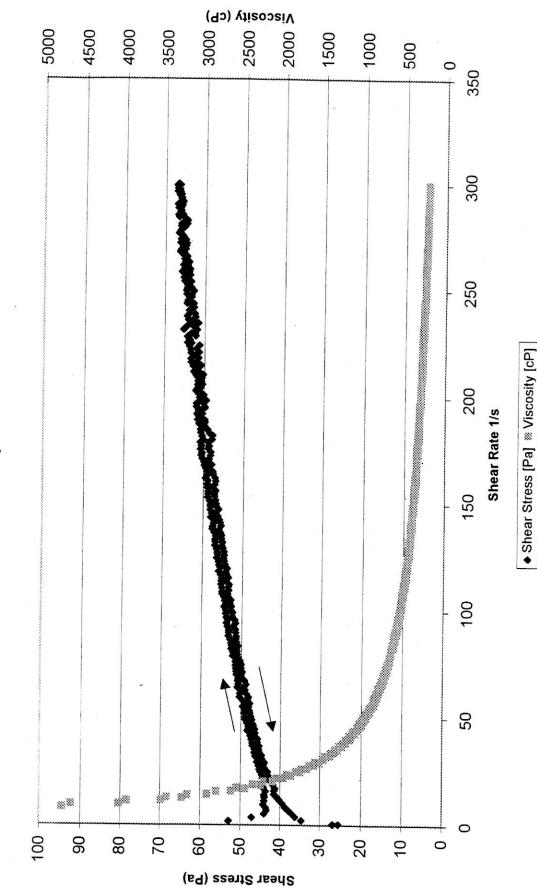
Measurement performed with a Haake M5 and SV I sensor

C-104 Aging Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #1



Measurement performed with a Haake M5 and SV I sensor

C-104 Aging Study - 1 Week Shear Stress and Viscosity vs. Shear Rate Analysis #3



Measurement performed with a Haake M5 and SV I sensor

Viscosity III CF	C-104 Feed	25 C		25.52	25 C	C-104 Feed		50 C	50 C	50 C	50 C
File Name	Material	33 1/s	150 1/s	298 1/s	Other?	File Name	Material	S	150 1/s	298 1/s	Other?
050800B up (0-300 1/s)	C-104 5 wt% Feed	14.6	10.0	6.8		050800H up (0-300 1/s)	C-104 5 wt% Feed	4.6	5.2	5.0	
050800B down (300-0 1/s)	C-104 5 wt% Feed	5.9	2.8	. 5.8		050800H down (300-0 1/s)	C-104 5 wt% Feed	4.0	5.2	2.9	
050800C up (0-300 1/s)	C-104 5 wt% Feed - R	15.7	5.1	4.0		0508001 up (0-300 1/s)	C-104 5 wt% Feed - R	6.4	5.3	2.4	
050800C down (300-0 1/s)	C-104 5 wt% Feed - R	3.2	2.9	2.1		0508001 down (300-0 1/s)	C-104 5 wt% Feed - R	0.4	0.8	2.4	
Average all		9.8	5.2	4.7		Average all		3.8	4.1	3.2	
Average without 1st up curve		8.3	3.6	4.0		Average without 1st up curve		3.6	3.8	2.6	
050800D up (0-300 1/s)	C-104 15 wt% Feed	23.28	5.73	6.37		050800J up (0-300 1/s)	C-104 15 wt% Feed	14.5	3.7	5.0	8
050800D down (300-0 1/s)	C-104 15 wt% Feed	10.33	5.705	5.347		050800J down (300-0 1/s)	C-104 15 wt% Feed			3.9	
050800E up (0-300 1/s)	C-104 15 wt% Feed - R	19.51	7.68	6.35		050800K up (0-300 1/s)	C-104 15 wt% Feed - R	16.5	6.6	6.2	
050800E down (300-0 1/s)	C-104 15 wt% Feed - R	8.358	5.54	4.87		050800K down (300-0 1/s)	C-104 15 wt% Feed - R	12.8	5.9	4.4	
Average all		15.4	6.2	5.7		Average all		14.6	5.4	4.9	
Average without 1st up curve		12.7	6.3	5.5		Average without 1st up curve		14.6	6.3	4.8	
050800F up (0-300 1/s)	C-104 25 wt% Feed	188.4	48.92	27.04		050800L up (0-300 1/s)	C-104 25 wt% Feed	245.1	57.8	28.9	
050800F down (300-0 1/s)	C-104 25 wt% Feed	160	44.62	26.06		050800L down (300-0 1/s)	C-104 25 wt% Feed	188.7	47.7	27.8	
050800G up (0-300 1/s)	C-104 25 wt% Feed - R	165.6	45.71	25.62		050800M up (0-300 1/s)	C-104 25 wt% Feed - R	173.8	47.9	25.2	
050800G down (300-0 1/s)	C-104 25 wt% Feed - R	145.6	42.8	24.9		050800M down (300-0 1/s)	C-104 25 wt% Feed - R	167.6	43.4	25.1	
Average all		164.9	45.5	25.9		Average all		193.8	49.2	26.7	
Average without 1st up curve		157.1	44.4	25.5		Average without 1st up curve	77	176.7	46.3	26.0	
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Viscosity in cP	Secondary Glass Formers		25 C	25 C	25 C			50 C	50 C	50 C	50 C
rile Name	Material	33 1/s	150 1/s		Other?	File Name	Material	33 1/s	150 1/s	298 1/s	Other?
062200A up (0-300 1/s)	C-104 5 wt% Feed	10.0	4.7	5.4		062300B up (0-300 1/s)	C-104 5 wt% Feed	13.2	4.9	1.4	
062200A down (300-0 1/s)	C-104 5 wt% Feed	0.0	0.5	2.6		062300B down (300-0 1/s)	C-104 5 wt% Feed	8.0	1.0	2.4	
062200B up (0-300 1/s)	C-104 5 wt% Feed - R	18.3	7.2	6.1		062300C up (0-300 1/s)	C-104 5 wt% Feed - R	9.1	2.1	4.0	
062200B down (300-0 1/s)	C-104 5 wt% Feed - R	4.6	4.3	2.7		062300C down (300-0 1/s)	C-104 5 wt% Feed - R	5.8	0.3	2.0	
Average all		8.2	4.2	4.2		Average all		9.0	2.0	3.1	
Average without 1st up curve		7.6	4.0	3.8		Average without 1st up curve		7.6	1.1	2.8	
062200C up (0-300 1/s)	C-104 15 wt% Feed	154.7	49.5	31.5		062300D up (0-300 1/s)	C-104 15 wt% Feed	248.5	57.6	e	
062200C down (300-0 1/s)	C-104 15 wt% Feed	125.9	42.01	28.4		062300Ddown (300-0 1/s)	C-104 15 wt% Feed	155.3	47.1	31.4	
062200D up (0-300 1/s)	C-104 15 wt% Feed - R	145.7	48.3	29.2		062300E up (0-300 1/s)	C-104 15 wt% Feed - R	200.1	51.5	34.3	
062200D down (300-0 1/s)	C-104 15 wt% Feed - R	126.7	42.6	27.65		062300E down (300-0 1/s)	C-104 15 wt% Feed - R	177.5	55.6	30.5	
Average all		138.3	45.6	29.2		Average all		195.4	53.0	32.6	
Average without 1st up curve		132.8	44.3	28.4		Average without 1st up curve		177.6	51.4	32.1	
062200F up (0-300 1/s)	C-104 25 wt% Feed	761.1	208.8	120		062300G up (0-300 1/s)	C-104 25 wt% Feed	1064	272.6	-	
062200F down (300-0 1/s)	C-104 25 wt% Feed	938.6	227.2	117		062300G down (300-0 1/s)	C-104 25 wt% Feed	1041	254.4		
062200H up (0-300 1/s)	C-104 25 wt% Feed - R	869.4	230.4	135.5		062300J up (0-300 1/s)	C-104 25 wt% Feed - R	1121.0	271.4	145.6	
062200H down (300-0 1/s)	C-104 25 wt% Feed - R	771.7	220.4	132		062300J down (300-0 1/s)	1 .	1077.0	262.0	146.0	
Average all		835.2	221.7	126.1		Average all		1075.8	265.1	146.0	
Average without 1st up curve		859.9	226.0	128.2		Average without 1st up curve		1079.7	262.6	145.2	
BARTA WAR II -									T		
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Average Viscosity Data

Viscosity in cr	AZ-102 Feed	25 C	25 C	25 C	25 C			50 C	50 C	50 C	50 C
rie Narie	Material	33 1/5	150 1/s	298 1/s	Other?	File Name	Material	33 1/s	150 1/s	ls/	Other?
051200A up (0-300 1/s)	AZ-102 5 wt% Feed	13.4	0.9	5.3		051200H up (0-300 1/s)	AZ-102 5 wt% Feed	18.7	5.2	8.4	
051200A down (300-0 1/s)	AZ-102 5 wt% Feed	8.0	2.5	4.4		051200H down (300-0 1/s)	AZ-102 5 wt% Feed	5.1			
051200B up (0-300 1/s)	AZ-102 5 wt% Feed - R	15.7	8.5	5.7		0512001 up (0-300 1/s)	AZ-102 5 wt% Feed - R	12.4	4.7		
051200B down (300-0 1/s)	AZ-102 5 wt% Feed - R	11.3	5.9	5.2		051200l down (300-0 1/s)	AZ-102 5 wt% Feed - R	10.7			
Average all		12.1	5.7	5.2		Average all		11.7	4.7		
Average without 1st up curve		11.7	5.6	5.1		Average without 1st up curve		9.6			
051200C up (0-300 1/s)	AZ-102 15 wt% Feed	527.9	153.1	79.1		051200J up (0-300 1/s)	AZ-102 15 wt% Feed	529.1	15	8	
051200C down (300-0 1/s)	AZ-102 15 wt% Feed	537.9	142.7	78.5		051200J down (300-0 1/s)	AZ-102 15 wt% Feed	626.3			
051200D up (0-300 1/s)	AZ-102 15 wt% Feed - R	517.1	141.3	78.99		051200K up (0-300 1/s)	AZ-102 15 wt% Feed - R	523.1			
051200D down (300-0 1/s)	AZ-102 15 wt% Feed - R	517.7	139.1	78.36		051200K down (300-0 1/s)	AZ-102 15 wt% Feed - R	546.1	143.6		
Average all	-	525.2	144.1	78.7		Average all	ı	556.2			
Average without 1st up curve		524.2	141.0	78.6		Average without 1st up curve		565 2			
060800C up (0-300 1/s)	AZ-102 20 wt% Feed	917.1	234.6	129.8							
060800C down (300-0 1/s)	AZ-102 20 wt% Feed	890.5	231.5	127.4							
060800D up (0-300 1/s)	AZ-102 20 wt% Feed - R										
060800D down (300-0 1/s)	AZ-102 20 wt% Feed - R										
Average all		903.8	233.1	128.6							
Average without 1st up curve		890.5	231.5	127.4							
051200E up (0-300 1/s)	AZ-102 25 wt% Feed	6220	1493	802.5		22.480					
051200E down (300-0 1/s)	AZ-102 25 wt% Feed	5281	1446	799							
051200F up (0-300 1/s)	AZ-102 25 wt% Feed - R	4047	1167	656.7							
051200F down (300-0 1/s)	AZ-102 25 wt% Feed - R	4002	1162	655.1							
051200G up (0-300 1/s)	AZ-102 25 wt% Feed - R	4017	1157	651.5							
051200G down (300-0 1/s)	AZ-102 25 wt% Feed - R	4016	1156	650.7							
Average all		4597.2	1263.5	702.6							
Average without 1st up curve		4272.6	1217.6	682.6		Average without 1st up curve		#DIV/0i	#DIV/0i	#DIV/0i	
				18							
										-	

Average Viscosity Data

Viscosity in cP	AZ-102 Mixing and Aging	25 C	25 C	25 C	25.0	
File Name	Material		150 1/s	s/	Other?	
061900A up (0-300 1/s)	AZ-102 1hr	275.9	89.6	53.0		
061900A down (300-0 1/s)	AZ-102 1hr	247.1	81.2	50.9		
061900B up (0-300 1/s)	AZ-102 5 1hr - R	254.8	77.5	48.1		
061900B down (300-0 1/s)	AZ-102 1hr - R	232.3	72.7	46.1		
Average all		252.5	80.3	49.5		
Average without 1st up curve		244.7	77.2	48.3		
062000A up (0-300 1/s)	AZ-102 ~24 hr	143.9	45.5	29.11		
062000A down (300-0 1/s)	AZ-102 ~24 hr	113.2	43.3	26.3		
062000B up (0-300 1/s)	AZ-102 ~24 hr - R	119.8	40.1	26.9		
062000B down (300-0 1/s)	AZ-102 ~24 hr - R	116.9	37	26.1		
Average all		123.5	41.5	27.1		
Average without 1st up curve		116.6	40.1	26.4		
062600A up (0-300 1/s)	AZ-102 ~ 1 week	80.59	23.6	16.94		
062600A down (300-0 1/s)	AZ-102 ~ 1 week	47.8	19.7	14.66		
062600B up (0-300 1/s)	AZ-102 ~ 1 week - R	66.29	24.29	16.65		
062600B down (300-0 1/s)	AZ-102 ~ 1 week - R	51.96	18.7	14.81	**	
Average all		61.7	21.6	15.8		
Average without 1st up curve		55.4	20.9	15.4		
072800A up (0-300 1/s)	AZ-102 Aged ~ 1 week	457	120.3	64.7		
072800A down (300-0 1/s)	AZ-102 Aged ~ 1 week	232	86.44	62.8		
072800B up (0-300 1/s)	AZ-102 Aged ~ 1 week - R	274.1	94.7	6.73		
072800B down (300-0 1/s)	AZ-102 Aged ~ 1 week - R	227.2	84.3	58.5		
072800C up (0-300 1/s)	AZ-102 Aged ~ 1 week - R	246.3	85.4	54.4		
072800C down (300-0 1/s)	AZ-102 Aged ~ 1 week - R	222.8	81.8	54		
Average all		276.6	92.2	58.7		
Average without 1st up curve		240.5	86.5	57.5		

APPENDIX C

Appendix C: Test Instruction

PNNL Test Instruction	Document No.: BNFL-TI-29953-082 Rev. No.: 0
Title: Preparation of simulated Sr/TRU Removal Solids fo	r Rheology Testing
Work Location: PSL, 1425	Page 1 of 9
Author: Richard T. Hallen	Effective Date: 3/1/00 Supercedes Date: New
Use Category Identification: Information	nered primary and difference of The selle
Identified Hazards: Radiologicalx Hazardous Materials Physical Hazards Hazardous Environment Other:	Required Reviewers: X Technical Reviewer
Are One-Time Modifications Allowed to this Test Ins NOTE: If Yes, then modifications are not anticipated to impa SBMS or the controlling Project QA Plan as appropriate.	truction? X Yes No No ct safety. For documentation requirements of a modification see
On-The Job Training Required?Yes orX_No FOR REVISIONS: Is retraining to this procedure required?YesX_No Does the OJT package associated with this procedure require reYesNoX_N/A	vision to reflect procedure changes?
Author Signature Author Signature Technical Reviewer D & Kurath	Date 3/2/08 3/2/08

Controlled Document

5.0 Test Instructions for Solids Preparation from Permanganate Treatment

The laboratory record book (LRB) shall be used to record other testing information as required by this procedure and all test conditions not stated by this procedure.

5.1 Pre-start for Scoping Studies

proceeding.

- 5.1.1 Inventory materials, equipment, supplies, and reagents to ensure all required items are available.
- 5.1.2 Do the following and initial and date when each item is completed.

 Review the work instructions in this test instruction before beginning. Any questions should be addressed to Dean Kurath or Rich Hallen. And questions need to be answered before

5.1.3 Obtain the following information:

M&TE List:	
Balance 1:	
Calib ID	380-06-01-006 Calib Exp Date 2/01
Cocation Location	PSL 1425
Balance 2:	380-86-81-013
Calib ID	Calib Exp Date 2/0/
Location	PSC 1425
Thermocouple:	
Calib ID	Calib Exp Date
Location	Thermocouple type
Digital Thermometer:	
Calib ID	Calib Exp Date
Location	
ASTM 90C 23.8	°C = 23 °C ERTO RZZYI
Kessler 811-066	

5.2 Permanganate Treatment of AN-107

5.2.1 Turn on stirrer.

5.2.2 While continuously stirring the waste add the metal salts to the simulant.	The may not
dissolve or may dissolve and precipitate but this is expected.	J 110 t

Fe(NO3)3 Target amount 56 8 Actual amount 568398 grams grams Ca(NO3)2 Target amount 700 grams 7.8% Actual amount 2.9032 grams Cr(NO3)3 Target amount 2.80 grams 1.85 Actual amount 1.8319 grams Pb(NO3)2 Target amount 12 7.77 grams Actual amount 0.784 4 grams MnClz·9HD 5.2.3 Collect a single 10 mL sample for analysis via ICP. 10:10 Am dupticed SM-01 + SM-02 collected 5.2.4 While continuously stirring the waste sample, personnel are to slowly add 599.97mL of 1.0 M Sr(NO₃)₂ solution. (based upon BNF-003-98-0023, add 1M Sr at a rate of 2 to 20 mL/min/L of waste, target 10 mL/min/L of waste or 70 mL/min) 10:20 addition 5 touted healer Tare bottle of 1M Sr \347.52 9 10:30 completed Tare Empty bottle Weight Added 5.2.5 While continuously stirring the waste sample, personnel are to slowly add 399.98 mL of 1 M NaMnO₄ solution. (based upon BNF-003-98-0023, add 1 M NaMnO4 at a rate of 2 to 20 mL/min/L of waste, target 10mL/min/L of waste or 70 mL/min) bedser

10:35 additeristated Tare bottle of 1M NaMnO4 976.229

Tare Empty bottle 415,20 9

Weight Added Weight Added

5.2.6 Heat the waste mixture at $50 \pm 5^{\circ}$ C with stirring for 4 hours after completing the addition 11:17 - both hot plates turned on -third not plate added of the NaMnO4.

5.2.7 Turn off the stirrer and allow the waste to cool to $25 \pm 5^{\circ}$ C. 11:43 t= 380c

5.3 Solids Removal with the Deadend Filter Unit

5.3.1 Fare the filter assembly/filter media. Not done Tare of the filter assembly

glasswool dankefadded to Keepin hove heat 12:10 - t= 45°C 12:32 t= 50°C not plates to Low.

13:58: += 49°C 5.3.3 Assemble a large filtration unit and filter all of treated waste in the treated simulant. The solids should have settled on cooling/setting. Decant all of the supernate from the treated waste to the filter. The supernate should filter faster without all of the solids/cake on the filter unit.

et 3:10/15:10 -100 nL 5 (urry sampled

16:10 44°C 15:02 t=48°C 16:45 stirer 15:39 t=46°C t=49°C 14:25 16:00 heat-hot platesternedoff

Collect duplicate samples of the damp sludge for analysis by ICP and IC. A single simulant sample should be collected after the shim chemicals are added for analysis by ICP.

Final supernature density

25 mL = 30.9474 grams

d = 1.2379 g/m L

Wt % solids

Jun #1 365.4644

Jun #2 18.2687 17.2481 19.2363 19.2387 3.7262 8.968 s

Tor#2 26.60 wt % solids

Junt 2 26.00 wt % solids

Junt 2 26.00 wt % solids

- NOT SUPPISING THAT # 1 is a little wetter, they were placed in Jac + Sealed Sooner. Jan #2 was less solids + after some periods of time - sooner. Jan #2 was less solids + after some periods of time - probably 10 minutes between souling of the two bootles/Jans.

probably 10 minutes between souling of the two bootles/Jans.

Word tract to M. World have expected 21/6/00

This

Formula Ca(NO3)2.4H2O Cr(NO3)3.9H2O Fe(NO3)3.9H2O Pb(NO3)2 MnCl2.4H2O Treatment of AN-10 per liter of waste	grams 236.15 400.15 404 331.2 197.9 07 simulant	ug/g 50 25 800 50 200	mg/L 63.55 31.775 1016.8 63.55 254.2	mmol/L 1.585579 0.611105 18.20689 0.306708 4.627034	g/L 0.374434 0.244534 7.355582 0.101582 0.91569		
	1M Sr 1M MnO4	0.0857 0.0571				2 moles 8 moles	
		Balance r Calibratio	number: n date:		<u> </u>		
Makeup Sr(NO3)2 use Sr(NO3)2 211.63 grams/mo Tare Bottle/flas add 36.278 g for each liter treated	grams Sr(NC	(lot # 03)2 add	actual weig	grams	r liter treated 3)2 added	gra	ams ams ams
Makeup NaMnO4 s use NaMnO4.H2O 159.94 grams/mo		/4 lot#	1.099			actual	128
Tare Bottle/flas add 18.278 g for each liter treated	grams NaMn	O4 j		grams simulant ram H2O per ht of KMnO4		gra	ims ims
Date prepared: Prepared by: Work Package Num	nber:	41.		ht of water a	added	4 21,3 Ugra	<u>ims</u>

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